



Numerical simulation of heterogeneous porous media burners using volume averaged modeling

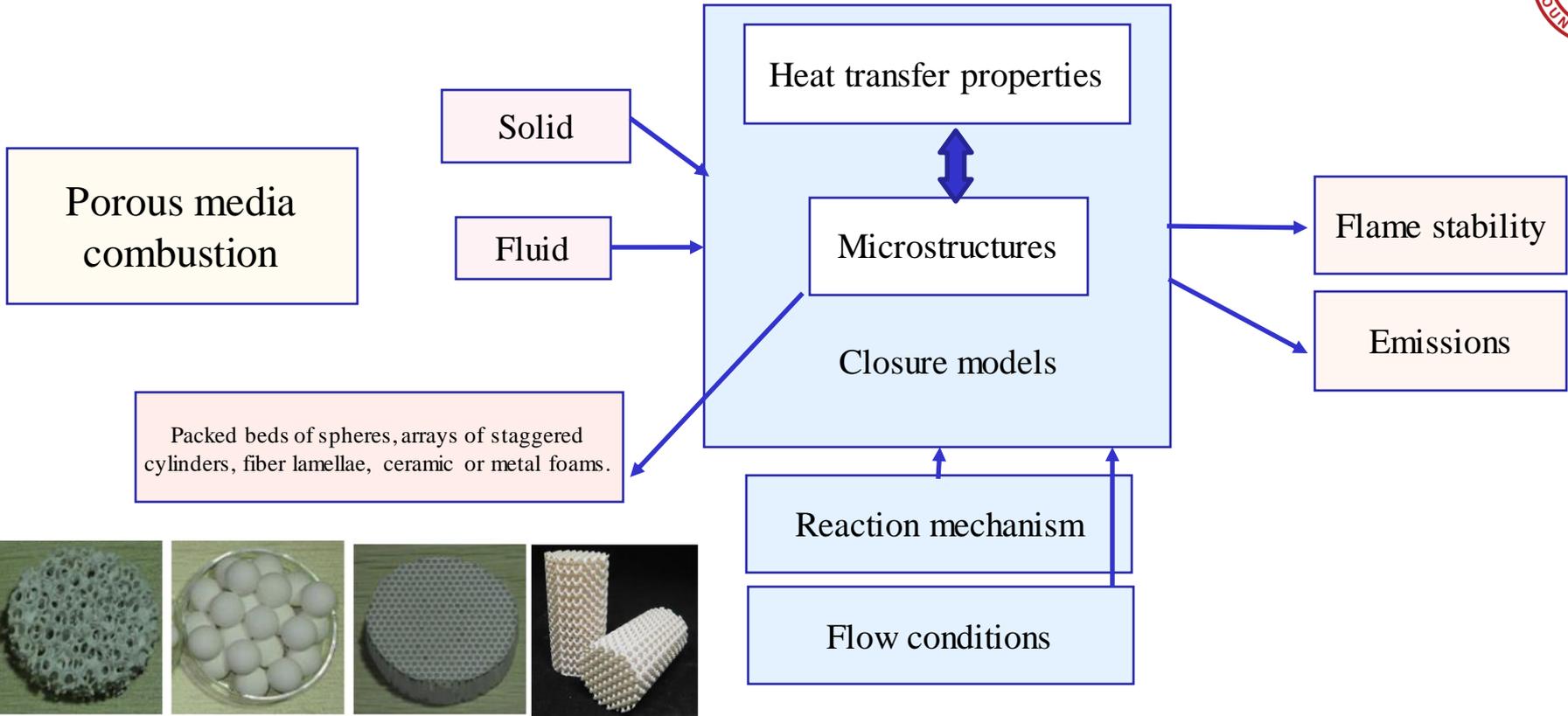
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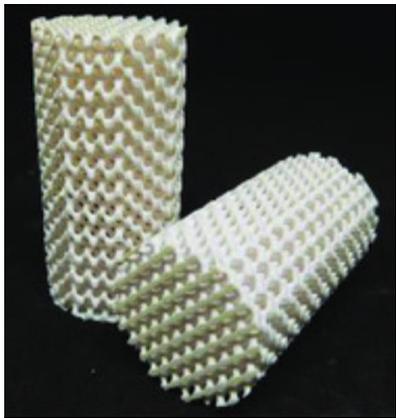
MODELING FRAMEWORK



How can we modulate these properties to obtain desired combustion characteristics?

MOTIVATION

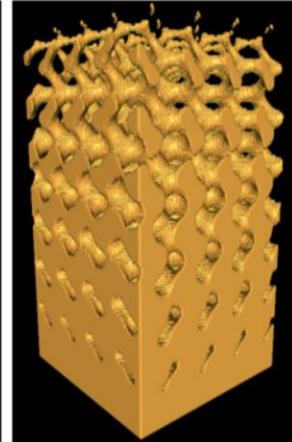
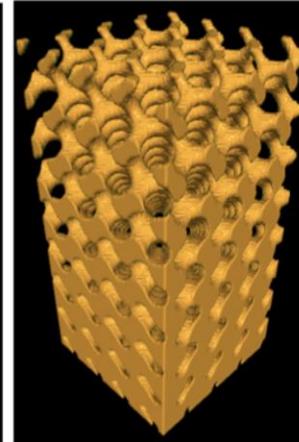
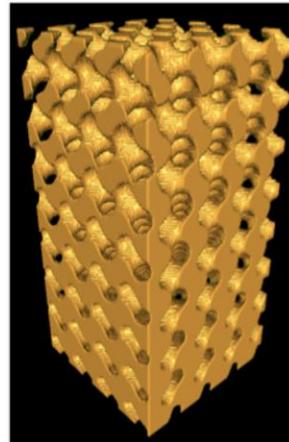
- * Porous media allows combustion to take place in lower fuel/air ratio (leaner equivalence ratio)
- * Microstructure affects the performance of porous media combustion



Uniform pore size



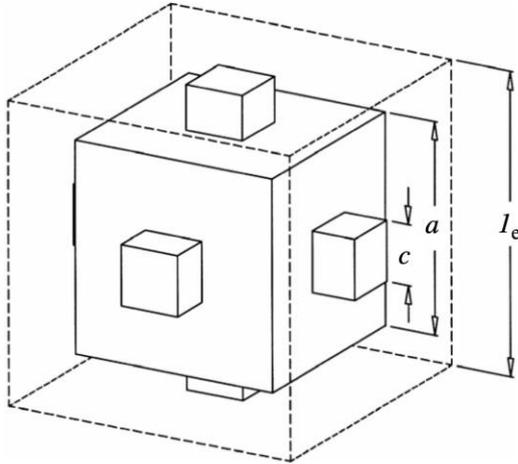
Two stage pore size



Graded pore size

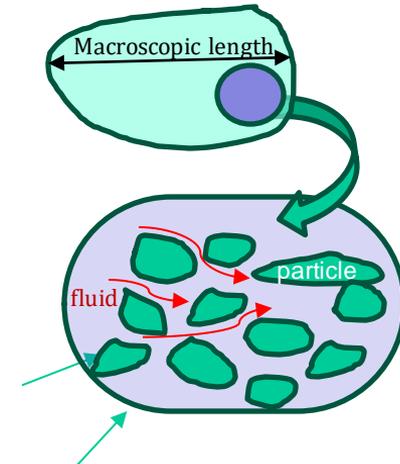
BACKGROUND

- * Combustion simulations using pore resolved model is computationally expensive
- * The microstructure affects heat transfer and performance of the burner
- * The microscopic variations in the microstructure is absorbed in an averaged macroscopic model
- * Volume Averaged Modeling can easily capture the global performance of the system



Pure fluid
(porosity = 1)

Pure solid
(porosity = 0)



A volume with average porosity of $\phi \in [0,1]$



EQUATIONS

$$\bar{\nabla} \cdot \mathbf{U} = 0$$

Continuity equation

$$\rho \left[\frac{\partial}{\partial t} (\mathbf{U}) + \bar{\nabla} \cdot (\mathbf{U}\mathbf{U}/\epsilon) \right] = -\bar{\nabla}(\epsilon P) + \rho \bar{\nabla} \cdot [\nu \bar{\nabla}(\mathbf{U})]$$

Momentum conservation

$$\rho c_{pg} \frac{\partial(\epsilon \bar{T})}{\partial t} + \rho c_{pg} \bar{\nabla} \cdot (\mathbf{U} \bar{T}) = \lambda_g \bar{\nabla} \cdot (\epsilon \nabla \bar{T}) + h_v (\bar{T}_s - \bar{T})$$

Fluid energy conservation

$$\rho_s c_{ps} (1 - \epsilon) \frac{\partial \bar{T}_s}{\partial t} = \bar{\nabla} (\lambda_{s,eff} \nabla \bar{T}_s) - h_v (\bar{T}_s - \bar{T})$$

Solid energy conservation

$$\epsilon \rho \frac{\partial Y_i}{\partial t} + \epsilon \rho \mathbf{U} \cdot \nabla Y_i = \rho \nabla \cdot (\epsilon D_{im} \nabla Y_i) + \epsilon \dot{\omega}$$

Species conservation

The closure of the volumetric heat transfer coefficient h_v depends on the microstructure

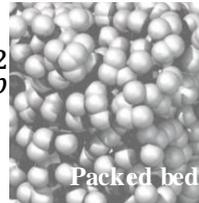


CLOSURE MODELS

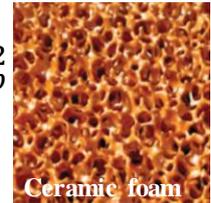
* Closure models

- Coupling of the heat transfer between the solid and the gas phases
- Heat transfer properties depends on the flow, microstructure and the material

$$h_v = 6k_g(1 - \epsilon)[2 + 1.1\text{Pr}^{1/3}\text{Re}_p^{0.6}]/d_p^2$$



$$h_v = 0.146k_g\text{Re}^{0.96}/d_p^2$$



* Flame stabilization

- Anchoring the flame is important for stable combustion
- Porous media enables flame stabilization at leaner equivalence ratios
- Enhanced heat recirculation in the structure



DETAILS OF SOLVER

- Pore size is modelled as a continuous distribution - A continuous pore size distribution leads to a continuous h_p distribution instead of a two section burner
- Reaction is modelled as a GRI3.0 mechanism - 53 species and 325 reactions
- Solid is inert and does not react with the gas mixture. Thermal non-equilibrium is present between the fluid and the solid matrix
- Solid loses heat through radiation
- The model captures the influence of pore size, thermal conductivity, Reynolds number, fuel mass fractions and is computationally less expensive than a detailed pore scale simulation



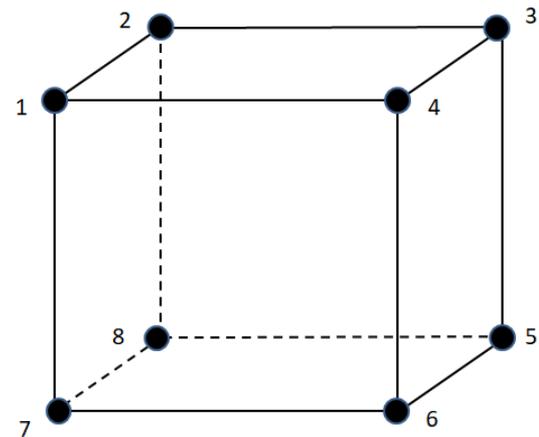
DETAILS OF SOLVER

- Finite volume method solver implemented on OpenFOAM
- Compressible reactive flow solver that uses PIMPLE algorithm
- Utilizing the power of OpenFOAM through continuous distribution of variables

$$(\mathbf{u}, p, Y_i, T)_j \quad \longrightarrow \quad (\epsilon, h_v, \mathbf{u}, p, Y_i, T)_j$$

- OpenFOAM supports TDAC for faster chemistry calculation
- Reactions are solved using the Arrhenius rate model

$$k = AT^\beta e^{(-T_a/T)}$$

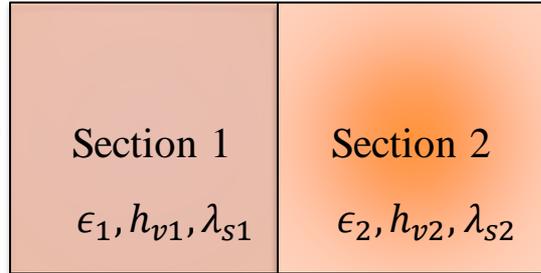




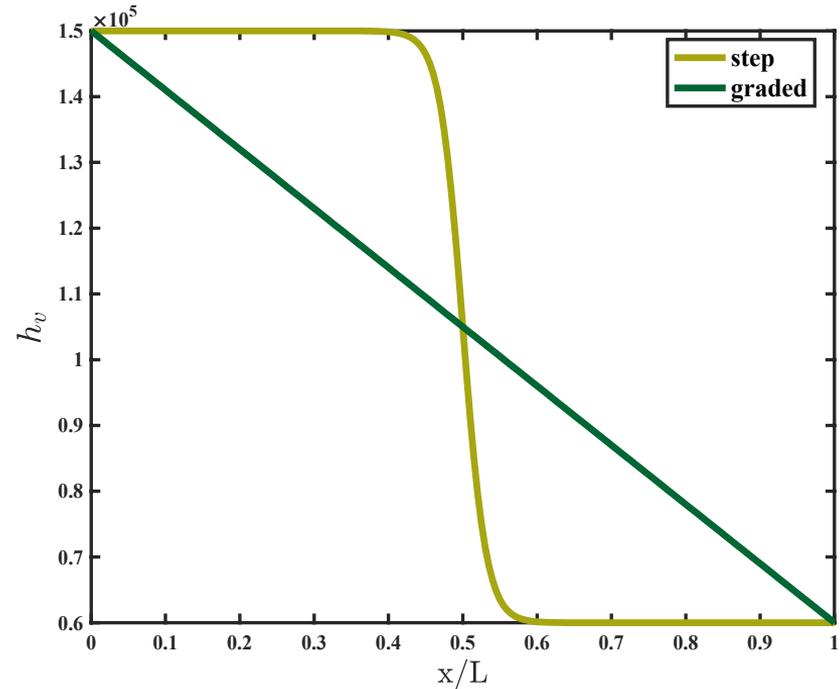
DOMAIN SETUP

$CH_4 + air$

u, T, p, ϕ



A typical two section porous burner

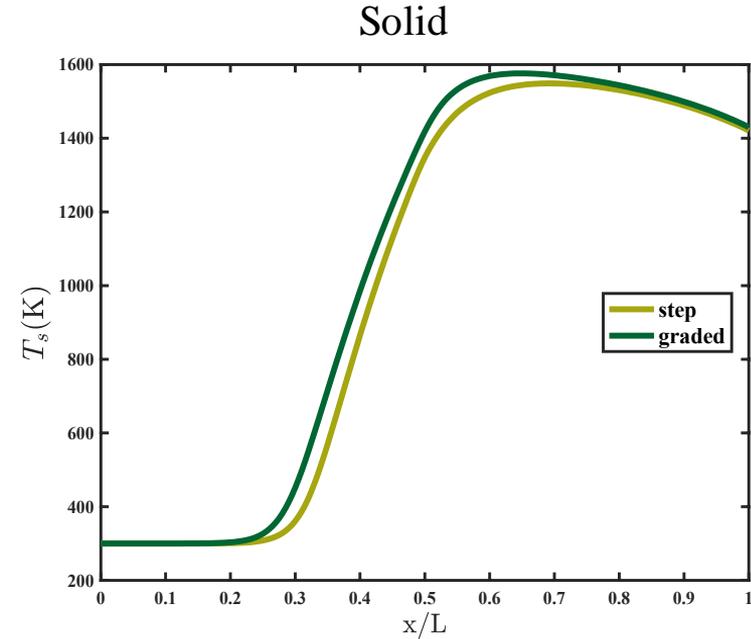
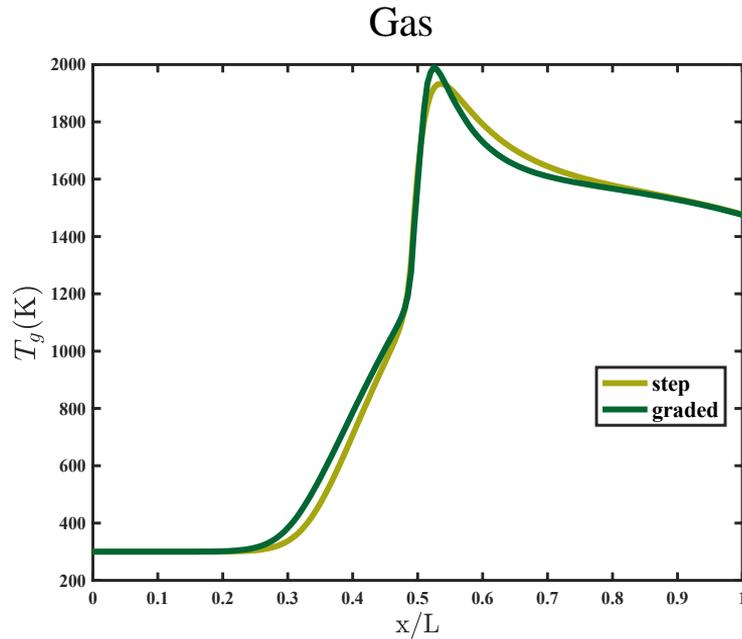


The different burners have different h_v variation



RESULTS

Temperature distribution is responsive to changes in geometry

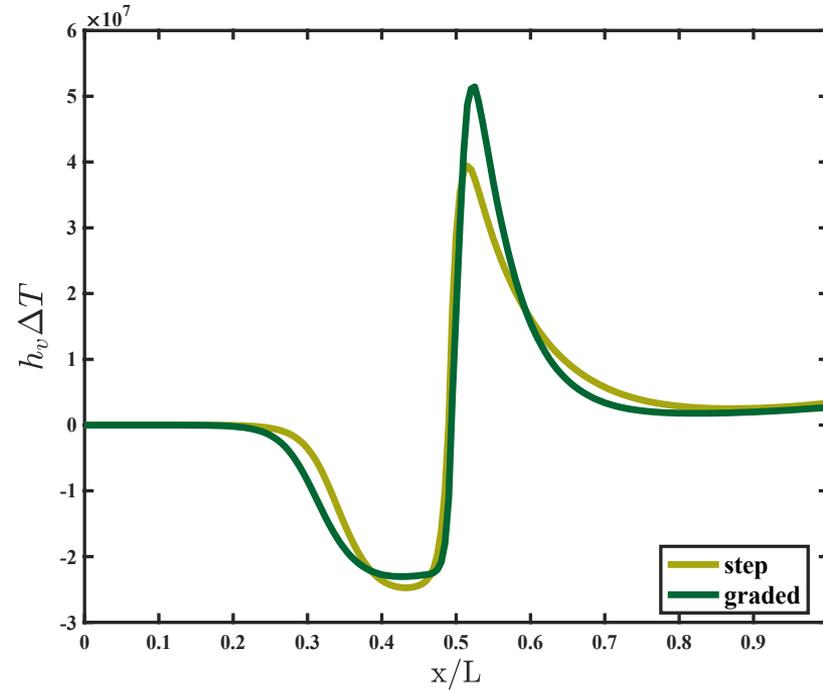


Gas and solid temperature profiles for different burners



RESULTS

Heat exchange profile shows the relative direction/magnitude of heat flow (Gas \leftrightarrow Solid)

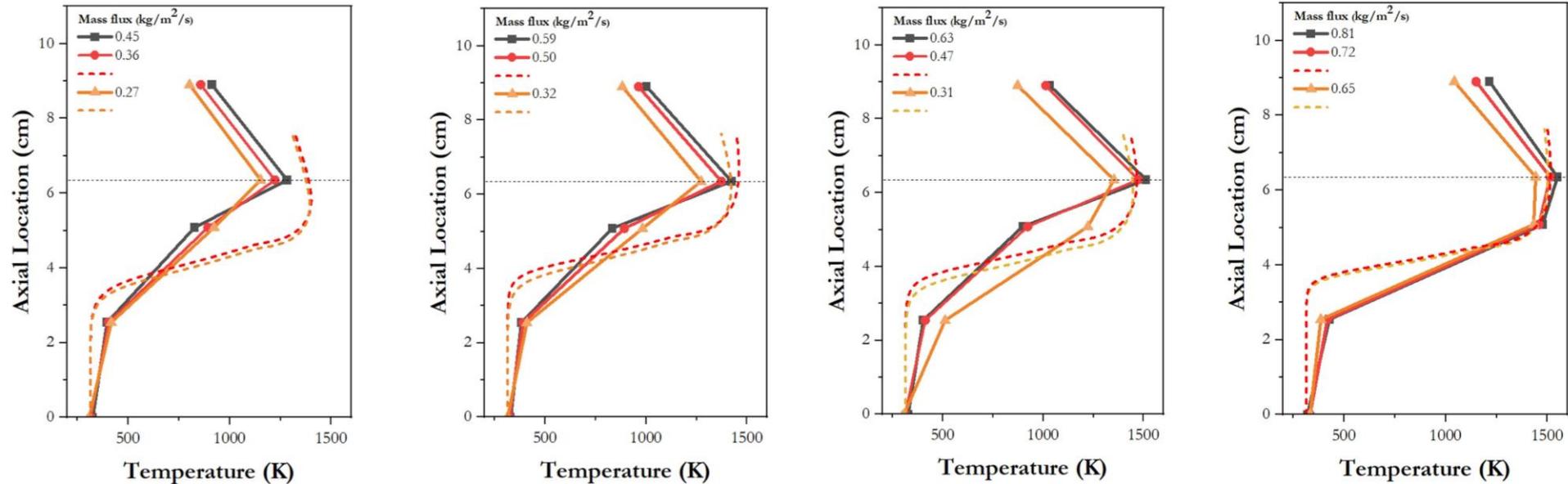


Heat exchange between solid and gas for different burners



RESULTS

Temperature predictions using solver and experiments

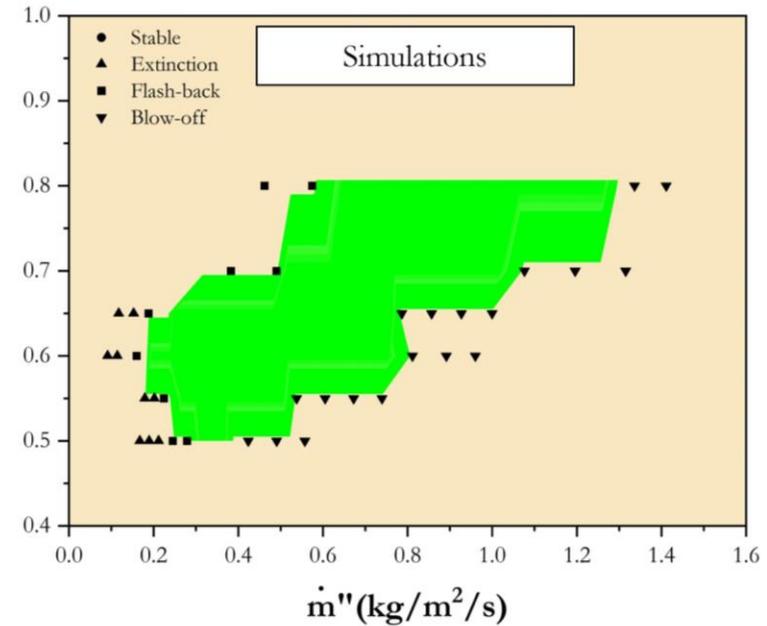
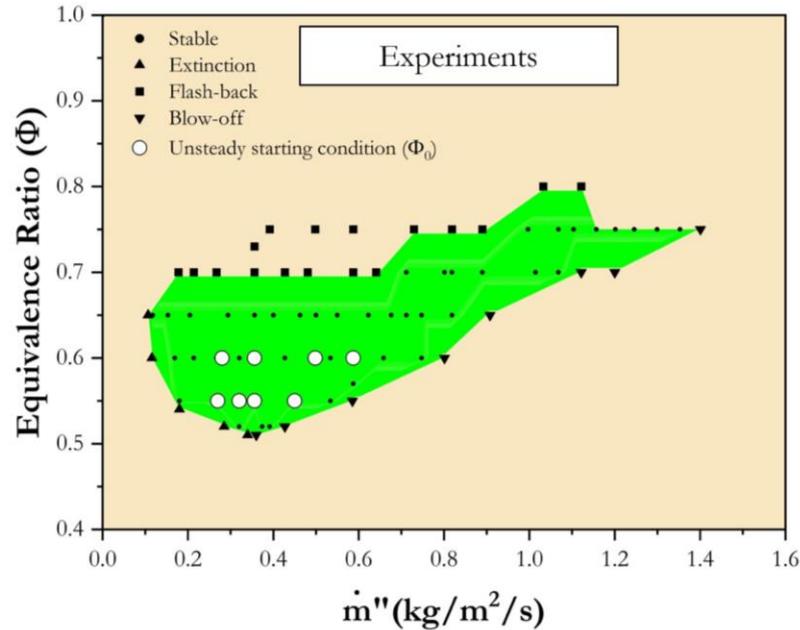


Axial temperature profiles for SiC burner



RESULTS

Sensitivity towards fuel/air ratio and inlet fuel flux

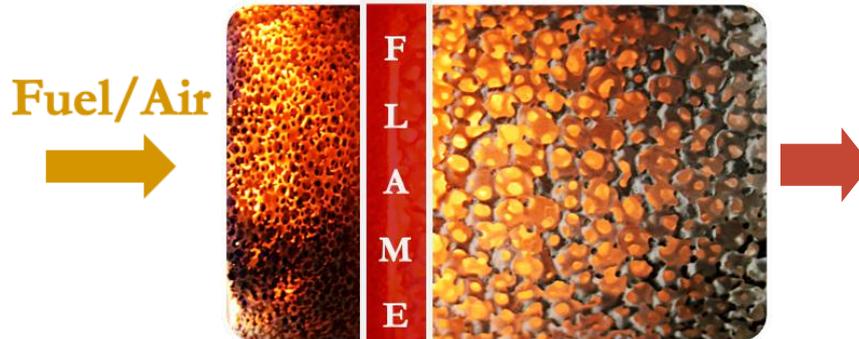


Stability map highlighting the effect of equivalence ratio and mass flux of fuel



CONCLUSIONS

- * OpenFOAM solver has been developed for volume-averaged porous media combustion simulations
- * A volume averaged model can be leveraged to quickly analyse the flame under certain conditions
- * Flame profile can be changed through different microstructures keeping inlet and fuel conditions same
- * Possibility of designing structures to attain required combustion characteristics





FUTURE WORK

- * Additive manufacturing can enable easier combustion validation for different morphologies
- * Combustion of different fuels can be simulated for wide range of applications
- * Experimental data for extensive relations pertaining to different closure models



THANK YOU!

Any questions ?