

# BIOPROCESSING SEPARATIONS CONSORTIUM

## *Three-Year Overview*

Technical Advances,  
Process Economics Influence,  
and State of the Science



## Primary Authors

Bioprocessing Separations Consortium Analysis Team: Sue Jones (Pacific Northwest National Laboratory), Eric Tan (National Renewable Energy Laboratory), Jennifer B. Dunn and Lauren Valentino (Argonne National Laboratory)

## Contributing Authors

**Argonne National Laboratory:** Edward Barry, Louis Edano, Patricia Ignacio-deLeon, Phil Laible, YuPo Lin

**Los Alamos National Laboratory:** Jim Coons, Taraka Dale, Cade Gasway, Benjamin Yap

**Lawrence Berkeley National Laboratory:** Ning Sun, Todd Pray, Eric Sundstrom, Jipeng Yan

**National Renewable Energy Laboratory:** Gregg Beckham, Mary Bidy, David Chiamonte, Ryan Davis, Stefano Dell'Orco, Steve Deutch, Abhijit Dutta, Chai Engtrakul, Stefan Haugen, Eric Karp, Lorenz Manker, Kim Magrini, Bill Michener, Hanna Monroe, Brady Peterson, Patrick Saboe, Mike Sprague, Nolan Wilson

**Oak Ridge National Laboratory:** Michael Z. Hu, Brian L. Bischoff, Aimee Church, Jae-Soon Choi, Zhenglong Li, Ting Wu, Tim Theiss

**Pacific Northwest National Laboratory:** Charlie Freeman, Vanda Glezakou, Suh-Jane Lee, Jian Liu, Marie Swita, Michael Thorson, Huamin Wang,

**Sandia National Laboratory:** Ryan Davis

## Acknowledgements

The Bioprocessing Separations Consortium would like to acknowledge support from Nichole Fitzgerald of the U.S. Department of Energy's Bioenergy Technologies Office (BETO) as well as Clayton Rohman of BETO. Each laboratory of the consortium acknowledges the following support.

Argonne is a U.S. Department of Energy laboratory managed by UChicago Argonne, LLC under contract DE-AC02-06CH11357.

Lawrence Berkeley National Laboratory is managed and operated by the University of California under contract number DE-AC02-05CH11231.

Los Alamos National Laboratory is operated by Triad National Security, LLC, for the National Nuclear Security Administration of U.S. Department of Energy (Contract No. 89233218CNA000001).

The work at the National Renewable Energy Laboratory was supported by the U.S. Department of Energy under Contract No. DE347-AC36-99GO10337.

The work performed at Oak Ridge National Laboratory was conducted under the auspices of the U.S. Department of Energy under Contract DE-AC05-00OR22725 with UT-Battelle, LLC, which manages ORNL.

Pacific Northwest National Laboratory is operated by Battelle Memorial Institute for the U.S. Department of Energy under Contract No. DE-AC05-76RL01830.

Sandia National Laboratories is a multi-mission laboratory managed and operated by National Technology and Engineering Solutions of Sandia, LLC., a wholly owned subsidiary of Honeywell International, Inc., for the U.S. Department of Energy's National Nuclear Security Administration under contract DE-NA0003525.

## Disclaimer

This report was prepared as an account of work sponsored by an agency of the United States Government. Neither the United States Government nor any agency thereof, nor UChicago Argonne, LLC, nor any of their employees or officers, makes any warranty, express or implied, or assumes any legal liability or responsibility for the accuracy, completeness, or usefulness of any information, apparatus, product, or process disclosed, or represents that its use would not infringe privately owned rights. Reference herein to any specific commercial product, process, or service by trade name, trademark, manufacturer, or otherwise, does not necessarily constitute or imply its endorsement, recommendation, or favoring by the United States Government or any agency thereof. The views and opinions of document authors expressed herein do not necessarily state or reflect those of the United States Government or any agency thereof, Argonne National Laboratory, or UChicago Argonne, LLC.

# Table of Contents

---

<b>Acronyms and Abbreviations .....</b>	<b>v</b>
<b>1 Executive Summary .....</b>	<b>1</b>
<b>2 Consortium Motivation .....</b>	<b>7</b>
<b>3 Consortium Approach .....</b>	<b>8</b>
<b>4 Consortium Portfolio .....</b>	<b>12</b>
4.1 Biochemical Processing .....	12
4.1.1 Polymeric and Ceramic Membrane Fractionation of Lignin.....	13
4.1.2 In Situ Product Recovery (ISPR).....	15
4.1.3 Membrane-Sorbent Separations for Diol Recovery.....	20
4.1.4 Ultrasonic Separation of Lignocellulosic Particles.....	22
4.1.5 Recovery of NaOH and Lignin Products .....	24
4.1.6 Economics and Sustainability.....	25
4.1.7 Industrial Relevance.....	29
4.2 Thermochemical Separations.....	33
4.2.1 Catalytic Hot Gas Filtration (CHGF) .....	33
4.2.2 EDI-Based Recovery of Dilute Organic Carbon and Ammonia in the Aqueous Phase.....	35
4.2.3 Removal of Ammonia from HTL Aqueous Streams as a Wastewater Treatment Option .....	37
4.2.4 Bio-oil and Biocrude Preprocessing with Adsorbents.....	40
4.2.5 Industrial Relevance.....	41
4.3 Seed Projects .....	44
4.3.1 Biochemical Catalyst Preservation .....	44
4.3.2 Algae Dewatering .....	47
<b>5 Stakeholder Engagement.....</b>	<b>51</b>
5.1 Industrial Advisory Board (IAB) .....	51
5.2 Meetings, Conferences, and External Communications.....	51
5.3 Directed Funding Opportunity.....	52
<b>6 Summary.....</b>	<b>53</b>
<b>7 References.....</b>	<b>55</b>

## Figures

1	Conversion pathways from feedstock to products. ....	8
2	Approach to prioritizing research challenges to incorporate in the Consortium’s portfolio. ....	9
3	Overarching challenges the Consortium addressed in its first 3 years. ....	10
4	Consortium structure. ....	12
5	Experimental process for lignin separation via TFF membrane. ....	13
6	Molecular weight response for lignin fractionation via polymeric membranes: 5 kDa, 1 kDa, and nano represent the membrane pore sizes; the y-axis is based on ultraviolet absorbance of gel permeation chromatography; compounds over 1 kDa that are present in the alkaline pretreatment liquor remain in the retentate. ....	14
7	Left: Visual product quality. Right: Molecular weight response for lignin fractionation via ceramic membranes. ....	14
8	Left: HED ISPR flow for carboxylic acid production and separation. Right: Conceptual separation effects. ....	15
9	Left: EDI ISPR acid recovery flow. Right: Conceptual separation effects. ....	16
10	HED-ISPR equilibrium concentration of butyric acid in the organic phase as a function of pH and the initial acid concentration in the aqueous phase ....	17
11	Bioreactor HED-ISPR for bio-ester production and separation. ....	17
12	Triethylphosphine oxide (TOPO) results: (a) Process diagram of acetic acid separation from extractant. In the first distillation column, extractant is easily separated from water and acid with four stages. A second column is needed to separate water from acid. (b) Energy input of the process per kilogram of acetic acid product as a function of acid concentration in the bioreactor at pH 3. ....	18
13	EC-ISPR acid recovery recovered 92% of butyric acid. ....	19
14	EDI membranes and performance for recovery of acetic acid from a dilute aqueous solution. ....	20
15	(a) Pervaporation membranes and sorbents evaluated for BDO separations; (b) Type-1 hydrophobic membrane performance at different vacuum pressures; (c) Type-2 superhydrophilic membrane performance at different temperatures. ....	21
16	Ultrasonic separation conceptual illustration. ....	22
17	Left: Ultrasonic experimental setup showing fines concentration in the standing wave. Right: Experimental results of fines removal in continuous flow. ....	23
18	Vessel-limited energetics of cellulosic fines removal using ultrasonic filtration in baseline and LANL operating modes. ....	24
19	Left: EDI concept. Right: acid base separation results. ....	25
20	Box flow diagram for SMB, EDI, and pertractive separations. ....	27
21	Separation costs for SMB, EDI, and pertractive technologies. ....	28

## Figures (Cont.)

22	Lifecycle GHG emissions for SMB, EDI, and pertractive technologies. ....	28
23	Life-cycle water consumption (L/MJ) in the production of renewable diesel through an acid intermediate. ....	29
24	Separation challenges for two types of thermochemical processes. ....	33
25	Hot gas filtration experimental setup. ....	34
26	Filtration and conversion results for various filter materials and catalysts. ....	34
27	Selective extraction of dilute organic acids from the thermochemical (TC) waste aqueous phase using the EDI platform system. ....	36
28	EDI results for acid and ammonia recovery from HTL aqueous phase. ....	36
29	Left: HiPAS membrane concept. Right: Acetic acid concentration over time in permeate stream as a result of pervaporation. ....	37
30	Waste HTL flow diagram. ....	38
31	Potential cost reduction through use of EDI for acid and base recovery from HTL aqueous phase. ....	38
32	GHG reduction for EDI-based recovery of mixed acids and ammonia from HTL aqueous phase. ....	39
33	Fossil energy consumption for EDI-based recovery of mixed acids and ammonia from HTL aqueous phase. ....	39
34	Water consumption for EDI-based recovery of mixed acids and bases from the HTL aqueous phase. ....	40
35	Effect of adsorbent type on carbonyl removal from bio-oil and nitrogen species removal from biocrude. ....	40
36	Economic impact of carbonyl removal from bio-oil. ....	41
37	Materials developed in the Consortium include nanoparticles, xerogels, and polymeric foams. ....	45
38	Adsorbent screening results for capturing three representative aldehydes: (a) formaldehyde, (b) acetaldehyde, and (c) benzaldehyde. ....	46
39	Experimental setups for separations via ultrasonics and membranes. ....	48
40	Characteristics of algae cultures used in the harvesting and dewatering study. ....	48
41	Ultrasonic removal of algal species showing agreement between batch and (steady) flow tests, which indicates the insignificance of hydrodynamic effects over the range of conditions studied. ....	49
42	(a) Concentration factors obtained in flow tests increases according to the ratio of filtrate to concentrate flow rates shown in parenthesis. (b) Ultrasonic harvesting energy as a fraction of the energy in the microalgae removed using ultrasound. ....	49

## Tables

1	Summary of technologies developed in Bioprocessing Separations Consortium .....	2
2	Target compounds identified during Industrial Listening Day .....	10
3	Industrial relevance of separation technologies applicable to biological conversion processes. ....	30
4	Industrial relevance for thermochemical separation applications. ....	42
5	Impurities that affect fermentation. ....	45
6	Binding ratios for various materials and impurities. ....	47
7	IAB members, FYs 2017–2019. ....	51
8	Direct Funding Opportunity projects between industry and Consortium members. ....	52
9	Consortium project slate: FYs 2020–2022. ....	54

# Acronyms and Abbreviations

---

APL	alkaline pretreatment liquor
Argonne	Argonne National Laboratory
BDO	butanediol
BETO	Bioenergy Technologies Office
BNL	Berkeley National Laboratory
EDI	electrodeionization
HED	hybrid extraction and distillation
HPA	heteropolyacid
HTL	hydrothermal liquefaction
GHG	greenhouse gas
ISPR	in situ product recovery
LANL	Los Alamos National Laboratory
LCA	lifecycle analysis
MFSP	minimum fuel selling price
NP	nanoparticle
NREL	National Renewable Energy Laboratory
ORNL	Oak Ridge National Laboratory
PNNL	Pacific Northwest National Laboratory
RW/PE	resin wafers with nonconductive polyethylene solid polymer binder
SMB	simulated moving bed
SNL	Sandia National Laboratory
SOT	state of technology
TEA	technoeconomic analysis
TFF	tangential flow filtration



*This page left intentionally blank.*

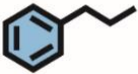






# 1 Executive Summary

---

The Bioprocessing Separations Consortium solves separations challenges that are unique to bioprocessing. To do this, the Consortium uses two methods: applying existing technologies to new challenges and developing new technologies that may address these unique challenges better than today's commercial technologies. In its research and development, the Consortium leverages its three core capabilities: materials development and evaluation, process development, and analysis and computation.

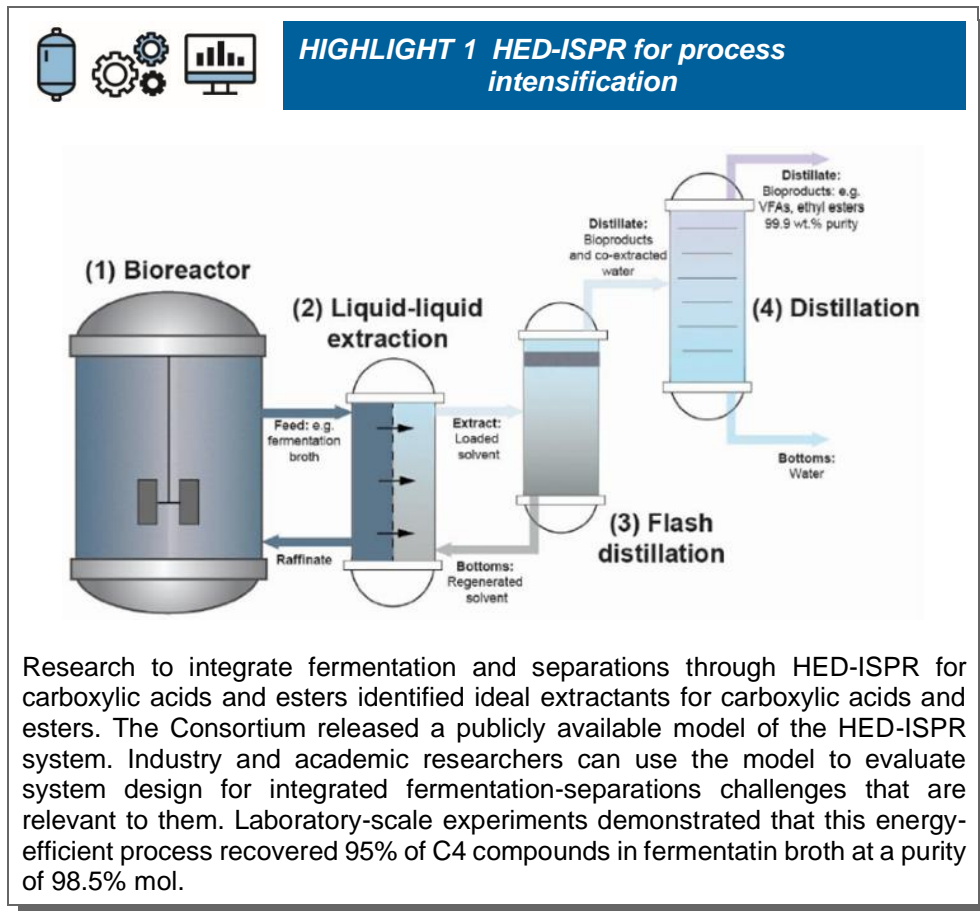
In its first three years, from 2016 to 2019, the Consortium addressed four critical challenges in biochemical and thermochemical processing. First, the Consortium targeted the fractionation of lignin to enable valorization of this portion of biomass that offers diverse, complex, and valuable building blocks and products. Second, Consortium researchers developed technologies to enable process intensification, which can reduce equipment needs, energy consumption, and waste generation, thereby cutting bioprocessing capital costs and rendering processes more efficient. Third, the Consortium sought to recover carbon from dilute aqueous streams that are common to bioprocessing; recovering dilute carbon can improve process efficiency and economics. Finally, Consortium researchers designed and developed new materials and catalysts to reduce targeted foulants and poisons in bioprocessing streams that can limit the lifetime of downstream catalysts or fermenting microorganisms. Table 1 lists the technologies that were examined and places them in the context of the Consortium's capabilities, types of bioprocesses, and critical challenges in bioprocessing separations. Overall, across these projects, we have developed separations technologies for 10 bioprocesses, addressed 9 target compounds in bioprocessing, developed 10 materials, and evaluated 4 processes for cost and sustainability.

Table 1 Summary of technologies developed in Bioprocessing Separations Consortium.<sup>a</sup>

Technology	Conversion Pathway		Challenges Addressed				Capabilities Applied		
	BC	TC	 Lignin Fractionation	 Process Intensification	 Dilute C Recovery	 Inhibitor Removal	 Materials	 Processes	 Analysis & Computation
HED-ISPR	X			X				X	X
EDI-ISPR	X			X			X	X	X
EDI	X	X			X	X	X	X	X
Ultrasonic	X		X					X	X
Pervaporation	X			X	X			X	
Distillation (membrane)	X				X			X	
Polymeric membranes	X		X		X			X	
Ceramic membranes	X		X					X	
Simulated moving bed	X				X			X	
Catalytic gas hot filtration		X		X		X	X	X	X
Adsorbents	X	X			X	X	X	X	X

<sup>a</sup> BC: Biochemical. TC: Thermochemical. ISPR: In situ product recovery. HED: Hybrid extraction and distillation. EDI: Electrodeionization.

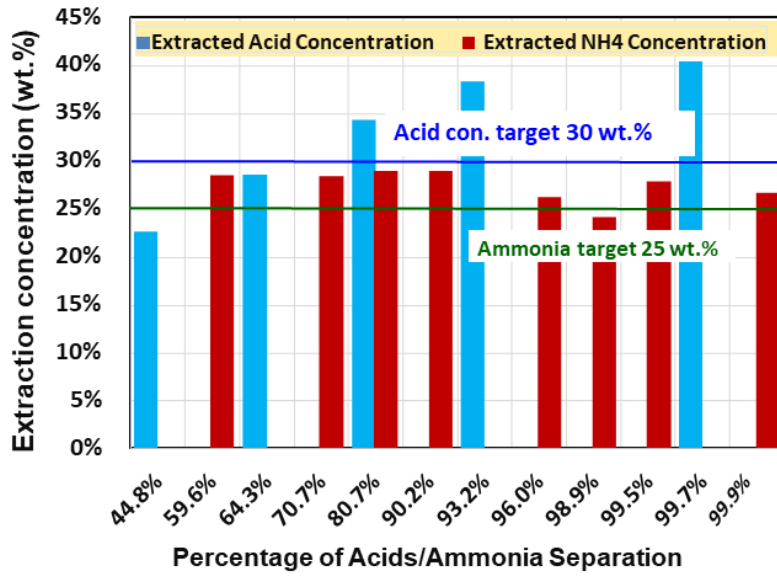
Particular Consortium research highlights include the following examples in Highlights 1–4.



Research to integrate fermentation and separations through HED-ISPR for carboxylic acids and esters identified ideal extractants for carboxylic acids and esters. The Consortium released a publicly available model of the HED-ISPR system. Industry and academic researchers can use the model to evaluate system design for integrated fermentation-separations challenges that are relevant to them. Laboratory-scale experiments demonstrated that this energy-efficient process recovered 95% of C4 compounds in fermentatin broth at a purity of 98.5% mol.



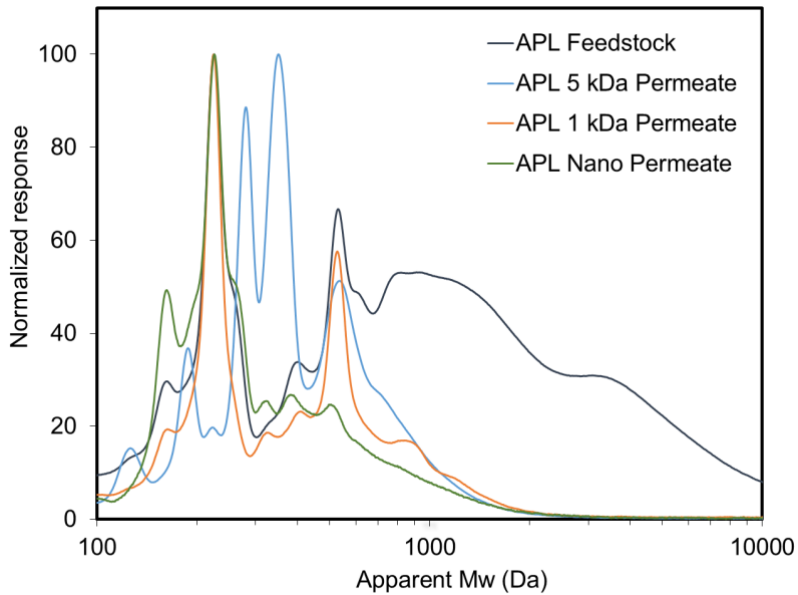
## HIGHLIGHT 2 EDI for recovery of dilute carbon in aqueous streams



EDI-based separations maintained high concentrations of recovered acid and NaOH regardless of the percentage removal. Concentrations of each species exceeded the target level.



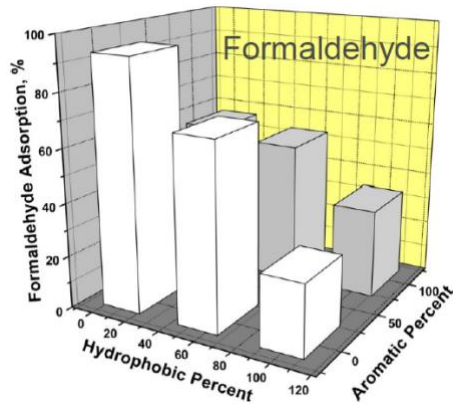
### HIGHLIGHT 3 Polymeric and ceramic membranes for lignin fractionation



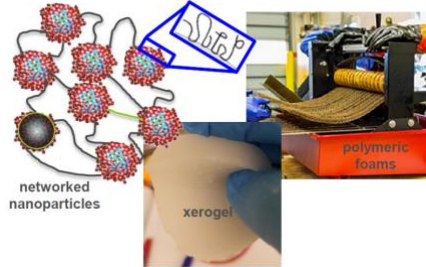
For lignin conversion, species with high molecular weights must be removed and other compounds separated as a function of molecular weight. Furthermore, lignin fractionation must occur at a sufficiently high, industrially relevant throughput. The Consortium's multi-stage filtration approach to lignin fractionation made significant progress towards these aims, removing compounds above 1 kDa (see above figure) and achieving a flux five to ten times greater than a single 450 Da filtration step.



#### HIGHLIGHT 4 Inhibitor removal with surface-treated nanostructured adsorbents



Designer high-surface-area adsorbents in development



Adsorbents tailored to remove impurities that hinder biological cultivation, such as aldehydes (figure above) showed specificity (over all components of feedstock stream or fermentation broth) of 4:1 for one feedstock contaminant and one inhibitor produced during bio-upgrading.

The Consortium is moving into its second three-year period and will continue to advance bioprocessing separations technologies, supporting research through analysis and interactions with the Consortium's Industrial Advisory Board (IAB).

## 2 Consortium Motivation

---

Overall, industrial separations constitute up to 15% of total energy consumption in the United States (Scholl 2016). In the bio-based economy, bioprocessing separations are significantly less mature than industrial separations that are common in the established petrochemical industry. Bioprocess-relevant separations are universally costly and complex, regardless of the conversion pathway (biochemical, thermochemical, hybrid) used because products are dilute and often in aqueous environments, and the mixtures that result from biomass deconstruction are chemically complex. Accordingly, bioprocessing separations are often a key driver of process costs and suffer from a lack of selectivity. In many cases, separations approaches are inspired by unoptimized bench-scale procedures; therefore, a technology baseline, or definition of the state of technology (SOT), is often lacking.

BETO supported the Bioprocessing Separations Consortium's formation in Fiscal Year 2017 to address the technical challenges and opportunities bioprocessing separations pose and stakeholder feedback (EERE 2014, 2015) that separations challenges impede the cost-competitive production of biofuels and bioproducts. BETO's internal analysis supports this feedback, identifying separations challenges that, if resolved, could reduce minimum fuel selling price (MFSP) of biofuels by up to 50%. The goal of the Bioprocessing Separations Consortium is to develop separations technologies that are cost-effective, high-performing, and scalable through coordinated research that targets industry-relevant bioprocessing separations challenges. As a result of the Consortium's efforts, biofuels and bioproducts industries will have new technologies available to them and they will be able to explore technology options through Consortium analysis.

The goal of the Bioprocessing Separations Consortium is to develop separations technologies that are cost-effective, high-performing, and scalable through coordinated research that targets industry-relevant bioprocessing separations challenges.

Furthermore, the Consortium interfaces with several BETO consortia and projects including ChemCatBio (ChemCatBio 2020), Chemical Upgrading of Biological Intermediates (Elander et al. 2019), Lignin-First Biorefinery Development (Beckham 2019), the Agile BioFoundry (Agile BioFoundry 2020), Co-Optima (EERE 2020), Performance Advantaged Bioproducts (Fitzgerald and Bailey 2018), and the Consortium for Computational Physics and Chemistry (CCPC 2020). The Consortium has multiple roles and objectives in these interfaces, including producing difficult-to-obtain purified products from crude mixtures for further processing, as well as evaluating and identifying cost-effective separations routes to target products of interest.

Motivated by the need to reduce bioprocessing costs to make the production of biofuels and bioproducts more cost-effective, the Consortium sought to advance the science and technology of bioprocessing separations in its first three years. This report documents these advances and provides a brief overview of the Consortium's direction going forward.



### 3 Consortium Approach

All biomass conversion pathways (Figure 1) require cost-effective, molecularly-efficient separations. The science and technology for the separations challenges encountered during biomass conversion remain at relatively early stages and at times must be developed on a case-by-case basis.

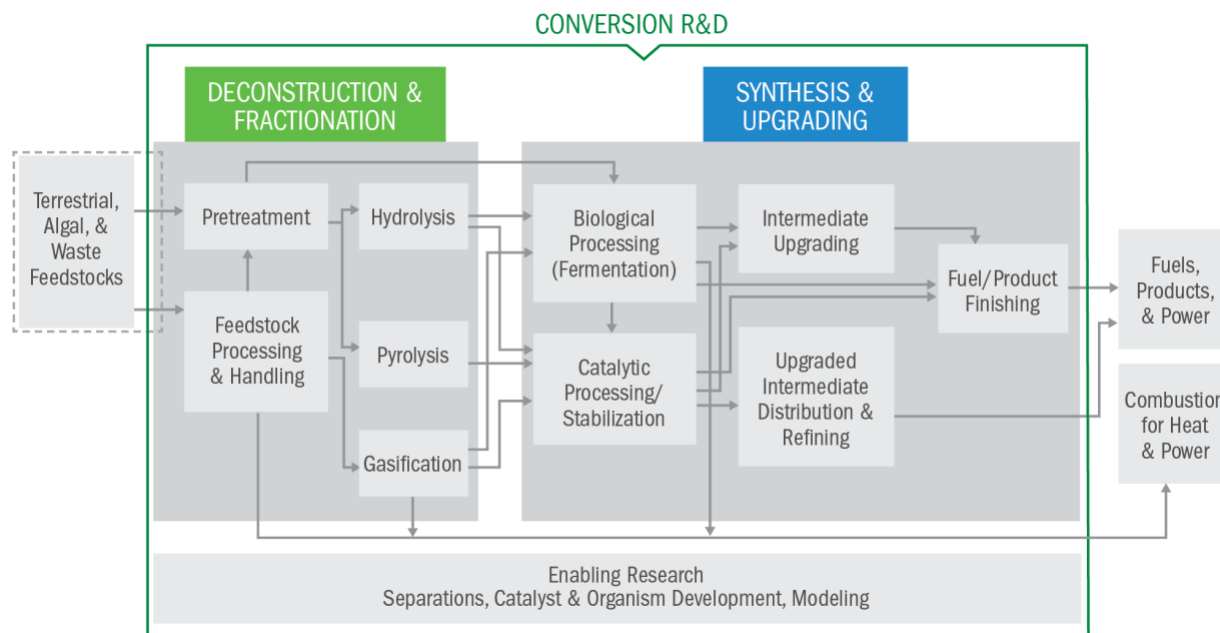


Figure 1 Conversion pathways from feedstock to products (Dunn et al. 2019).

Given the breadth of separations challenges, establishing research priorities for the Consortium requires a structured approach. Figure 2 outlines the approach the Consortium uses to select projects. To start, the Consortium gathers information regarding relevant separations challenges from a variety of external sources. For example, the Consortium confers with the advisory board (Section 5.1) at least twice a year during face-to-face meetings. It also seeks advice from the broader research and industrial community through activities such as the 2017 Listening Day (Bioprocessing Separations Consortium 2017). At this meeting, the Consortium gathered information about compounds of interest to the community (Table 2) and gaps in technologies available to recover them from bioprocesses. The Consortium also carried out a Directed Funding Opportunity (see Section 5.3) in which industry collaborates with national laboratories to solve separations challenges of direct interest to a partner company. Finally, we also solicit feedback from other research teams in the BETO research and development portfolio that face separations challenges.

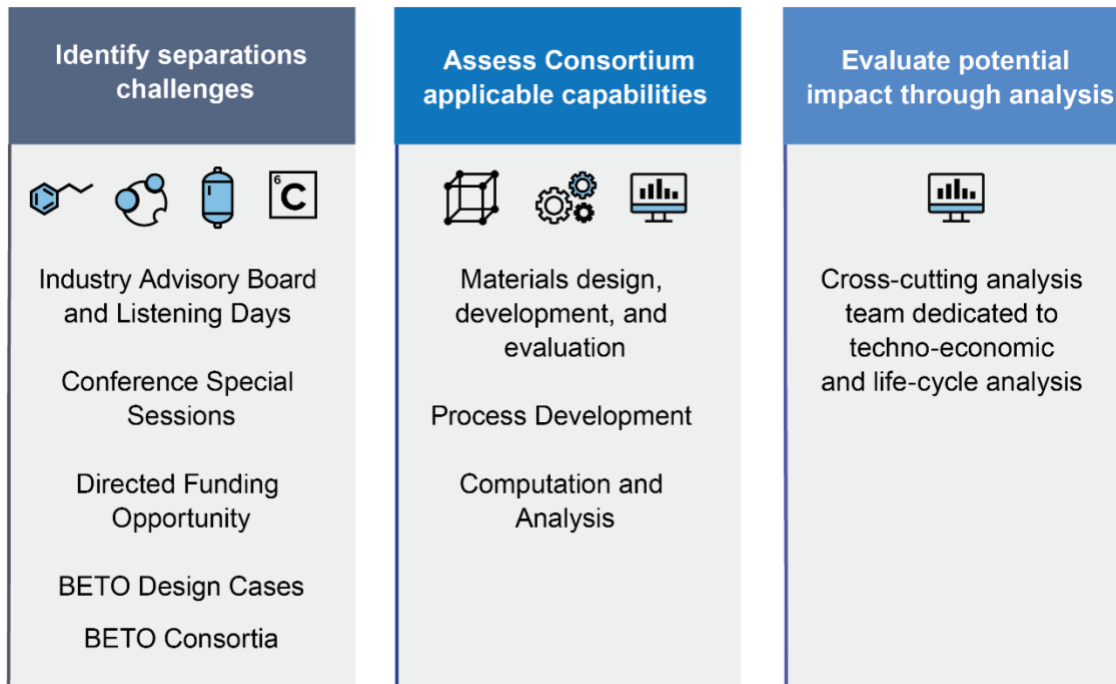


Figure 2 Approach to prioritizing research challenges to incorporate in the Consortium’s portfolio.

The next step in identifying priority and viable projects is to assess whether Consortium capabilities are suitable to address the identified challenges. The Consortium’s key capabilities center on materials design, development, and evaluation, process development, and computation and analysis. It is also important to assess whether the proposed technology can contribute to meeting cost targets for biofuels and bioproducts through overall improved bioprocessing. The Bioprocessing Separations Consortium analysis team addresses this issue and advises on this topic as the Consortium selects challenges for focus. With this process to guide project selection, the Consortium’s research portfolio as described in this report has been designed to cover both biochemical and thermochemical process-related challenges and encompass a variety of technology solutions.

At its outset, the Consortium reviewed the existing design cases in the BETO portfolio and identified four overarching separations challenges that formed the basis of the Consortium’s project portfolio for its first 3 years (Figure 3).

Table 2 Target compounds identified during Industrial Listening Day.<sup>a</sup>

Product Class	Associated Barriers Discussed	Possible Solutions Discussed
Alcohols	High energy requirements for distillation and dewatering	Membranes for dewatering, process configuration-based approaches, and molecular interactions
Organic acids (monomers of low molecular weight acids, short chain fatty acids)	High purity necessary for polymer applications	Resin-based capture, moving bed-type chromatography Focus on removing the organic from the water rather than dewatering Improve predictions of acid-water interactions
Aldehydes and ketones (furfural, butyraldehyde, acetone)	Can inhibit fermentation	In-situ removal from fermentation broth
Oils and fatty acids (oleic and linoleic acids), hydrophobic biofuel precursors	Isolation of closely related structures with different properties	Exploit charged character Chromatography potentially with silver-functionalized resin In-situ removal Intracellular product recovery through dewatering, cell lysis, lipid secretion, and separating lipid products from membrane lipids

<sup>a</sup> Source: Bioprocessing Separations Consortium (2017).

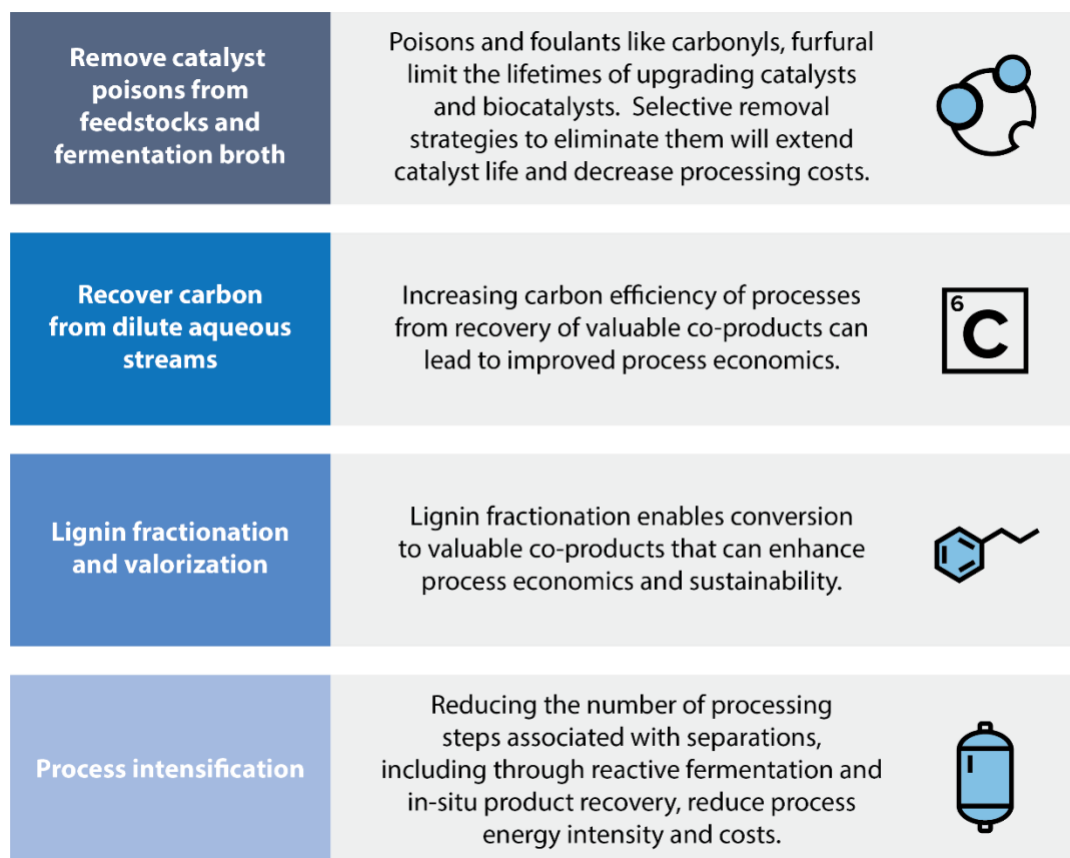


Figure 3 Overarching challenges the Consortium addressed in its first 3 years.

First, the presence of low-molecular-weight foulants in bio-oil limits the performance and lifetime of catalysts used for upgrading thermochemical intermediates. This catalyst lifetime is a key driver of thermochemical processing costs, and the removal of catalyst poisons has the potential to enhance catalyst life downstream. Furthermore, reaction byproducts can poison microorganisms in biochemical processes; therefore, these microorganisms benefit from the removal of such inhibitory compounds to improve rate, titer, and yield of the desired product.

Second, improving the carbon efficiency of bioprocessing could improve processing costs through the recovery of additional carbon in the form of various coproducts. Dilute carbon products in both biochemical and thermochemical processes exist in aqueous streams, and their recovery could enhance carbon efficiency and process economics.

Third, the opportunity to convert lignin into value-added products could reduce the MFSP of biofuels. However, in order to do this the lignin must first be fractionated as a function of molecular weight.

Finally, process intensification is key to improving process economics by reducing capital and operating costs associated with processes. The projects described in the subsequent sections address these key themes, which were the focus of the Bioprocessing Separations Consortium from Fiscal Year (FY) 2017 through FY 2019.

## 4 Consortium Portfolio

Figure 4 shows the Consortium structure for FYs 2017–2019. Experimental research was organized around separation issues related to biochemical processes (e.g., fermentation) and thermochemical processing (e.g., direct liquefaction). We also selected two seed projects that were performed in FY 2017.

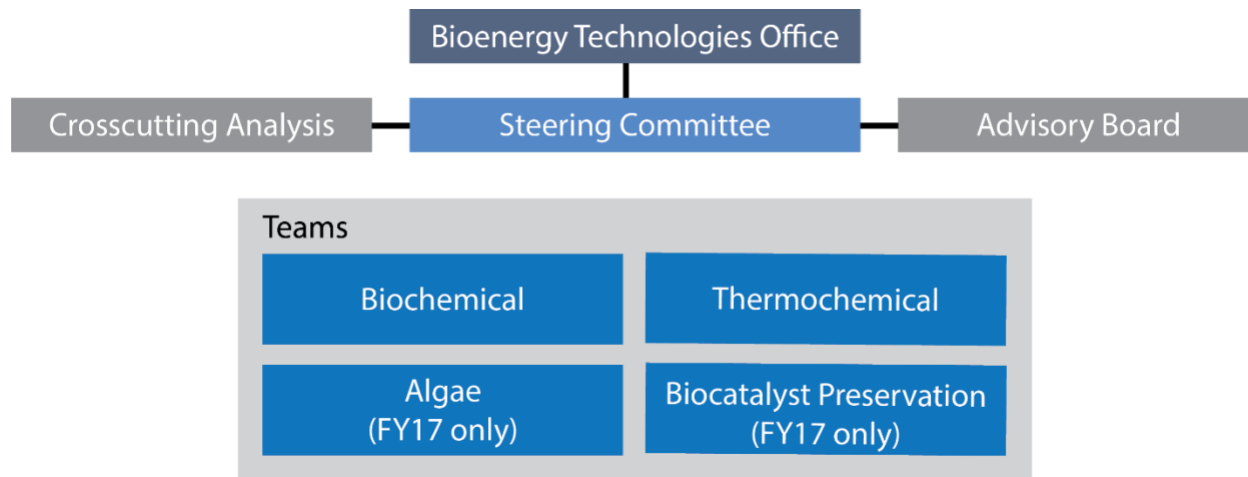


Figure 4 Consortium structure.

The Steering Committee is made up of Consortium lab members who work directly with BETO. They are charged with overseeing the research teams, providing guidance on technical direction, monitoring progress and impact, coordinating external communications, and managing Consortium business via reporting and monthly calls. Within the Consortium, the analysis team’s purpose is to help direct research toward economic and sustainable outcomes, compare separation strategies, and consider risk in terms of applicability at a commercial biorefinery scale. The IAB provides real-world perspectives.

The following sections (4.1-4.2) describe the motivation, approach, outcomes, and gaps in the Biochemical and Thermochemical teams’ work to date. We also report results for two consortium seed projects (4.3).

### 4.1 Biochemical Processing

Within biochemical processing, a key challenge is recovering products at necessary purity levels from fermentation broth, which is a complex and dilute mixture. Process integration could cut overall costs. Also, cost-effective routes to lignin utilization are essential for viable lignocellulosic biorefineries.



### 4.1.1 Polymeric and Ceramic Membrane Fractionation of Lignin

**Motivation.** Lignin fractionation is key to its efficient and economically viable conversion to value added products (Humpert 2016). The Consortium continues to investigate multistage filtration to maximize lignin fractionation flux to reach industrially relevant throughput using three technologies, informed in part by interactions with the Lignin First Biorefinery Development and Lignin Utilization Projects, both also supported by BETO. The filtration stages are polymeric membranes in the range of 2–5  $\mu\text{m}$  followed by nanofiltration with ceramic membranes at approximately 450 Da.

**Approach.** The experimental setup consists of corn stover pretreatment with a base, then solid-liquid separation followed by membrane separation (Figure 5). Note that both polymeric and ceramic membranes are operated in tangential flow filtration (TFF) mode and both can foul (Arkel 2014). Ceramics have the advantage of being stable under pH 12–14 conditions that are typical when biomass pretreatment is achieved with caustic-enabled mechanical deconstruction. Selected polymeric membranes can be operated within a pH range of 1.5–12, and membrane regeneration has been demonstrated for this lignin fractionation application.

Although fouling was not a significant issue at the laboratory scale, it may become a challenge at larger scales. One option to reduce fouling on ceramic membranes is to use rotary disk filtration, a dynamic filtration technique that operates by rapidly moving the membrane surface to generate a high shear force at the filter surface. This high shear force constantly sloughs off material and reduces cake formation. This reduction in cake formation allows large reductions in volume while maintaining high permeance.

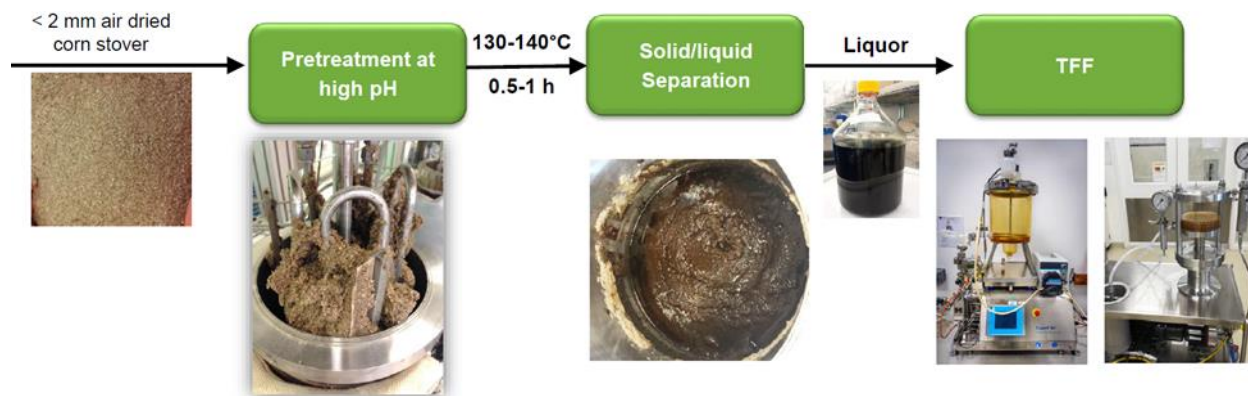


Figure 5 Experimental process for lignin separation via TFF membrane.

**Results.** Results for testing with different polymeric membrane materials are shown in Figure 6. The data demonstrate molecular weight fractionation using commercial TFF membrane separations.

The molecular weight response in Figure 6 indicates that large molecules (>1 kDa) were separated by ultrafiltration (1 kDa and 5 kDa) and nanofiltration. Compounds over 1 kDa that initially are present in the alkaline pretreatment liquor (APL; black line) remain in the retentate. It is these large molecules that most impede lignin fractionation and subsequent processing. The ceramic membrane pore sizes of 5 and 1 kDa were also effective at removing high-molecular-weight components and color (Figure 7).

The relative clarity of the 5- and 1-kDa permeates compared to the lignin liquor feed indicates the absence of the high molecular weight compounds. Overall, this multistage approach to filtration improves flux approximately 5 to 10 times compared a single-step 450-Da filtration. Filters with this pore size are essential to remove high-molecular-weight components from

The Consortium's multistage filtration approach to lignin fractionation achieved a flux 5–10 times greater than a single 450-Da filtration step.

lignin streams. Future work aims to increase permeance of these nanofiltration membranes to achieve industrially relevant processing throughput, which is at least 1 L/hr/m<sup>2</sup>/bar.

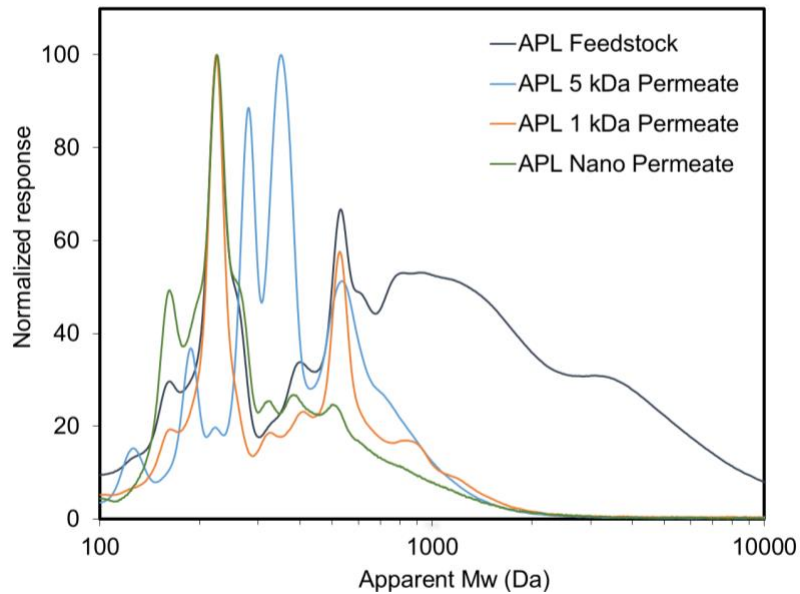


Figure 6 Molecular weight response for lignin fractionation via polymeric membranes: 5 kDa, 1 kDa, and nano represent the membrane pore sizes; the y-axis is based on ultraviolet absorbance of gel permeation chromatography; compounds over 1 kDa that are present in the alkaline pretreatment liquor (APL; black line) remain in the retentate.

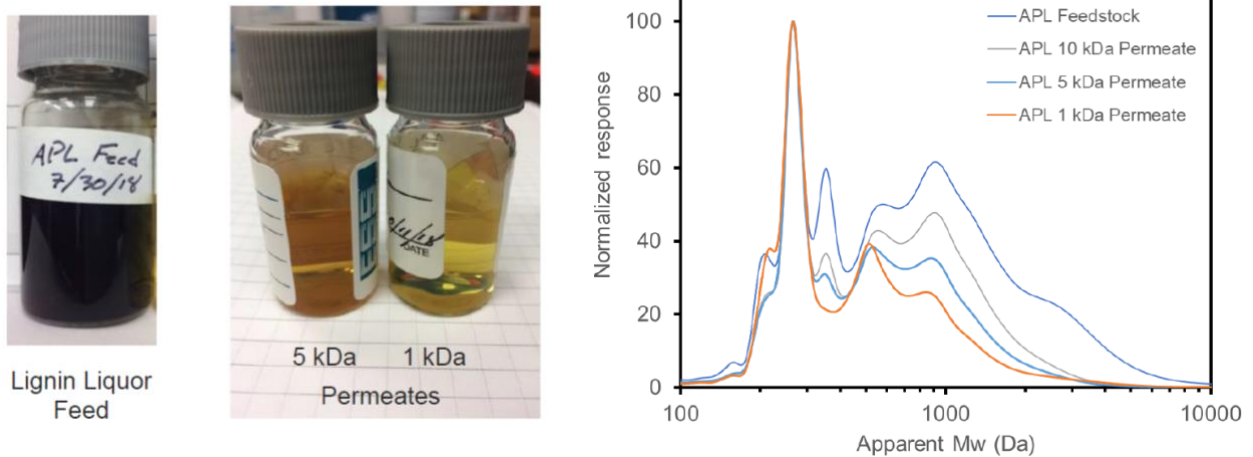


Figure 7 Left: Visual product quality. Right: Molecular weight response for lignin fractionation via ceramic membranes. Compounds over 1 kDa that are present in the APL feedstock remain in the retentate.



## 4.1.2 In Situ Product Recovery (ISPR)

**Motivation.** Often, distillation is the go-to separations strategy to recover products post-fermentation in a biorefinery. However, opportunities exist to leverage other separations techniques that could be less energy intensive and offer opportunities for process intensification.

The Biochemical Separations Team investigated ISPR to recover carboxylic acids from fermentation broth. Two technologies were used: hybrid extraction and distillation (HED) and electrodeionization (EDI).

In general, ISPR systems increase fermentation rate, titer, and yield by extracting a product from fermentation broth as it is produced. This ameliorates end-product inhibition, thereby allowing longer fermentation times with greater productivity.

**Approach.** The HED-ISPR apparatus developed in the Consortium (Figure 8) comprises a membrane contactor coupled with a distillation unit. In contrast, the EDI-ISPR separations (Figure 9) rely on ion-exchange resins and electric fields to affect acid recovery.

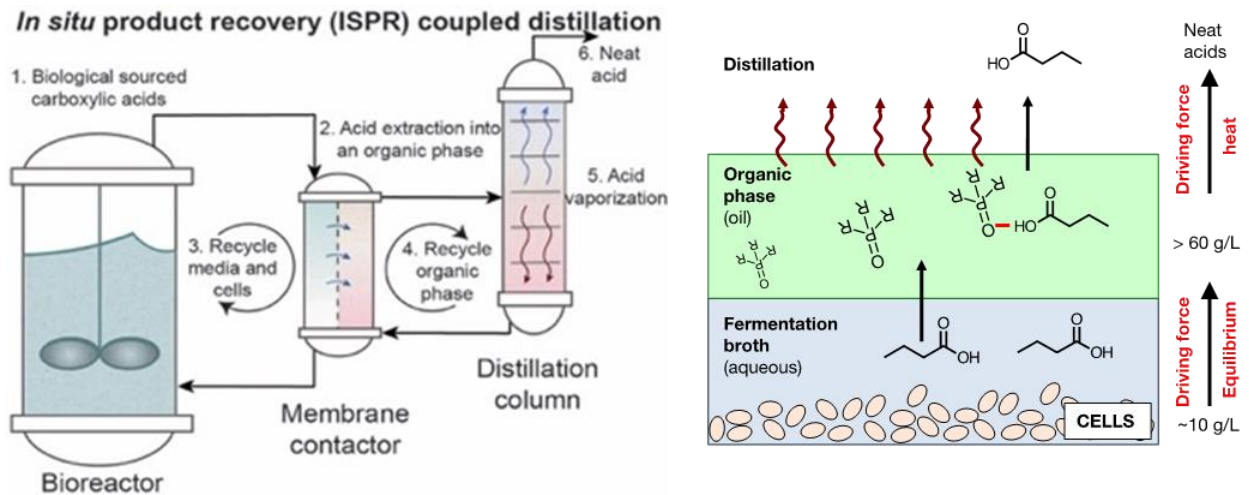


Figure 8 Left: HED-ISPR flow for carboxylic acid production and separation. Right: Conceptual separation effects (Saboe et al. 2018).



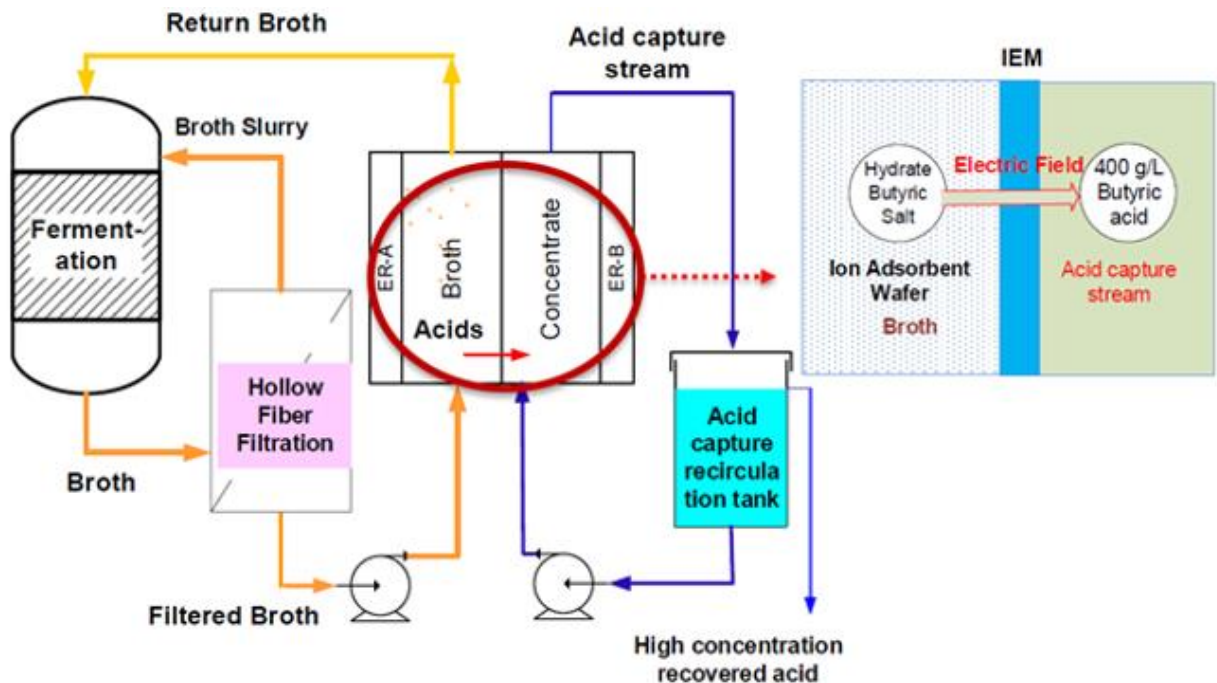


Figure 9 Left: EDI-ISPR acid recovery flow. Right: Conceptual separation effects.

**Results: HED-ISPR.** Research and development of HED-ISPR resulted in four key outcomes. First, a large number of extractants were evaluated for carboxylic acids and esters. Experimental screening of more than 20 extractants found the best extractant for carboxylic acid recovery is the commercial phosphine oxide extractant Cyanex 923 because of its ability to form strong acid base pairs with the acidic protons on carboxylic acids (Saboe et al. 2018). For esters, experimental screening found oleyl alcohol to be the most effective because its hydrostatic interaction with carbonyl functional groups in ester compounds is stronger (Saboe et al. 2019).

HED-ISPR research led to identification of ideal extractants for carboxylic acids and esters. A publicly available model of the system is available to researchers exploring the technology. The energy-efficient process recovered 95% of C4 compounds in fermentation broth at a purity of 98.5% mol.

Second, important thermodynamic properties for carboxylic acids in fermentation systems were measured and reported for different solvents. These properties can be used in modeling and developing new processes to separate carboxylic acids.

Third, a system model requiring only fermentation pH and maximum titer for microorganism productivity was developed (NREL 2019),<sup>1</sup> made publicly available, and used to improve microbial performance. The model is an interactive MATLAB® application to easily predict organic phase acid loading for single and/or mixed acid systems (Figure 10). The model allows users to design a complete HED-ISPR system for a given carboxylic acid or ester bioproduct including the downstream distillation train needed for pure product recovery. Figure 11 illustrates an example of a system for bio-ester production and separation designed using this model.

Finally, the energy efficiency of the process was determined and compared to a benchmark to justify ongoing research and development. The HED-ISPR system has proven to be energy efficient; the energy footprint for the HED-ISPR does not exceed the combustion heat of the target product. For fuels, this means that the energy input into the system should not exceed approximately 20% of the HHV for that fuel to avoid gross energy inefficiencies. ASPEN modeling confirmed that the HED-ISPR system energy footprint was <20% of the HHV of the separated acids at a target concentration of >98% purity, meeting this target (Figure 12). Overall, the HED-ISPR system separated 98.5 mol% pure C<sub>4</sub> carboxylates from a live culture at a yield of approximately 95% of total butyric acid produced in the culture.

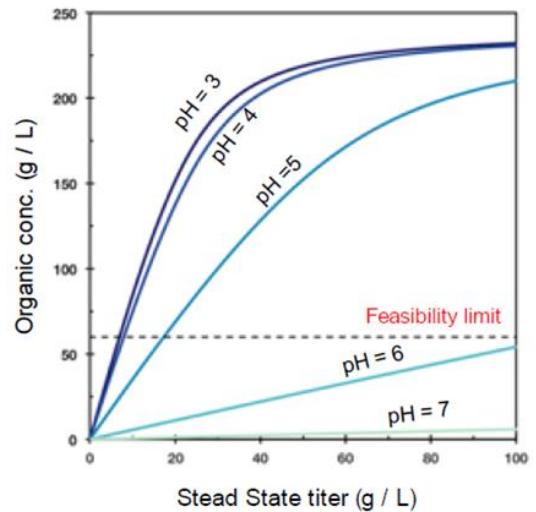


Figure 10 HED-ISPR equilibrium concentration of butyric acid in the organic phase as a function of pH and the initial acid concentration in the aqueous phase (i.e., steady state titer) (Saboe et al. 2018). The concentration in the organic phase must be >60 g/L to achieve a system energy footprint that is less than 20% of the carboxylic acid's higher heating value (HHV).

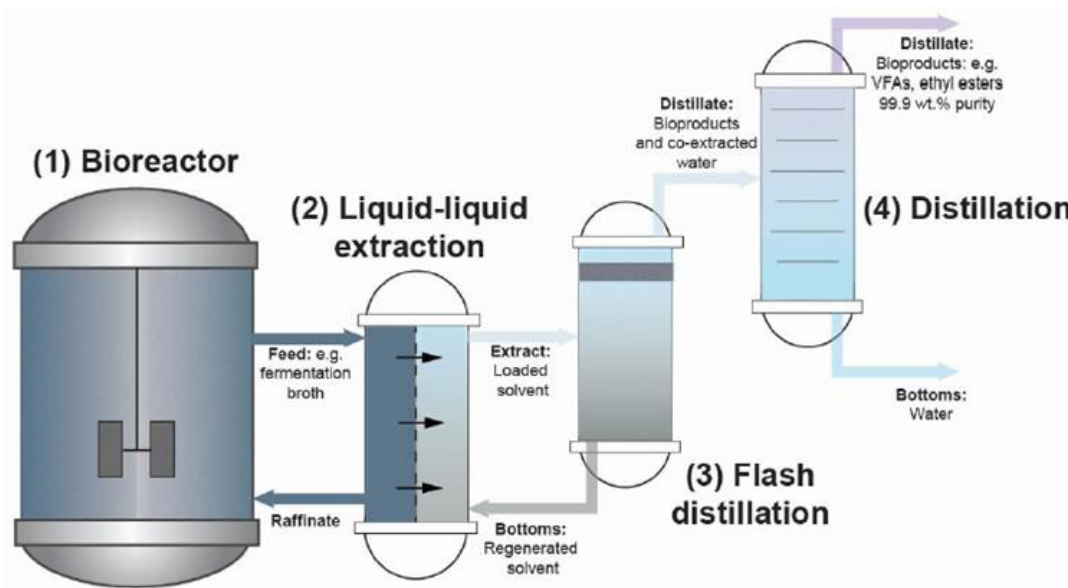


Figure 11 Bioreactor HED-ISPR for bio-ester production and separation (Saboe et al. 2019).

<sup>1</sup> MATLAB code used to generate Fig. 7, S7 and S15† is available on GitHub.com (NREL-SEP/CON/LL/Model\_ISPR – [https://github.com/NREL-SEP/CON/LL/Model\\_ISPR](https://github.com/NREL-SEP/CON/LL/Model_ISPR))

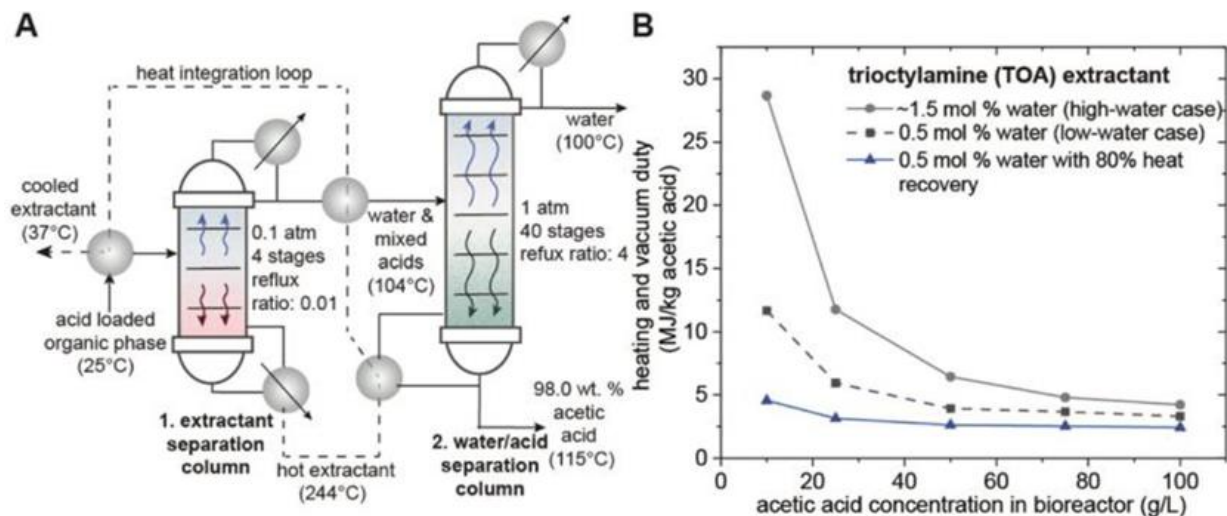


Figure 12 Trioctylphosphine oxide (TOPO) results: (A) Process diagram of acetic acid separation from extractant. In the first distillation column, extractant is easily separated from water and acid with four stages. A second column is needed to separate water from acid. (B) Energy input of the process per kilogram of acetic acid product as a function of acid concentration in the bioreactor at pH 3. As acid titer in the bioreactor increases, the energy input decreases. Increasing water content in the organic phase increases the energy input (Saboe et al. 2018).

**Results: EDI-ISPR.** The second approach to ISPR incorporated resin-wafer EDI rather than HED. In EDI, the target organic acids are directly captured by ion-adsorbent wafers. They are then extracted, converted, and concentrated without the use of solvent or acidification chemicals. Figure 13 illustrates EDI's ability to selectively capture the target carboxylic acid (butyric) at a constant concentration in the capture tank regardless of the remaining amount of acid in the fermentation broth. Overall, the energy demand was <1.0 kWh/lb acid, and more than 90% of the acid was recovered (Figure 13).

EDI-ISPR with modified resin wafers increased separation rates for acetic acid in a dilute aqueous solution 2.5 times above those achieved with conventional wafers. Energy consumption was simultaneously cut by 60%. Costs of carboxylic acid recovery were below the market price of these compounds.

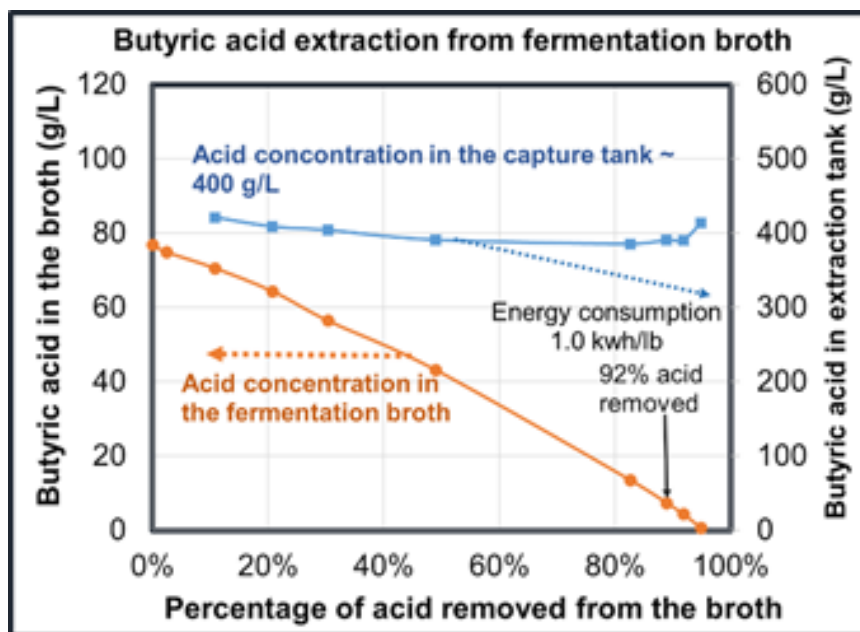


Figure 13 EC-ISPR acid recovery recovered 92% of butyric acid.

Further enhancing the separation efficiency requires improved resin wafer (RW) material. A new conductive ionomer binder was developed in the laboratory to replace the nonconductive polyethylene binder in the conventional resin wafer (RW/PE). A 2.5-fold increase in separation rates was achieved with the novel ionomer bound RWs in comparison to RW/PE (Figure 14). The right panel of Figure 14 is a preliminary experimental result for the EDI-based recovery of acetic acid extraction from mock aqueous solution using the new wafer material. As an example of property characterization for the new wafer material, the middle panel displays its enhanced conductivity as compared to RW/PE.

Compared to experiments using RW/PE, experiments using the advanced wafer material exhibited over 60% less energy consumption and a nearly 2.5x higher capture rate. The acid extraction performance shows a potentially significant reduction of the processing cost of EDI operation stemming from lower energy consumption and greater capture rates.

Integrated experiments with EDI-ISPR achieved >95% capture of the 65% yield (g/g) of C<sub>2</sub>/C<sub>4</sub> carboxylic acids from the fermenter broth with a total energy consumption of approximately <1.0 kWh/lb. During the 70-hour integrated fermentation-separation operation, adding a neutralization chemical (i.e., NaOH) was avoided due in-situ recycling of NaOH back to the fermenter. The captured carboxylic acid product titer was in the range of 180-250 g/L in pure acid form. This separation performance will enable organic acid capture with an approximate cost in the range of \$0.05-0.1/lb pure acid. Organic acids generally cost between \$0.5–2.0/lb., so this result is a promising indication of economic viability.

Remaining research and development includes evaluation of the new resin wafer material's stability in an actual industrial processing stream over a long period of operation. Furthermore, the EDI-ISPR system needs a robust techno-economic analysis (TEA); this work is planned moving forward. Notably, EDI utilizing a three-compartment configuration can recover NaOH in addition to separating butyric acid. Further enhancements in process cost and sustainability may be possible if EDI-ISPR is used to capture NaOH for reuse in the fermenter where it is critical for pH adjustment.

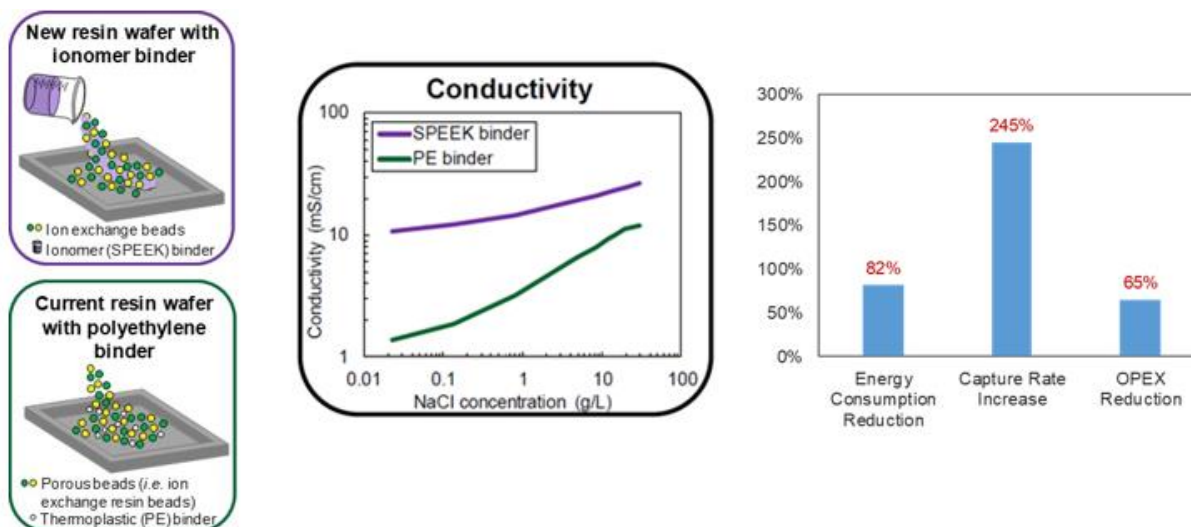


Figure 14 EDI membranes and performance for recovery of acetic acid from a dilute aqueous solution. Improvements in far-right figure are in comparison to RW/PE and demonstrate significant reduction in energy consumption with a 2.5-fold increase in capture rate.



### 4.1.3 Membrane-Sorbent Separations for Diol Recovery

**Motivation.** Organic acids are just one of the many products from fermentation; alcohol recovery is also important to industry and the BETO portfolio (Table 2). Distillation is often a standard separations approach for alcohols like ethanol. Heavier alcohols and diols, however, are not necessarily well-suited for distillation.

One diol of particular industrial interest is 2,3-butanediol (BDO). The Consortium has investigated new approaches to recover this diol from fermentation broth because current industrial methods for its recovery are energy-intensive, requiring multiple distillation stages at high temperatures. In addition, the process requires a hydrogenation reactor to decompose the oligomers produced at such high temperatures.

**Approach.** The new approach to BDO separations in the Consortium is to apply selective membranes that pull 2,3-BDO from the broth, which is a complex mixture of BDO, inorganic salts, proteins, and organic by-products that is more than 90% water. Such a high water content required a membrane to be developed (Figure 15a) that allows for highly selective, high-throughput permeation of water and targeted removal of impurities at low temperatures (e.g., 60–80°C).

**Results.** Membrane performance in separating BDO and water is shown in Figures 15b and 15c: The hydrophobic membrane achieved a separation factor (SF) of over 15 with a flux 0.4 liters per hour per square meter (L/hr/m<sup>2</sup> or LMH) at a very mild vacuum pressure (5 in. Hg). In addition, newly synthesized superhydrophilic membranes achieved an even higher SF of approximately 160, with a higher flux of 0.7 LMH. Both SF and flux of the superhydrophilic membranes are 7 times larger than literature state-of-the-art results (Xu et al. 2018; Shao et al. 2009).

Newly developed superhydrophilic membranes exceed state-of-the-art separation factor and flux by 7 times.

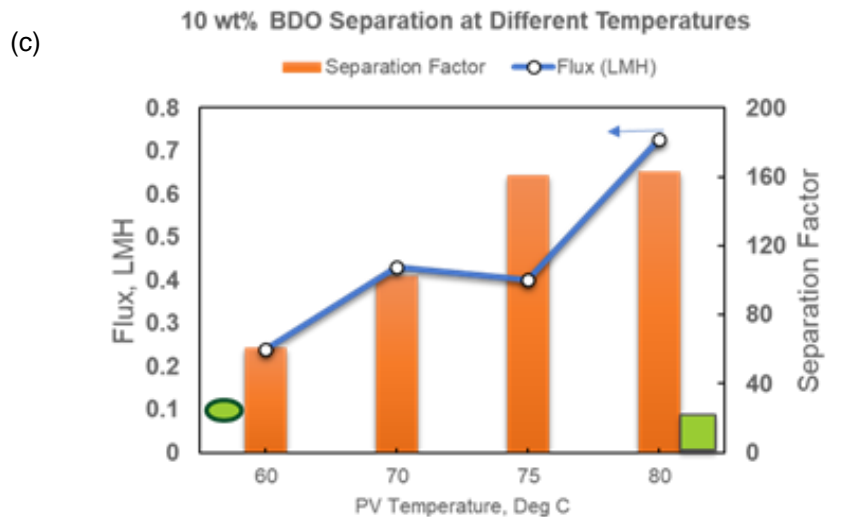
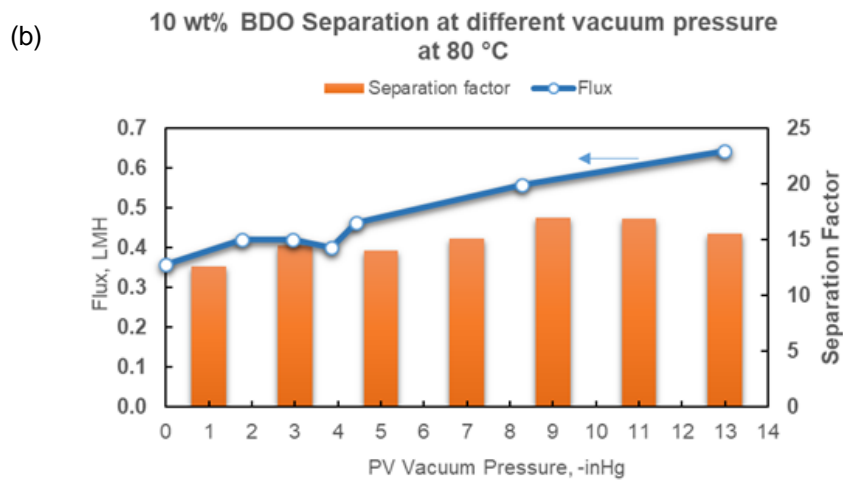
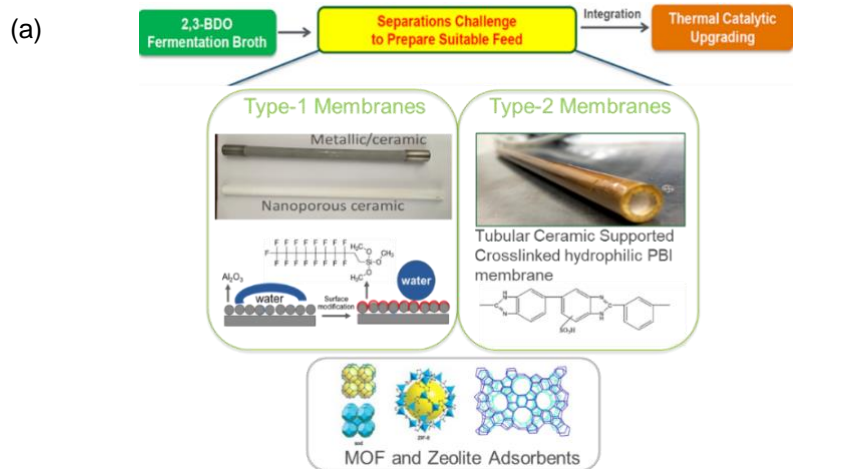


Figure 15 (a) Pervaporation membranes and sorbents evaluated for BDO separations; (b) Type-1 hydrophobic membrane performance at different vacuum pressures; (c) Type-2 superhydrophilic membrane performance at different temperatures. These results demonstrate that the separation factor and flux of the superhydrophilic membrane are seven times the state-of-the-art (green spots) based on literature data (Xu et al. 2018; Shao et al. 2009).

In addition to enriching BDO, sorbent materials, including mordenite framework inverted-structured zeolites and zeolitic imidazolate frameworks tested in parallel with membrane pervaporation, have shown the potential to selectively separate BDO from catalyst coking molecules such as glycerol, acetoin, or sugars. The enriched, purified BDO stream serves as suitable feed to catalytic upgrading reactors to ultimately achieve better BDO conversion to fuels and chemicals at a lower cost. This will be quantified through analysis.



#### 4.1.4 Ultrasonic Separation of Lignocellulosic Particles

**Motivation.** In biochemical processes that utilize lignin, fine particles foul equipment and impede lignin conversion. Ultrasound is one technology that could be used to remove lignocellulosic fines because standing acoustical waves concentrate particles at regularly spaced nodes (Figure 16). Particulates aggregate into larger entities and eventually precipitate out from solution.

Key research questions in the application of ultrasound to removal of lignocellulosic fines included whether particle size was in the range that works well for ultrasonic separations and how much energy is required to separate lignocellulosic fines using ultrasound.

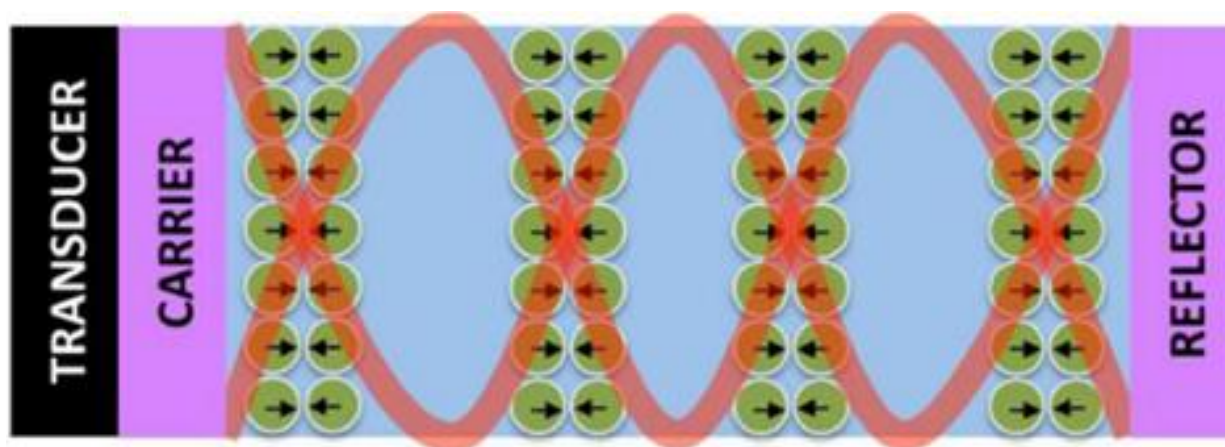


Figure 16 Ultrasonic separation conceptual illustration. Energy is applied to a system, generating a standing acoustic wave. Lignocellulosic fines concentrate at the nodes of waves and then precipitate.

**Approach.** Tests were carried out to establish energy requirements for a reference suspension of lignocellulosic particles using the experimental setup shown in Figure 17. To acquire sufficient volumes of suspended fines, washed alkali deacetylated corn stover was obtained from LBL, wet milled, and resuspended in water at a concentration of  $0.56 \pm 0.03$  g AFDW/L, where AFDW is ash free dry weight. Tests were carried out in two distinctly different operating modes: (1) a baseline mode representing current industry practice, and (2) a proprietary low-energy approach.

**Results.** Agreement was observed between quiescent batch and flow tests, which indicates that hydrodynamic drag forces did not impair performance under the conditions tested. Hydrodynamic effects, however, become apparent when the feed flow rate is too high and entrained solids are swept out of the vessel. Based on the fraction of fines removed in Figure 17 (~50%), it is likely that a significant portion of the milled fines in the reference suspension are too small for ultrasonic removal.

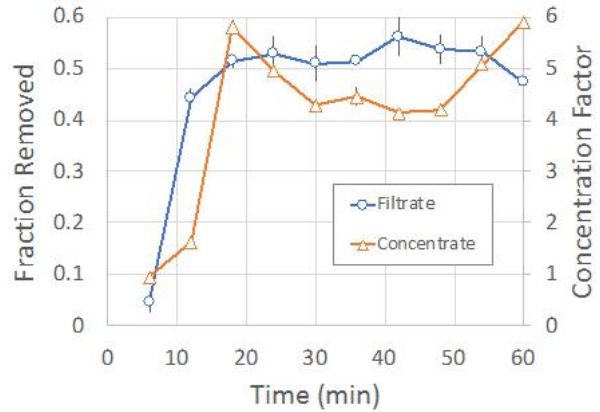
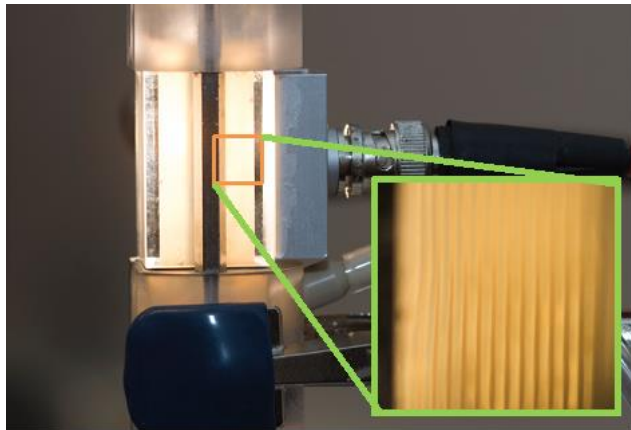


Figure 17 Left: Ultrasonic experimental setup showing fines concentration in the standing wave. Right: Experimental results of fines removal in continuous flow. Fines in both filtrate and concentrate streams reach near-steady-state concentrations after the first 20 minutes.

In order to assess the viability of ultrasonic technology for the separation of lignocellulosic particles, the energy required to remove lignocellulosic fines is compared to their energy content in Figure 18. The energy content serves as a general reference for fines suspensions and is calculated by assuming a HHV value of 17 MJ/kg AFDW. The relative energy costs, indicated by red and blue lines in Figure 18, display a minimum and illustrate that maximum fines removal comes at a higher fractional energy cost. The minimum can span a range of costs, but it generally corresponds to 40–60% of removable particles.

Although both operating modes are in the same energy band as centrifugation (i.e., 1–5 kWh/m<sup>3</sup>), the Consortium-developed mode removes more fines than conventional operation at a fixed energy input. The energetics shown in Figure 18 also serve as a master curve for lignocellulosic fines removal and can be diagonally shifted to obtain first-order performance estimates for suspensions with different concentrations of fines. For example, a suspension twice as concentrated as the reference suspension should yield twice the fines removal at the same energy input. By shifting the data at constant energy input until twice the removal is indicated, the performance curve at the more concentrated condition can be approximated.

Consortium-developed ultrasound technology can be more efficient at fines removal than conventional ultrasound technology.

However, the master curve paradigm does have limitations. First, at some point adding more particles to the feed suspension will start to degrade performance. Second, the paradigm fixes performance in the centrifugation energy band while lower energy bands are theoretically attainable. The energy band is determined by the test vessel used in this study and was optimized given the vessel constraints, but it is still relatively inefficient. Vessels capable of shifting the performance band to lower energies are on hand at LANL but require significantly more material for testing.

Although lower energies are theoretically attainable, they are likely within an order of magnitude of the results shown. This master curve approach provides insights useful for TEA in terms of estimating particle removal as a function of energy input under these two operating scenarios. However, it does not address the uncertainty originating from particle loading and energy band limitations.



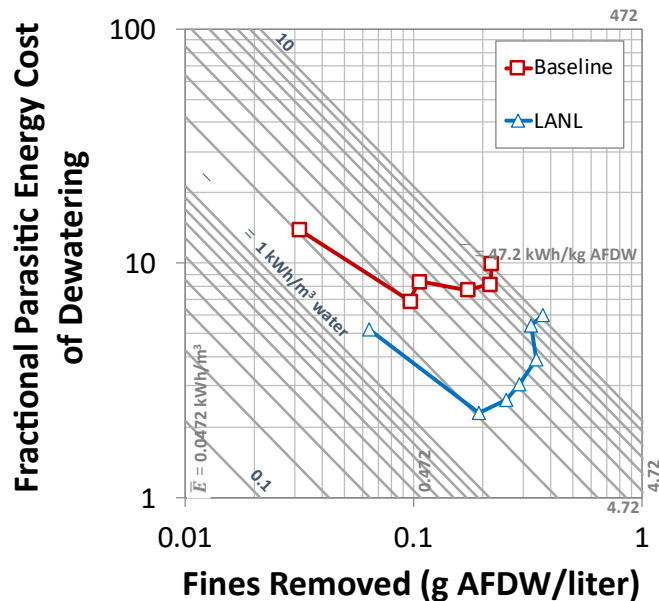


Figure 18 Vessel-limited energetics of cellulosic fines removal using ultrasonic filtration in baseline and LANL operating modes. The diagonal lines indicate the energy input per volume of suspension. Vertical and horizontal lines are referenced to the HHV of 17 MJ/kg to indicate the energy content of the removed fines and the energy input per unit mass of fines removed, respectively. The same feed suspension was used in both sets of tests shown. Additional fractional energy improvements require vessel optimization.



#### 4.1.5 Recovery of NaOH and Lignin Products

**Motivation.** EDI is well-suited to recover charged species, including NaOH used in homogeneous lignin depolymerization. Recovery and reuse of NaOH avoids consumption of fresh NaOH in the process that incurs cost and environmental impacts.

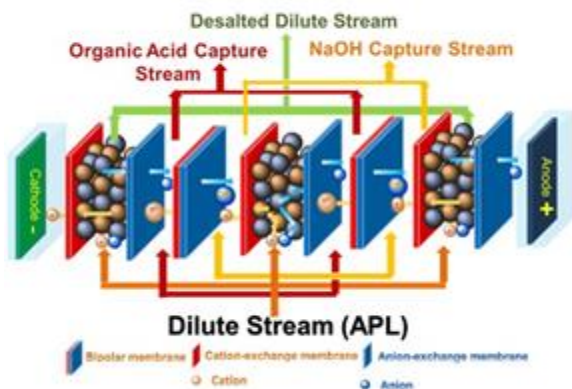
**Approach.** EDI (Figure 19) was selected as the separations technology to recover NaOH because it has a unique capability to separate charged species from aqueous solutions. Please see Section 4.1.2 for more information about the EDI experimental apparatus.

**Results.** EDI recovered 99% of NaOH and 95% of carboxylic acids at a 35–40 wt% concentration (Figure 19). The cost of recovering NaOH is lower than the cost of NaOH used in TEA of bioprocessing (\$0.52/kg). This result is promising; however, the EDI

The cost of recovery of NaOH with this EDI approach is lower than the cost of NaOH used in TEA of bioprocessing (\$0.52/kg).

process must be integrated into an overall process model to fully evaluate the benefits and drawbacks of its application. Accordingly, this approach was initially integrated in the preliminary TEA of biochemical conversion of hydrolysate sugars to hydrocarbon fuels via short-chain carboxylic acid intermediates. Data gaps that must be addressed to fully evaluate EDI in this application include the need for improved adsorption material to capture and extract acids from lignin and to purify the acids and bases after capture.

### Three-compartment Electrochemical Separation Device



### Simultaneous Capture of Carboxylic Acid and NaOH from APL

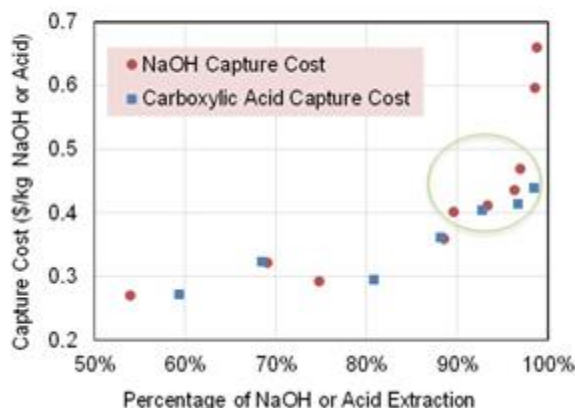


Figure 19 Left: EDI concept. Right: acid base separation results. EDI recovered 99% of NaOH and 95% of carboxylic acids at a 35-40 wt% concentration. NaOH was captured at a cost below the market price used in techno-economic analysis (~\$0.52/kg).



## 4.1.6 Economics and Sustainability

Within the Biochemical Separations Team, acid recovery is a common theme because acids are important as intermediates in the production of biofuels and as valuable products themselves. Analysis for biochemical separations therefore focused on acid recovery strategies, undertaking process modeling for three possible acid recovery techniques.

The baseline process was a simulated moving bed (SMB) system. Other strategies—EDI and pertractive separation—were compared to SMB. EDI was assessed within the context of a pH 7 fermentation, with the intent of later assessing lower pH cases. The third process was pertractive separation integrated with low-pH fermentation. The processes, shown in Figure 20, were modeled within the context of a conceptual commercial-scale biorefinery using a biochemical design case as the framework (Davis et al. 2018).

The preliminary TEA results show the relative cost results compared to the baseline (Figure 21). Note that these costs assume that lignin is burned for power; lower fuel production costs can be achieved through the conversion of lignin to chemicals.

Pertractive technologies (HED-ISPR) showed the lowest overall MFSP. One driver of this result is higher targeted yields (at 100%), and low raw material make up (i.e., salt wastes) because of the low-pH fermentation and limited electricity demand in this case.

Analysis results demonstrated that Consortium-developed technologies of pertractive separations and EDI applied to acids separations in biochemical processes offered opportunities for reduced cost and enhanced sustainability as compared to off-the-shelf simulated moving bed technology.

In this separations approach, the liquid membrane results in less solvent loss. The EDI approach was more expensive than the pertractive approach, primarily because the yields of recovered acid were lower (at 95%) and greater energy consumption. Because EDI does not require low-pH fermentation as modeled, EDI could potentially be a mitigation strategy that may perform better than HED-ISPR in the anaerobic acids pathway. HED-ISPR requires a fermentation step that operates best at lower pH. Some organisms, however, cannot tolerate  $\text{pH} \leq 5$ . In those cases, EDI-ISPR is a better technology solution.

The cost results were reviewed by the IAB and were included HED-ISPR was adopted for the acid pathway in the *FY 2018 Biochemical Design Report* (Davis et al. 2018).

Using the material and energy flows from the process modeling that informed the TEA, lifecycle analysis (LCA) was carried out using corn stover as a feedstock to estimate lifecycle greenhouse gas (GHG) emissions and water consumption. Compared to the SMB technology, EDI and pertractive separations exhibit lower life-cycle GHG emissions of the renewable diesel product produced by the biorefinery (Figure 22). Lower yields in the SMB case is one underlying factor of these results. Another key driver of GHG emissions in conversion (represented in the fuel portion of the biofuel lifecycle) is NaOH consumption used during biomass deconstruction.

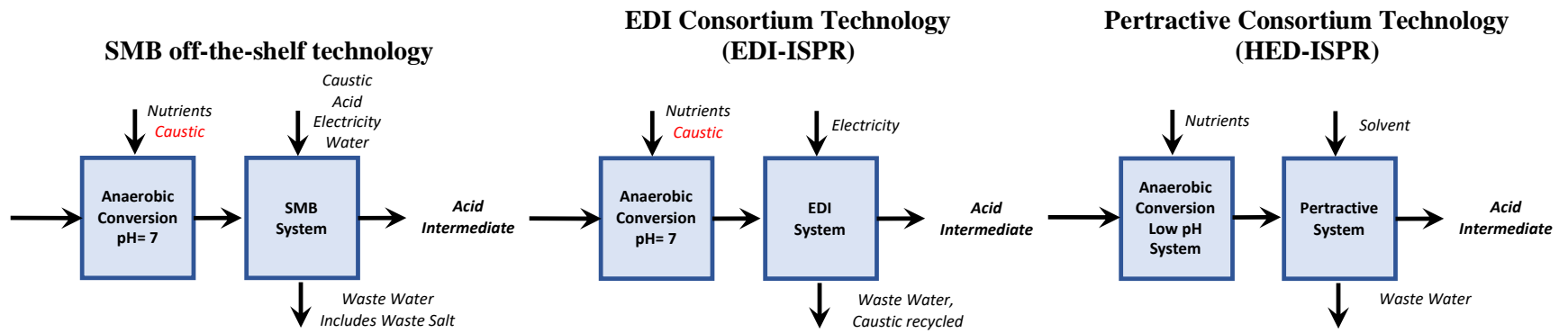


Figure 20 Box flow diagram for SMB, EDI-ISPR, and pertractive (HED-ISPR) separations.

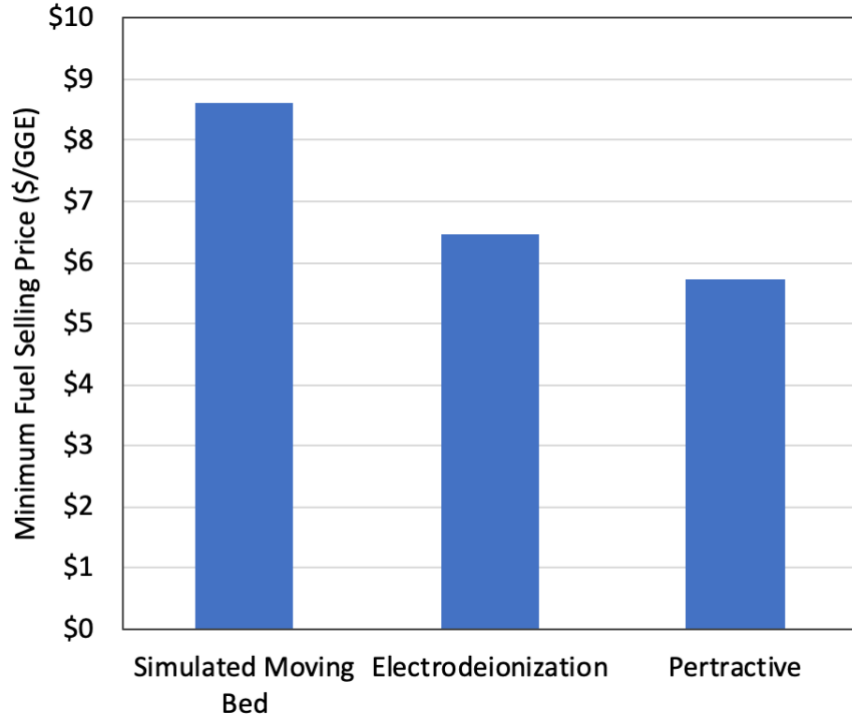


Figure 21 Separation costs for SMB, EDI, and pertractive technologies for an example biorefinery configuration (Davis et al. 2018). In this configuration, lignin is burned in a boiler; lower MFSP results are possible by alternative routes upgrading lignin to value-added coproducts.

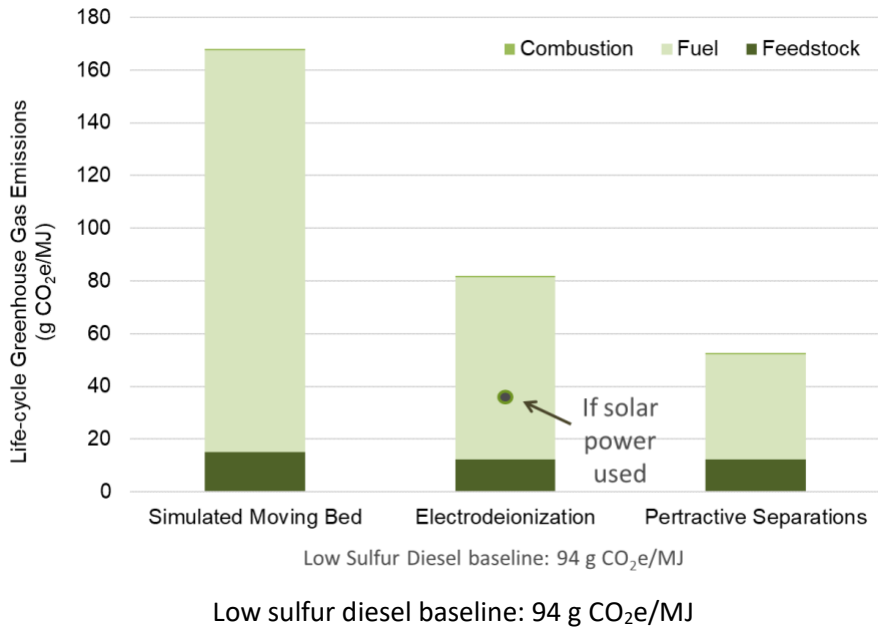


Figure 22 Lifecycle GHG emissions for SMB, EDI, and pertractive technologies. Emissions for EDI are lower than that of both alternatives if solar power is used.

Life-cycle water consumption was also estimated for the three separations approaches (SMB, EDI, and pertractive separations) that could be used in the production of the acid intermediate (Figure 23).

As for GHG emissions, the low yield in the SMB case resulted in more water consumed per MJ fuel than in the other cases. The SMB case also consumes more chemicals, such as  $H_2SO_4$ , to regenerate the resin in the moving beds.

Overall, the pertractive approach to separating the acid intermediate is most promising from a cost and sustainability perspective if a low-pH fermentation can be achieved. If this is not feasible, the EDI approach outperforms the SMB approach.

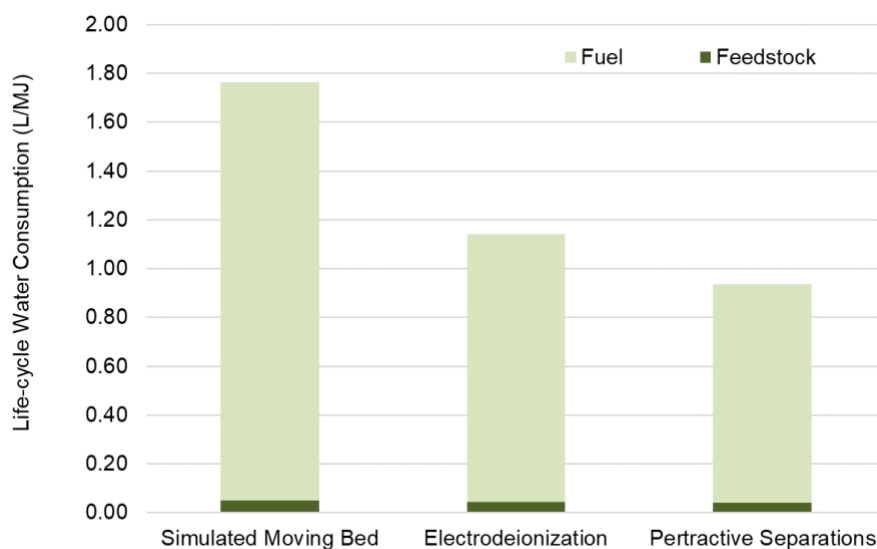


Figure 23 Life-cycle water consumption (L/MJ) in the production of renewable diesel through an acid intermediate.

### 4.1.7 Industrial Relevance

The Consortium seeks to advance the understanding and performance of existing and new separations technologies towards solving industrially relevant separation problems. Table 3 summarizes the Consortium technologies with respect to organic acid and alcohol recovery from biological reactor system broths, and lignin fractionation and recovery.

Table 3 Industrial relevance of separation technologies applicable to biological conversion processes.

Separation technology	Current applications	Potential applications	Current Scale	Projected future scale	Types of compounds	Advantage over other technologies	Remaining gaps
HED-ISPR	Organic acid recovery from fermenter broth	Organic acid separation from aqueous streams. Carboxylic acid recovery from aqueous HTL. Carboxylic acid recovery from aqueous catalytic fast pyrolysis stream.	~100–400 g	4–10 kg	Organic acids/ carboxylic acids	ISPR allows amelioration of end-product inhibition increasing bioprocess titers rates and yields. Lowers water footprint of system ~10-fold.	Integrate distillation system directly to extraction loop for full proof of concept.
EDI	ISPR organic acid recovery from fermenter broth; lignin, and NaOH recovery from aqueous streams.	Acid and base recovery from aqueous streams. Organic acid separation from aqueous streams. Carboxylic acid recovery from aqueous HTL. Phenolic acid capture from APL. Biogas upgrading.	5-20 g/hour (250 gallons/day) at the bench scale	1-10 kg/hour (>5,000 gallons/day) at the field-pilot scale	Organic acids/ inorganic acid & base/ ammonia	Enable continuous fermentation without neutralization. Produce >30 wt.% pure organic acid capture without the use of solvent or acidification chemicals.	Full assessment of EDI technologies' costs and potential to reduce overall processing costs.
Ultrasonic	Lignocellulosic fines; microalgae and bacteria culture harvesting; protein suspension dewatering.	Organic/inorganic particle suspensions; liquid emulsions; molecular separation via adsorption.	A range of scales available. Suspension or emulsion flow rates vary from around 100–500 mL/hr for the smallest vessel, up to 18 L/hr for the largest.	Larger scales accessible via multiple modular designs.	Phase-separated particles or aggregates from ~1–100 $\mu\text{m}$ . Particle density must deviate from the media density.	Acts as a membrane-less filter, avoiding chemical cleaning and backflush operations. No chemical additives. No moving parts.	TEA of an integrated ultrasonic separator.

Table 3 (Cont.)

Separation technology	Current applications	Potential applications	Current Scale	Projected future scale	Types of compounds	Advantage over other technologies	Remaining gaps
Pervaporative Membrane and Distillation	Higher alcohol recovery from fermentation broth	Molecular enrichment of various aqueous solutions, including organic acids, alcohols, diols, and other oxygenates.	0.1–1 L	1–10 L	Organic acids/ carboxylic acids.	Less energy intensive, lower cost.	Advancement of selectivity, flux/capacity, and stability of separation materials (membranes and sorbents)
Polymeric Membrane	Lignin molecular weight fractionation, cell and debris removal from fermentation broth, protein or biopolymer purification and recovery	Biopharmaceutical manufacturing, enzyme production, bacteria removal, gas separation, and wastewater treatment	100 mL to 600 L	>1,000 L	Biofuels and bioproducts such as protein, enzymes, bipolymer or fuel molecules ranging from 150 Da to 700 KDa	High selectivity, reusability	Membrane fouling, surface area and pump capacity need to be increased
Ceramic Membrane	Lignin molecular weight fractionation; cell and debris removal from fermentation broth	Filtration of crude extracts and biomass pretreatment streams; color removal depolymerized stream filtration; filter sterilization; pretreatment for SMB process; solvent recovery	1–10 kg	Current pilot plant units are ~1,000–10,000 kg of solution filtration (throughput)	Aqueous streams and oil-based streams. Depolymerized materials. Solvent purification.	Low energy, durable with high up time, can be implemented in rotating units for high uptimes.	Cleaning cycles need to be defined, energy analysis has never been performed, color removal pore sizes need to be defined.



Table 3 (Cont.)

Separation technology	Current applications	Potential applications	Current Scale	Projected future scale	Types of compounds	Advantage over other technologies	Remaining gaps
SMB	Lactic acid purification (Cargill); commodity chemical purification; natural product purification	SOT for purification of molecules from complex mixtures	NREL 1–10 kg of purified product. Industrially millions of kilograms/day scale (e.g., paraffin separation from gasoline)	Operates today at 21,000 t/yr to 1,6000,000 t/yr and possibly larger scale	Low-molecular-weight organic compounds	Continuous, lower solvent load than column chromatography, energy efficient, can apply to almost any separation, allows separation of many molecules that cannot be separated by distillation.	High cost of stationary phase, solvent recovery operation rarely factored into analysis of technology, middle cuts can be challenging, generally limited to A/B separations, resin fouling can require extensive upfront filtration.

## 4.2 Thermochemical Separations

Thermochemical processes cover a wide range of methods and applications. However, a common problem is catalyst fouling and premature deactivation. Another challenge shared with biological conversion processes is product recovery from dilute aqueous streams. The thermochemical separations challenge areas of Consortium research are illustrated in Figure 24.

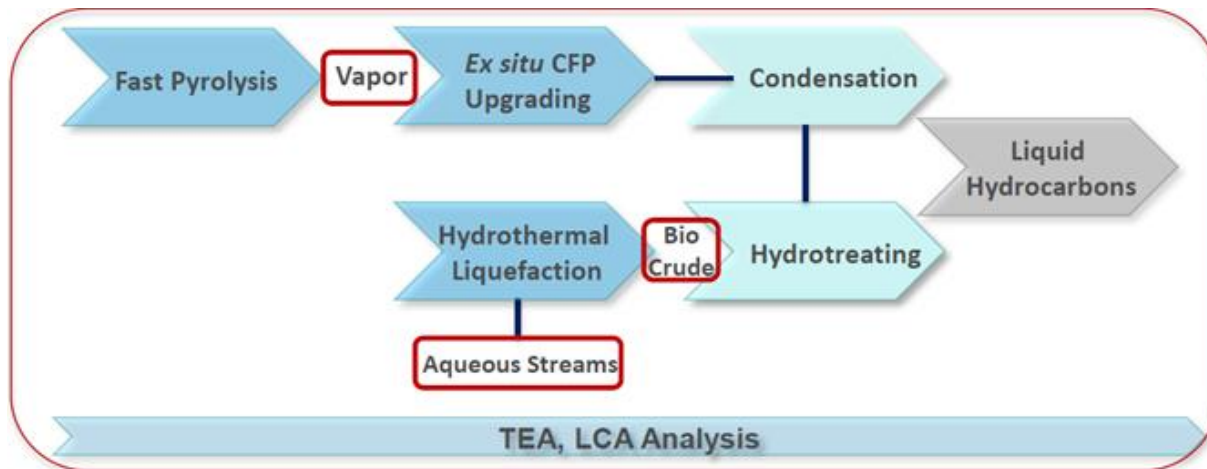


Figure 24 Separation challenges for two types of thermochemical processes.

Catalyst longevity is a key driver of TEA results for thermochemical processes. A key barrier to increased catalyst longevity is the presence of toxins in processing streams that deactivate the catalyst. Furthermore, aqueous streams formed in thermochemical processing can contain potentially valuable carbon species that could be recovered to improve process economics. Finally, the benefits of process intensification in thermochemical processes have been subject to exploration within this area of the Consortium.



### 4.2.1 Catalytic Hot Gas Filtration (CHGF)

**Motivation.** Biomass fast pyrolysis vapors contain char, alkali aerosols, and carbonyls. These impurities destabilize the bio-oil vapors fed to upgrading catalysts. They also destabilize the condensed vapors that are further upgraded over fixed bed catalytic reactors. These compounds also poison catalysts.

A Consortium project investigated CHGF both to trap inorganic material and to convert small organics into material that is easier to upgrade. The use of a CHGF downstream of a fast pyrolysis reactor is based on the premise that hosting catalysts within an HGF system can reduce capital costs by eliminating one or more reactor systems that would otherwise host the catalyst. The greatest benefits of CHGF can come from increased organic liquid-range yields and improved carbon efficiency via coupling chemistry to prevent carbon losses to the gas phase. Downstream catalytic reactors can benefit from the ease of catalyst maintenance and can be further tailored towards selectivity improvements for better quality fuels and valuable coproducts.

Previous sensitivity studies have quantified the impacts of these changes (Dutta et al. 2018) including on capital costs, carbon efficiency, catalyst maintainability, and cost savings from reduced oxygen content in the pyrolysis oil.

**Approach.** Figure 25 illustrates the CHGF research apparatus setup in which the industrially available Pall ceramic filter is (a) housed in a metal holder; the filter can be (b) coated with catalyst or (c) packed with

particulate catalyst in its interior. The right panel in Figure 25 shows the placement of the CHGF unit between the biomass pyrolyzer and the liquid product condensation train. Alternatively, clean vapors can be supplied to the DCR upgrading unit for catalytic conversion to fuels and chemicals.

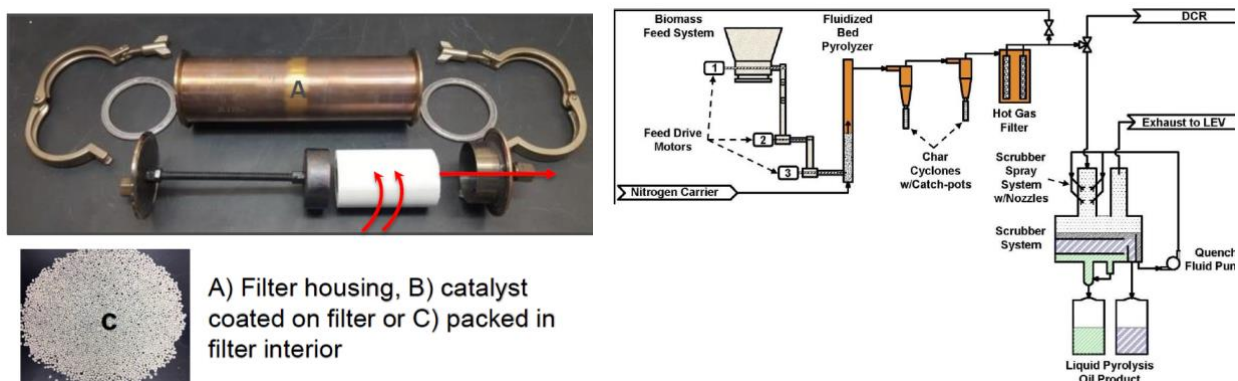


Figure 25 Hot gas filtration experimental setup (Peterson et al. 2019).

**Results.** The biomass type and catalyst type both affect the catalytic pyrolysis vapor composition. This composition in turn affects downstream catalyst lifetime and oil stability. Research into biomass composition effects on pyrolysis vapor composition determined that vapor from pyrolysis of pine and pine residues exhibited similar responses to reaction over zeolites. Acetic acid in these vapors was converted to acetone, which is easier to upgrade, when doped carbides (Lu et al. 2018) and  $\text{CeO}_2$  were used as catalysts. Furthermore, the ceramic hot gas filter removed >99% char and alkali from the pyrolysis vapor (Figure 26), particulates that if left in the vapor enhance coking and organic cracking. In addition, the removal of heavy vapor components, such as benzene, toluene, xylene (BTX), anthracenes, and naphthalenes, reduces the carbon losses to upgrading catalyst coking.

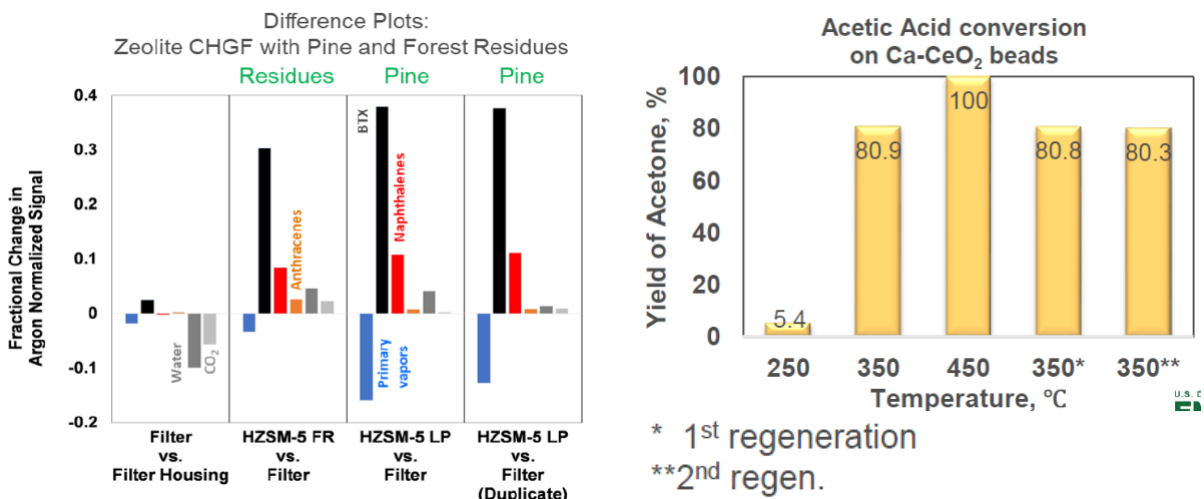


Figure 26 Filtration and conversion results for various filter materials and catalysts (Peterson et al. 2019).

The process was intensified by adding  $\text{CeO}_2$  and zeolite catalysts to the interior of the filter to convert unreactive oxygenates to upgradable components, thereby increasing carbon conversion to products. Overall, tuneability of the vapor chemistry was demonstrated using an industry-accepted filter along with catalyst sorbent performance, lifetime, and regenerability.

Another alternative, a titania-supported molybdenum heteropolyacid (Mo-HPA/TiO<sub>2</sub>) catalyst, was developed in FY 2019 to target further improvements in fast pyrolysis vapor quality. The HPA catalyst demonstrated vapor hydrodeoxygenation by reducing the concentration of reactive species such as sugars and acids, alkylation activity allowing the conversion of lighter molecules to liquid range products, and reduced carbon losses to the aqueous phase (Peterson et al. 2019). In summary, the catalyst's performance was promising. However, the greatest challenge of this approach lies in the development of an efficient HPA catalyst regeneration method within the environment and operating protocols of the HGF system.

Catalysts tested for CHGF exhibited promising performance in removing or converting catalyst foulants. To realize these benefits, it is essential to develop an HPA catalyst regeneration method.

Typically, continuous operation of HGF systems involves regular blowback to remove particulates. Blowbacks are short gas flow pulses in the reverse direction of process flow. They help dislodge solid material the filter candle traps. Short pulses will allow efficient regeneration only if the catalyst on-stream time is at least an order of magnitude or longer than the regeneration time. Longer regeneration times, as exhibited in the current state of technology, will require significant spare capacity in the filtration system.

The requirement for this spare capacity defeats the premise that a CHGF reduces capital costs. Thus, future research should focus on quicker catalyst regeneration and longer catalyst on-stream times to help reduce the requirement of spare CHGF capacity during continuous operation.



#### 4.2.2 EDI-Based Recovery of Dilute Organic Carbon and Ammonia in the Aqueous Phase

**Motivation.** The hydrothermal liquefaction (HTL) aqueous phase, and to a much lesser extent, the catalytic pyrolysis aqueous phase, contains a significant amount of organic carbon, much of which is in the form of organic acids. If the organic acids in the aqueous stream are recovered, their sale can offset some of the cost to produce biocrude.

**Approach.** EDI (Figure 27) was applied to the HTL aqueous stream to evaluate its potential for acid recovery and, as described later, ammonia recovery. By applying EDI, organic acids were recovered as a single product stream. At high concentrations of recovery, the costs to recover acids and ammonia using EDI alone becomes prohibitive. To achieve greater acid concentration, membrane-based techniques were explored following EDI.

**Results.** EDI was implemented in a three-compartment configuration to recover ammonia in a separate mixed alkaline stream (Figure 28). As shown, organic acids and ammonia were continuously removed from the fermentation broth and transferred into separate acid and base product streams. Regardless of the percentage removal (x-axis), high concentrations of acid and base were continuously extracted into the product streams (y-axis). For comparison, the target levels of acid and ammonia concentration in the acid and base streams are indicated by the horizontal blue and green lines, respectively.

EDI-based separations maintained high concentrations of acid and NH<sub>3</sub> regardless of the percentage removal. Concentrations of each species exceeded the target levels.

The results from testing with acid surrogates (Figure 29) indicate >50wt% acetic acid concentration is possible when a HiPAS membrane (Lu et al. 2019) is applied following EDI. HiPAS membranes are made of modified polymer coated ceramic tubular supports. They can be operated continuously at high temperatures, and they both are acid-resistant and scalable.

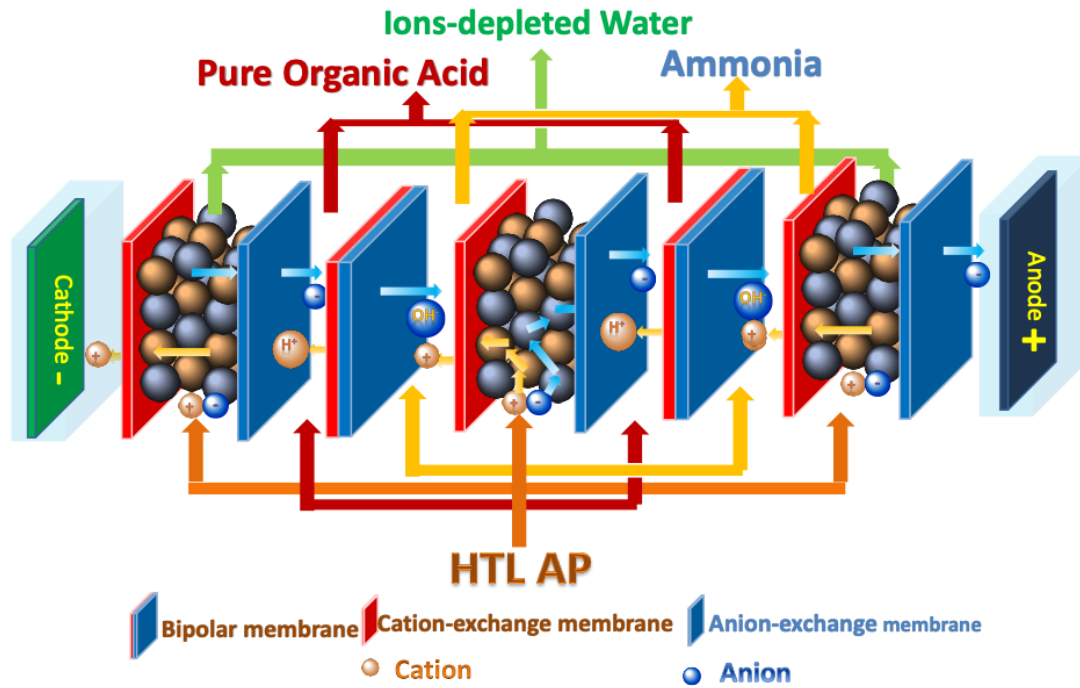


Figure 27 Selective extraction of dilute organic acids from the thermochemical (TC) waste aqueous phase using the EDI platform system.

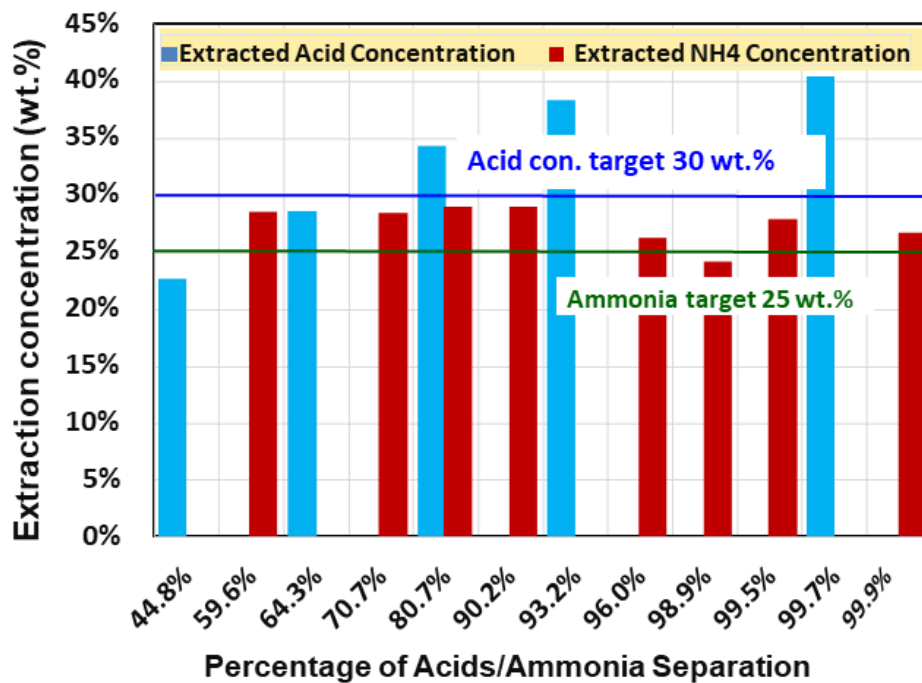


Figure 28 EDI results for acid and ammonia recovery from HTL aqueous phase. The concentration of acid and ammonia each exceeded the target concentrations.

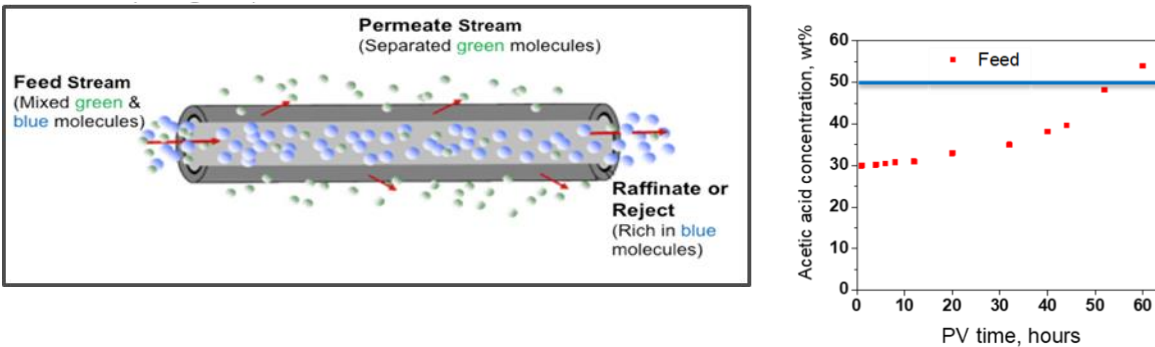


Figure 29 Left: HiPAS membrane concept. Right: Acetic acid concentration over time in permeate stream as a result of pervaporation (PV). The target concentration was exceeded after 50 hours.

Development gaps include the need to separate the mixed acid stream into individual components, which would add cost, and to purify the ammonia stream by removing sodium and other contaminants. In addition, the recovery of non-ionic species, such as alcohols in the aqueous stream, could potentially add value (Hu et al. 2018).



### 4.2.3 Removal of Ammonia from HTL Aqueous Streams as a Wastewater Treatment Option

**Motivation.** In addition to acids, HTL aqueous streams also contain dissolved ammonia. This presents a costly problem if the ammonia has to be removed prior to downstream use or before the aqueous stream can be recycled (Figure 30). Recovering ammonia can eliminate the cost to treat the aqueous stream prior to recycling when the wastewater treatment plant (WWTP) has nitrogen restrictions. In addition, ammonia could provide another revenue source for the biocrude plant. Figure 30 illustrates the flow sheet, showing EDI as part of the biocrude production pathway.

**Approach.** Experimental results from Section 4.2.2 were applied in TEA and LCA to evaluate the benefits of ammonia removal with EDI for reducing ammonia concentrations to levels allowed at wastewater treatment plants. These levels vary by location; in some cases, there is no restriction on ammonia levels and removal is unnecessary.

**Results.** Preliminary TEA results that evaluate EDI's viability to remove ammonia cost effectively are shown in Figure 31. When the EDI process is used—at 90% ammonia recovery, 30% ammonia concentration, and no impurities—the selling price for the finished (hydrotreated) fuel is below the design target. Similarly, assuming a discounted value for mixed acids (as opposed to separated and purified acids), it is possible to reach the cost target (Figure 31).

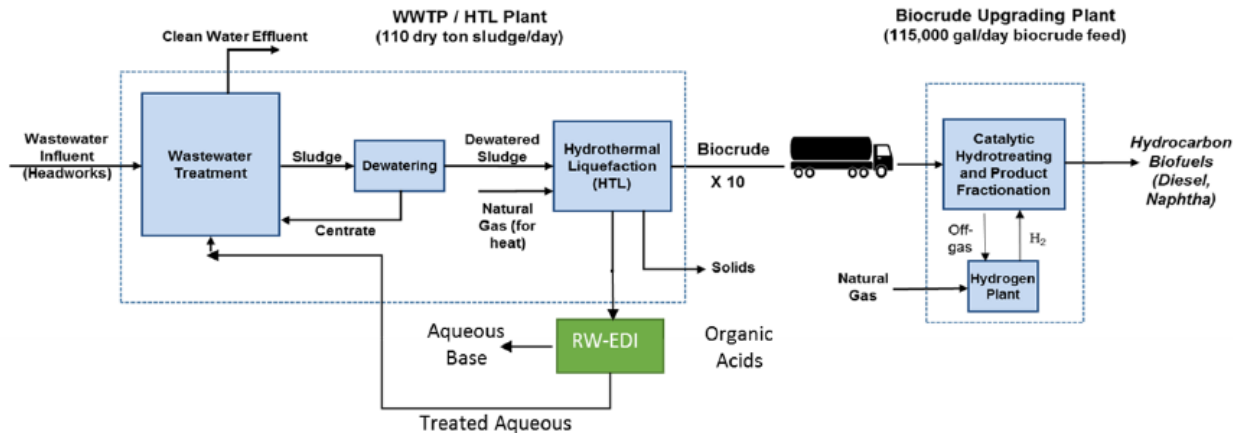


Figure 30 Waste HTL flow diagram.

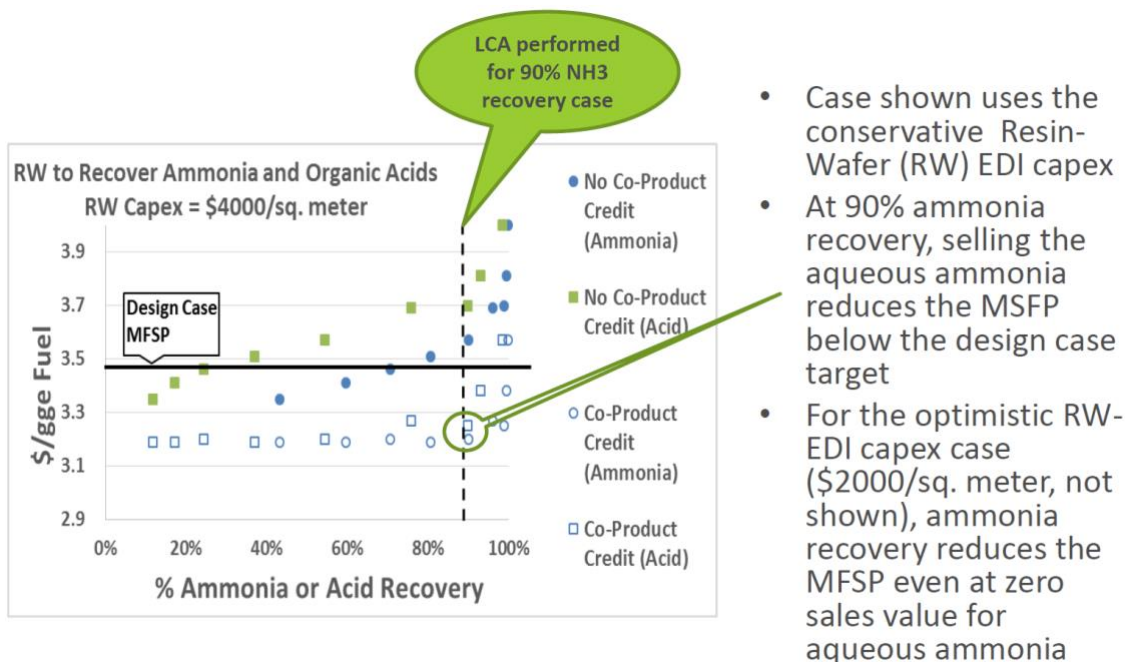


Figure 31 Potential cost reduction through use of EDI for acid and base recovery from HTL aqueous phase.

The preliminary LCA (Figure 32) was completed assuming ammonia and acid coproducts are recovered. In the case of acids, acetic acid was adopted as the type of acid that would be sold as a coproduct. It was assumed that no energy or materials were consumed to separate and purify the acetic acid. The EDI case in Figure 32 is then a best-case result. If, however, there were no displacement credit for acetic acid, the EDI case would still outperform conventional NH<sub>3</sub> removal.

Fossil fuel consumption shown in Figure 33 is lower for the EDI case than for the conventional ammonia removal case. Again, these are preliminary best-case scenarios because energy, emissions, and water associated with separating acid coproducts are not yet included.

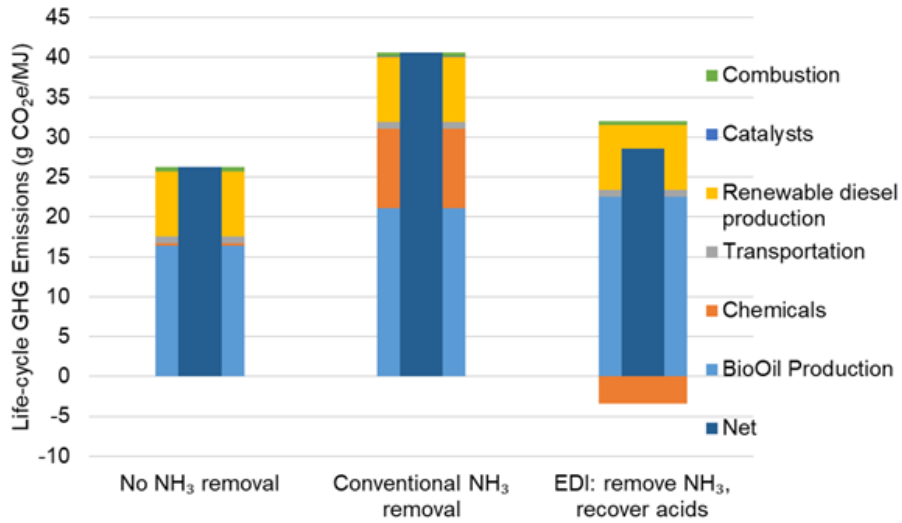


Figure 32 GHG reduction for EDI-based recovery of mixed acids and ammonia from HTL aqueous phase.

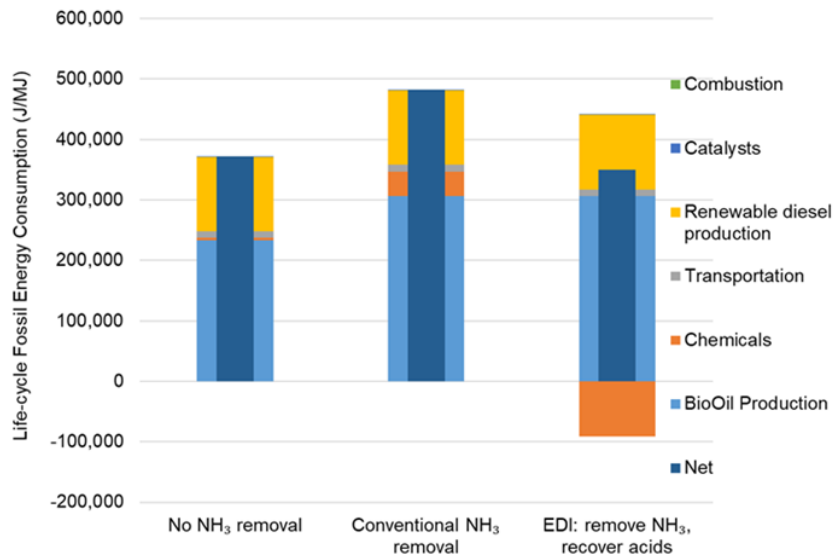


Figure 33 Fossil energy consumption for EDI-based recovery of mixed acids and ammonia from HTL aqueous phase.

Water consumption was also less compared with the conventional ammonia removal case (Figure 34). In the conventional case, quick lime (CaO) consumption mainly drives water consumption.



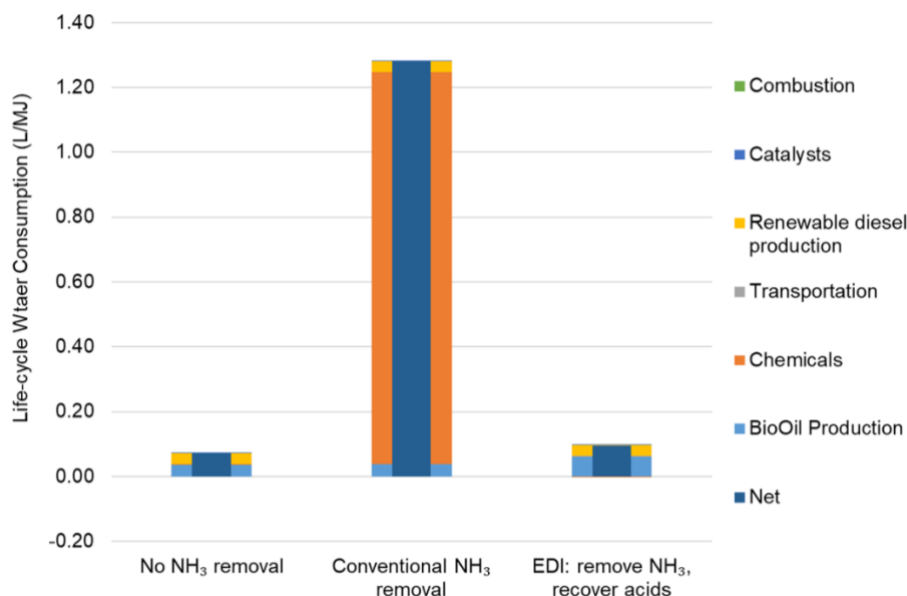


Figure 34 Water consumption for EDI-based recovery of mixed acids and bases from the HTL aqueous phase.



#### 4.2.4 Bio-oil and Biocrude Preprocessing with Adsorbents

**Motivation.** Early work has also focused on developing polymer and inorganic adsorbents to remove nitrogen species from HTL biocrude and carbonyl species from woody bio-oil. The species removal prior to hydrotreating was intended to reduce hydrogen consumption, reduce hydrotreating catalyst costs, and recover high-value nitrogen-containing species.

**Approach.** Molecular sieves and several different types of resins were evaluated as adsorbents for removal of the targeted species.

**Results.** Carbonyl removal from fast pyrolysis bio-oil was 34%, exceeding the 25% target (Figure 35, left; Lu et al. 2019). For nitrogen species removal from HTL biocrude with pyridine as a nitrogen surrogate, 52% pyridine removal was achieved (Figure 35, right).

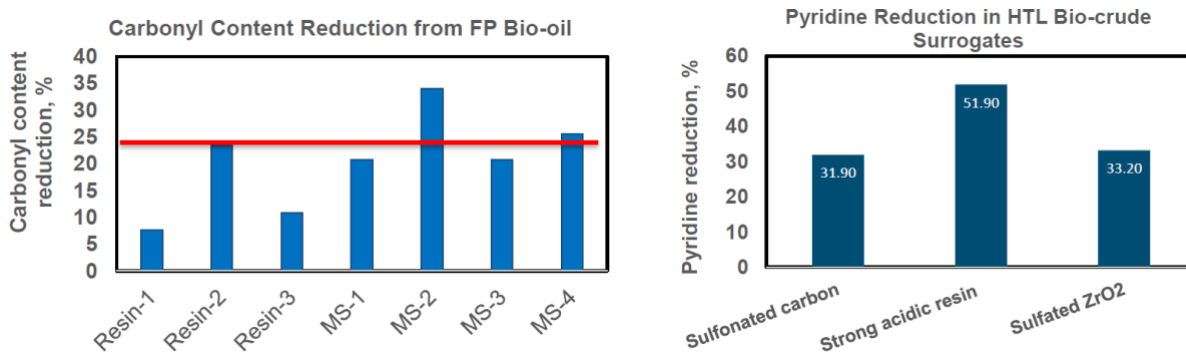


Figure 35 Effect of adsorbent type on carbonyl removal from bio-oil and nitrogen species removal from biocrude. Carbonyl adsorption surpassed the target for two molecular sieves and pyridine removal reached 52%.

For carbonyl reduction in pyrolysis oil, preliminary TEA (Figure 36) suggests that carbonyl reduction could significantly reduce the cost to produce hydrocarbon fuel from fast pyrolysis oil. The largest impact would come from eliminating the stabilizer cost (a pretreatment reactor ahead of the hydrotreater that uses very expensive catalyst) and using the removed carbonyls as heating oil rather than further processing them to produce additional fuel.

Data gaps for carbonyl removal include downstream hydrotreating testing to correlate carbonyl removal with downstream hydrotreating catalyst maintenance. Data gaps for nitrogen removal from HTL biocrude include testing with real biocrude, developing sorbents with strong acidity and high site density for biocrude cleaning, understanding membrane maintenance, and downstream hydrotreating testing. Results from experimental work with carbonyl removal were published in 2019 (Lu et al. 2019).

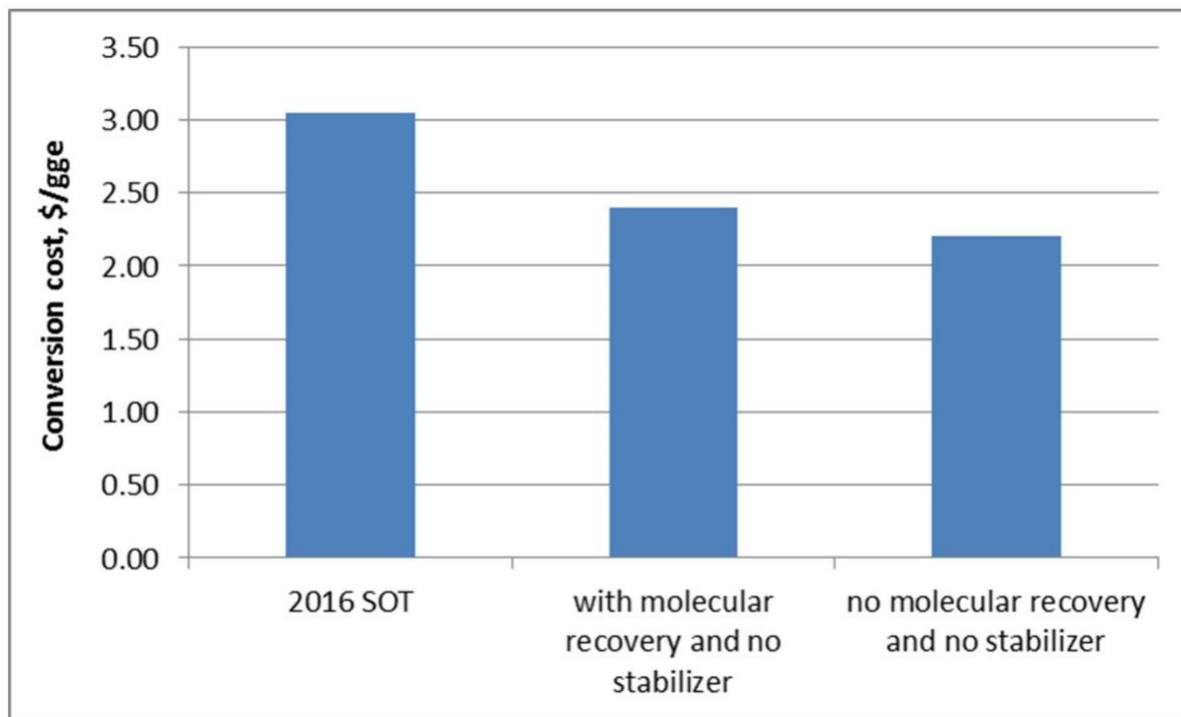


Figure 36 Economic impact of carbonyl removal from bio-oil.

#### 4.2.5 Industrial Relevance

As described in Section 4.1.6, the Consortium seeks to advance the understanding and performance of existing and new separations technologies toward solving industrially relevant separation problems. Table 4 summarizes the Consortium technologies with respect to thermochemical processes.

Table 4 Industrial relevance for thermochemical separation applications.

Separation technology	Current applications	Potential applications	Current Scale	Projected future scale	Types of compounds	Advantage over other technologies	Remaining gaps
CHGF	Removal of particulates from the vapor phase. Current applications do not involve inclusion of a catalyst.	Current applications during biomass conversion can be in biomass pyrolysis and gasification processes; particulate carryover can be problematic downstream. Inclusion of a catalyst can add catalytic upgrading of the chemical species in the vapor, in addition to particulate removal.	Catalytic hot gas filtration is currently in the research stage, typically in bench-scale test systems.	Vapor upgrading of biomass fast pyrolysis vapors at a commercial scale. However, technology development is at an early stage for such applications, as described in "remaining gaps."	Reactive oxygenated vapor species from fast pyrolysis are candidates for conversion in this step. This conversion can help stabilize fast pyrolysis vapors for further downstream upgrading.	If successful, the greatest benefit will be savings on reactor system capital costs, with the potential elimination of a dedicated reactor system, because the catalyst and associated reactions can occur in CHGF.	Development of catalysts with regeneration protocols (and associated on stream times) that allow regeneration within the hot gas filter (where the catalyst is housed), without significant redundant equipment. In this context, it may be necessary to regenerate the catalyst using the blowback cycle of the hot gas filter.
EDI	Removal/capture/concentration of organic acids from dilute carbon aqueous phase; simultaneous removal/capture/concentration of ammonia and organic acid	Recycle, purify, and concentrate N molecules in waste stream of HTL. The resin wafer can also incorporate catalyst material for in-situ esterification of organic acid into esters.	Currently, we operate at 5 g/h organic acid capture with >30wt.% titer in the capture stream; >99.5% ammonia removal from the HTL waste stream	EDI is ready for >10 kg/h acid capture (>5,000 gallons/day) operations		High productivity (throughput) of capture organic acids or other charges species in single stage and without chemical additives.	Improve capture productivity to achieve a >3-fold increase and halve energy consumption.
Membrane	Acid-resistance separations to enrich carboxylic acid in the HTL aqueous phase	Applicable to concentrations (dewatering) of other oxygenates such as organic acids, alcohols, diols, etc.	0.1–1.0 L	~10 L	Organic (carboxylic) acids, alcohols, diols, other water-soluble oxygenates, etc.	Less energy intensive, high-selectivity separations, low cost	Need to further enhance the membrane flux to reduce the processing time.

Table 4 (Cont.)

Separation technology	Current applications	Potential applications	Current Scale	Projected future scale	Types of compounds	Advantage over other technologies	Remaining gaps
Adsorbents	Carbonyl/ carboxylic acid reduction from woody pyrolysis bio-oils; removal of cyclic N compounds from HTL biocrudes	Clean up TC streams for catalyst preservation and product purification	0.1–0.5 L	1–100 L	Carbonyls, carboxylic acids; cyclic N-compounds	Less H <sub>2</sub> consumption, less catalyst deactivation, less ammonia gas emission, better energy efficiency and process economics	Need to improve adsorption selectivity, capacity, and regeneration of sorbent materials

## 4.3 Seed Projects

In FY 2017, exploratory research was conducted within two small tasks: biochemical catalyst preservation and algae processing.



### 4.3.1 Biochemical Catalyst Preservation

**Motivation.** Organisms used in biochemical conversion can be severely affected by contaminants in the bioreactor feed. These impurities arise from feedstocks, contamination during processing, and inhibitors produced during fermentation. This challenge prompted research into advanced materials (Figure 37) for low-cost, selective separations and initially targeted common interfering chemical classes such as aldehydes and carboxylic acids. The intended impact is to drive down bioconversion costs through increased titers, rates, and yield along with decreased lag phases of culture and to potentially reinvigorate consolidated bioprocessing.

Contaminant concentrations can be addressed through the use of adsorbents such as:

- Solid, high-surface area adsorbents candidates, including:
  - Surface-treated nanostructured adsorbents with high binding and recovery that can be magnetically manipulated (cycling has been demonstrated), and
  - Reusable, environmentally benign adsorbent foams.
- Flexible aerogels with highly microporous silica network with high capacities (e.g., adsorbing eight times their weight of product for some hydrophobic targets), good specificity and reusable.

**Approach.** Experimental work focused initially on nanoparticle (NP) networks because they are uniform and adaptable to small-scale synthesis. In contrast, polyurethane foams at small scales have heterogeneity issues, and aerogels were considered too new and unpredictable.

## Designer high-surface-area adsorbents in development

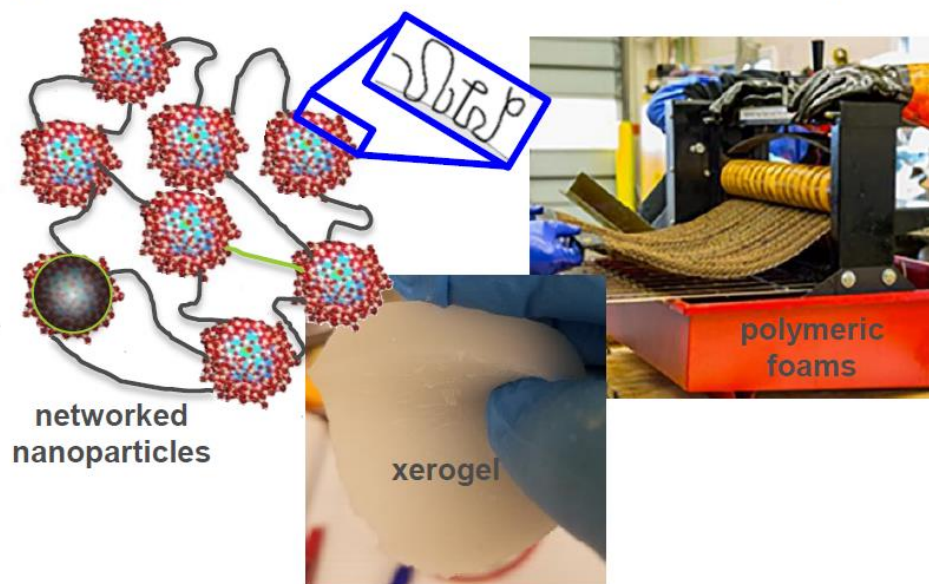


Figure 37 Materials developed in the Consortium include nanoparticles, xerogels, and polymeric foams.

NP networks are made up of chemically bonded NPs that use polymer chains with bifunctional coupling agents to form extended, looping chains of aromatic silanes. The surface treatment involves heterogeneous vapor-phase polymerization. Mixtures of hydrophobic (e.g., octyl, octadecyl, phenyl species) and hydrophilic (e.g., hydroxyl, amino, carboxyl species) elements were used to selectively target aldehydes. Primary amines are key to separations and their specificity results from strategic incorporation of hydrophobic and aromatic elements along with the amines.

Aldehydes were chosen as the target impurity because they interfere with most lignin valorization schemes, are produced by almost all lignocellulosic deconstruction strategies, and contribute to color and odor issues, which limit the potential of lignin for use in some applications (Table 5).

More than 20 designs for surface treatment combinatorics for NP were synthesized and characterized. Linkers between NP remained highly hydrophobic to limit cellular interactions. Five amine ratios and two aromatic:alkyl ratios were explored to tune aldehyde adsorption (Figure 38).

Table 5 Impurities that affect fermentation.

Target number	Toxin or inhibitory species	
	Feedstock stream	Fermentation broth
1	Furfural/methyl furfural	Butryaldehyde
2	Ferulic acid	Malondialdehyde
3	Benzoic acid	Succindialdehyde
4	Coumaric acid	Tolualdehyde
5	Phenyl acetate	Isoprenol/geraniol

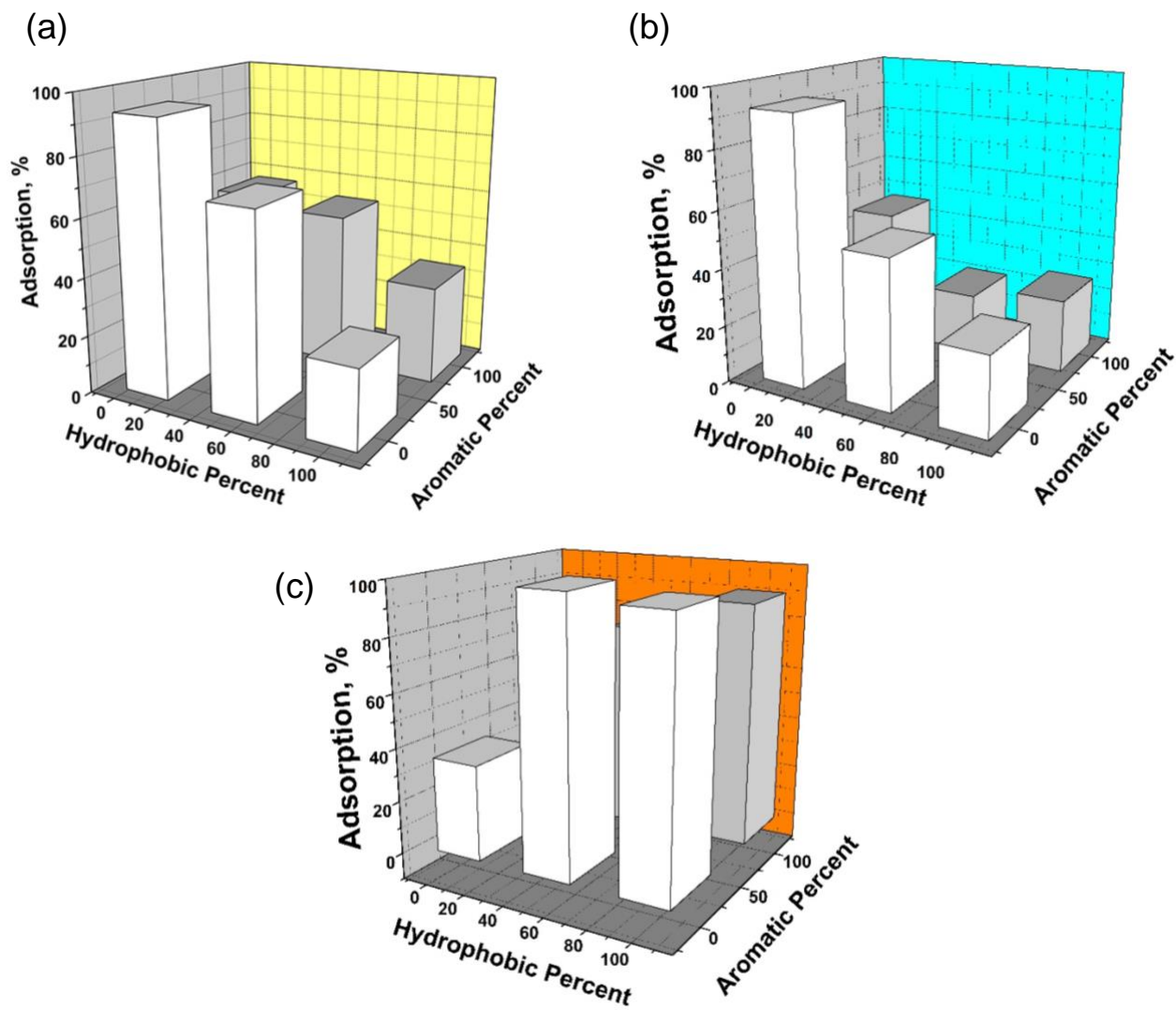


Figure 38 Adsorbent screening results for capturing three representative aldehydes: (a) formaldehyde, (b) acetaldehyde, and (c) benzaldehyde.

Process stream interference was measured with gravimetric analysis. Process streams studied (seven total) were mock feedstock hydrolysates, actual fermentation broths of mid-log-phase cultures (*E. coli*, *R. sphaeroides*), and actual fermentation broths of production hosts (*Pseudomonas putida* KT 2440, *S. cerevisiae*). Each experiment ran for 3 hours with agitation at 37°C and 0.5% adsorbent.

**Results.** Table 6 lists the binding ratio of the aldehyde to the total of other bound components. Specificity is defined as the amount of toxin bound relative to the binding of all other components of the process stream. Specificity benchmarks were set at >5. At times, results indicated specificity of >30. Specificity targets were achieved for inhibitors found within a feedstock stream such as formaldehyde, acetaldehyde, and hydroxymethyl furfural. Toxic intermediates coproduced during the bio-upgrading process, such as methylglyoxal, were also successfully bound. Four or more biocatalyst inhibitors exhibited

Nanoparticle-based adsorption exceeded binding specificity (ratio of bound toxin to binding of other stream components) benchmarks of five and reached 30 in some cases. Targeted inhibitors included those found within a feedstock stream and a toxic intermediate coproduced during bio-upgrading.

specificity (over all components of feedstock stream or fermentation broth) of 4:1 for one feedstock contaminant and one inhibitor produced during bio-upgrading.

Data gaps for this research include additional study of binding capacities, reuse potential, and potential for direct incorporation into process streams of passive binding elements, possibly with membrane shields.

Table 6 Binding ratios for various materials and impurities.

Toxin/Inhibitor	Best Material(s) Ref. No.	Specificity Binding Ratio <sup>a</sup> (aldehyde:stream interference, w:w)			
		DMR-EH	<i>E. coli</i> (LB)	Other, Minimal <sup>b</sup>	Other, Rich <sup>c</sup>
Formaldehyde	156	6.3	15.0	6.7	5.0
Acetaldehyde	156	5.8	13.8	6.1	4.6
Furfural <sup>d</sup>	152	29.1	36.4	11.2	14.2
	157	14.6	18.2	5.6	7.8
Hydroxymethylfurfural	156	12.2	29.4	13.0	9.8
Methylglyoxal	156	15.3	36.8	16.3	12.2

<sup>a</sup> Errors <2% in the analytics for the top and bottom datapoints of the ratio.

<sup>b</sup> Results on two materials shown for furfural. One is hydrophobic and the other relatively more hydrophilic. Either is likely useful in bioreactors; down-selection dictated by the medium used for growth and the target that is produced.

<sup>c</sup> Averages from *P. putida* KT2440 in M9-glucose medium and *R. sphaeroides* in MR26 medium.

<sup>d</sup> Averages from *P. putida* KT2440 in LB; *R. sphaeroides* in  $\epsilon$ YCC; and *S. cerevisiae* in YPD medium.



### 4.3.2 Algae Dewatering

**Motivation.** Dewatering algae cultures from approximately 0.1 to 20 wt% for use in downstream conversion processes imparts a significant cost to biofuels (Coons et al. 2014). Every kWh/m<sup>3</sup> of energy applied to harvesting contributes approximately \$1/GGE to the price of biofuel. This seed task evaluated ultrasonic filtration and crossflow membrane filtration for algae dewatering.

**Approach.** Tests were conducted as shown in Figure 39; harvesting and extraction were performed independently at each site in a single stage process. Conditions applied for ultrasonic tests represent current industry practice. Three feedstock species of microalgae were selected to cover a wide range of cell sizes. The size of the microalgae varied as shown in Figure 40. Ultrasonic separation was used in batch and hour-long flow experiments where steady-state removal was achieved rapidly, yielding concentrations as high as 10 wt%.





Ultrasonic Test System

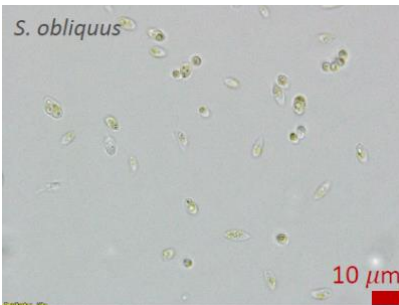


Recirculating Membrane Test System

Figure 39 Experimental setups for separations via ultrasonics and membranes.

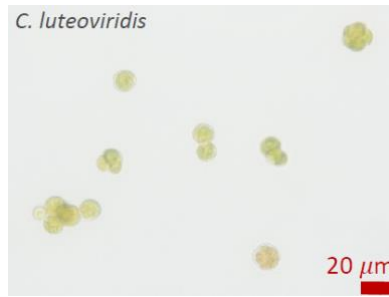
***Scenedesmus obliquus***

Ellipsoidal cells ( $3 \times 6 \mu\text{m}$ ),  
single cells, few aggregates



***Chlorella luteoviridis***

Large spherical cells ( $8\text{--}16 \mu\text{m}$ ),  
many aggregates of  $>3$  cells



***Nannochloropsis salina***

Small spherical cells ( $2\text{--}3 \mu\text{m}$ ),  
single cells, no aggregates

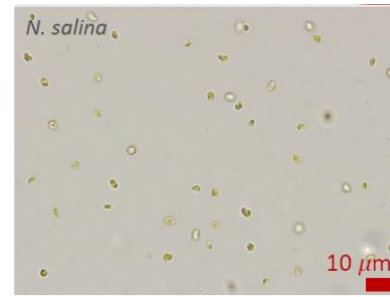


Figure 40 Characteristics of algae cultures used in the harvesting and dewatering study.

Membrane filtration was also used to dewater the microalgae. A crossflow filtration setup minimized the buildup of pore-clogging materials on the filter and concentrated the microalgae while continuously returning the retentate back to the feed. The fabricated membrane systems were stainless steel (434) with pore sizes of 4 and  $0.5 \mu\text{m}$ . They were operated at  $<10$  psi transmembrane pressure.

**Results.** Figure 41 shows the effects of energy input and cell size on microalgae removal. Energy inputs are similar to those of centrifugation. The figure shows agreement between batch and (steady) flow tests, which indicates the insignificance of hydrodynamic effects over the range of conditions studied.

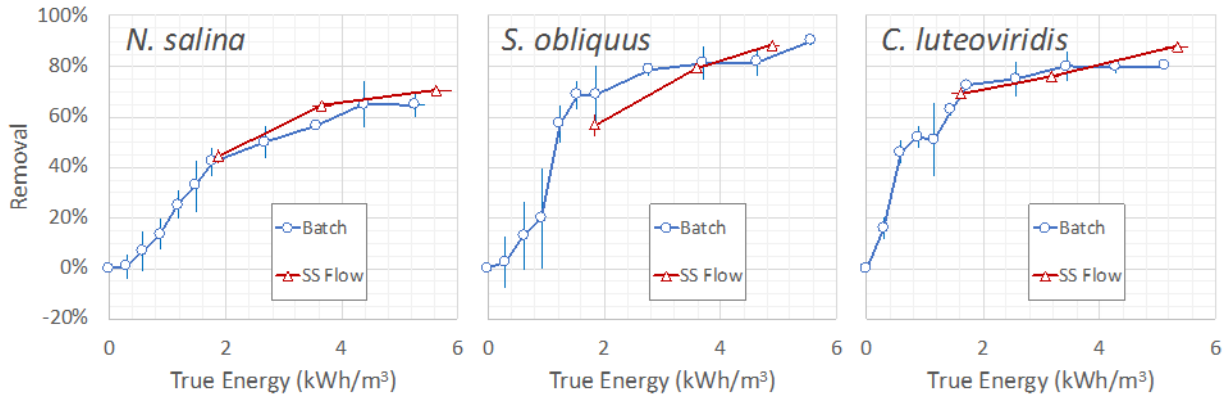


Figure 41 Ultrasonic removal of algal species showing agreement between batch and (steady) flow tests, which indicates the insignificance of hydrodynamic effects over the range of conditions studied. Microalgae cell size increases from left to right.

Concentration factors were shown to be largely a function of the ratio of filtrate to concentrate flow rates, as shown in Figure 42a. One metric to evaluate the viability of this technique to dewater algae is to compare the energy consumed in ultrasonic dewatering to the energy content of the algae that are recovered. Figure 42b illustrates this metric for three algae species. HHV values for the microalgae varied from 14 MJ/kg for *N. salina* to around 21 MJ/kg for the other species. Even at these high energy inputs, the effects of properties on fractional energy consumption are evident. Here, cell size, HHV, and biomass concentration are shown to affect the fractional energy needed for dewatering, with cell size being the most pronounced and larger cells requiring less energy for harvesting.

Cell size, HHV, and biomass concentration are shown to affect the fractional energy needed for dewatering, with cell size being the most pronounced and larger cells requiring less energy for harvesting.

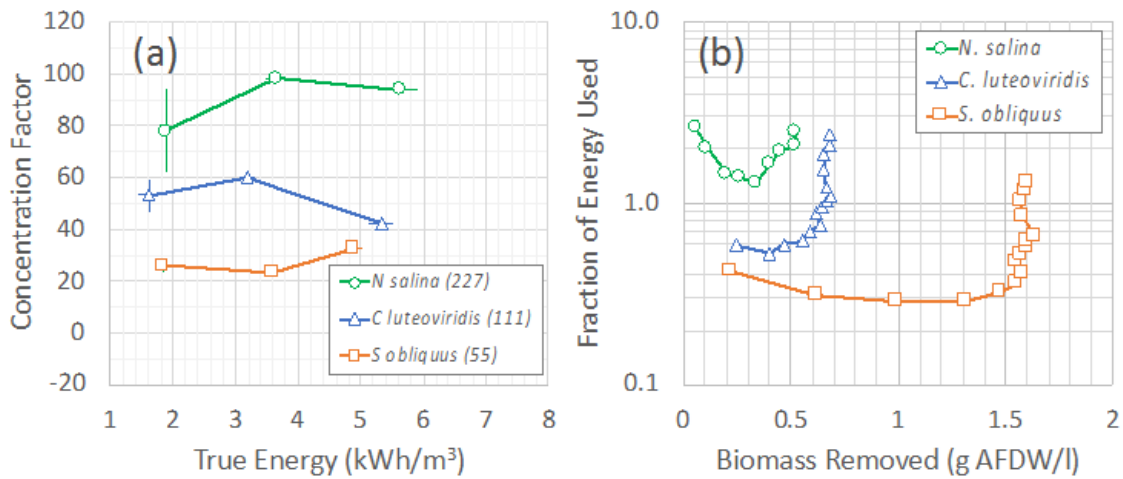


Figure 42 (a) Concentration factors obtained in flow tests increases according to the ratio of filtrate to concentrate flow rates shown in parenthesis. (b) Ultrasonic harvesting energy as a fraction of the energy in the microalgae removed using ultrasound.

Following ultrasonic dewatering, membranes were applied to further increase algae concentration. We tested each algae strain that had no detectable algae in the permeate. *N. salina* was concentrated by a factor of 20, to 6wt%, and *S. obliquus* by a factor of 25, to 10wt%. Both far exceeded the target of achieving 1 wt%.

Energy consumption of the membrane-based dewatering was 25 to 30 times (158 kWh/m<sup>3</sup>) more than for the ultrasonic separator. Internal membrane pressure was kept below 10 psi (0.02 kWh/m<sup>3</sup>), which suggests that a dead-end setup with no retentate recycle to the feed would consume much less energy. Although the crossflow membrane filtration setup requires much less filter area than a dead-end system, it also utilizes around four orders of magnitude more energy.

Data gaps include optimizing the configuration of ultrasonic separation and membrane filtration technologies. In addition, capital costs for ultrasonic separation need to be more fully developed to enable comparative TEA of this technology in comparison to others.

# 5 Stakeholder Engagement

## 5.1 Industrial Advisory Board (IAB)

The IAB (Table 7) helps the Consortium maintain an industry-relevant focus and provides knowledge of recent technology advances and challenges. The board is composed of eight industry advisors as well as an advisor from the Advanced Research Projects Agency-Energy (ARPA-E). The board meets with the Consortium twice a year and provides advice, reviews results and progress in comparison with work plans, provides feedback regarding prioritization of research projects, and informs development of the Consortium’s strategy for out years.

Table 7 IAB members, FYs 2017–2019.

Member	Affiliation
Kazuhito Suzuki	Ajinimoto
Binita Bhattacharjee	Amyris
Marc VonKeitz	ARPA-E
Steve Taggart	BP
Esteban Chornet	Enerkem
Tom Xu	DuPont
James Oyler	Genifuel
Bo Chen	Genomatica
Bob Rozmiarek	Virent

## 5.2 Meetings, Conferences, and External Communications

- Biannual face-to-face meetings with the IAB
  - FY 2017: NREL, December; Baltimore, May;
  - FY 2018: Argonne, December; ORNL, June; and
  - FY 2019: Argonne, December; NREL, May.
- Listening Day (May 23, 2017) was held in collaboration with AltSep, an industry workshop. Half of the attendees were from industry, a quarter from the national laboratories, and the balance from federal agencies and national associations. The breakout sessions covered industry-relevant separations issues and streamlining collaborations with the national laboratories. The resultant public report served as reference for Consortium planning (Bioprocessing Separations Consortium 2017).
- Targeted conferences: Special sessions were held at two conferences in 2018 with invited speakers from industry to highlight bioprocessing separations challenges and disseminate information about the Consortium and its technical progress. In FY 2019, an overview of the Consortium was presented outlining the purpose, key results and future plans:
  - 40<sup>th</sup> Symposium on Biotechnology for Fuels and Chemicals (April 29–May 2, 2018)
  - BioWorld Congress on Industrial Biotechnology (July 16–19, 2018)
  - Green Chemistry and Engineering—Green and Sustainable Chemistry Conference (June 11–13, 2019)

To facilitate external communications and disseminate information about the Consortium, an external website ([www.bioesep.org/](http://www.bioesep.org/)) has been established. The website provides stakeholders information about the Consortium’s current project portfolio and how to interact with the Consortium.

### 5.3 Directed Funding Opportunity

Directed Funding Opportunities (DFOs) are meant to accelerate the development of separations technologies for the commercialization of biomass-derived fuels and chemicals by engaging with industry to overcome their most pressing bioprocessing separations challenges and leveraging Separations Consortium capabilities and expertise. These opportunities allow industry to test BETO-funded separations technologies and assess their value.

The DFO project collaborations were established via conference calls with interested applicants to review industry needs and Consortium capabilities and to identify partners. Based on these initial meetings, \$2.4 million in federal funds were requested (>2x over subscription) and five \$200,000 federal fund projects were awarded. The five projects (Table 8) span a variety of feedstocks, conversion routes, and products and are an opportunity to showcase the Consortium’s ability to provide comprehensive solutions to industrial bioprocessing separations challenges.

Table 8 Direct Funding Opportunity projects between industry and Consortium members.<sup>a</sup>

Company	Waste/gas feedstock	Cellulosic sugar feedstock	Product	Lab(s)
Visolis		X	Mevalonic acid	Argonne, LBNL
Kalion		X	Glucaric acid	ORNL, LBNL, Argonne, NREL
Mango Materials	Biogas		Polyhydroxyalkanoates from methanotrophs	LBNL
DMC Biotechnologies		X	Farnesene, liquid hydrocarbons	Argonne, LBNL
HelioBioSys	Atmospheric CO <sub>2</sub>		Expandable Polystyrene from cyanobacterial consortium	LBNL, SNL, LANL

<sup>a</sup> LBNL = Lawrence Berkeley National Laboratory; ORNL = Oak Ridge National Laboratory; NREL = National Renewable Energy Laboratory; SNL = Sandia National Laboratory; LANL = Los Alamos National Laboratory.

## 6 Summary

---

Separations are a key challenge for industrial-scale bioprocessing applications because they are costly and complex. The Bioprocessing Separations Consortium was established in Fiscal Year 2017 to address various technical challenges that preclude the cost-competitive production of biofuels and bioproducts.

In its first three years, the Consortium developed six types of separation solutions important for efficient biochemical and thermochemical processing of biomass to fuels and chemicals. The Consortium interfaced with industry through its IAB, Listening Day, and conference special sessions to ground its portfolio in real-world challenges. Separations accomplishments included:

- Extraction technology coupled with in-situ fermentation product recovery: Research to integrate fermentation and separations through HED-ISPR for carboxylic acids and esters identified ideal extractants for these carbonyl compounds. The Consortium released a publicly available model of the HED-ISPR system. Industry and academic researchers can use the model to evaluate system design for integrated fermentation-separations challenges that are relevant to them. Laboratory-scale experiments demonstrated that this energy-efficient process recovered 95% of C4 compounds in fermentation broth at a purity of 98.5% mol. EDI was also integrated with ISPR and captured >95% of pure organic acids, consuming <1.0 kWh/lb. acid, an industrially relevant benchmark. A comparison of a simulated moving bed (SMB) baseline, EDI-ISPR, and HED-ISPR, concluded that the HED-ISPR showed the lowest overall MFSP and life-cycle GHG emissions.
- Electrochemical separation for recovery of organic acids and bases (e.g., caustic, ammonia) from aqueous streams: EDI-based separations were developed to maintain high concentrations of recovered acid and NaOH regardless of the percentage removal. Concentrations of each species were shown to exceed target levels.
- Polymeric and ceramic membrane development for lignin fractionation: For lignin conversion, species with high molecular weights must be removed and other compounds separated as a function of molecular weight. Furthermore, lignin fractionation must occur at a sufficiently high, industrially relevant throughput. The Consortium's multi-stage filtration approach to lignin fractionation made significant progress towards these aims, removing compounds above 1 kDa and achieving a flux five to ten times greater than a single 450 Da filtration step.
- Adsorbent techniques for selective removal of carbonyls and small organic nitrogen containing molecules: Adsorbents tailored to remove impurities that hinder biological cultivation, such as aldehydes, showed specificity (over all components of feedstock stream or fermentation broth) of 4:1 for one feedstock contaminant and one inhibitor produced during bio-upgrading. Adsorbents were applied to remove 34% of carbonyl species from fast pyrolysis biofuel, corresponding to nearly \$1/GGE decrease in the conversion cost to approximately \$2.50/GGE.

Altogether, these technical accomplishments resulted in ten journal publications and seven patents. The Separations Consortium also established five industrial collaborations through the DFO. These five projects encompass separation of various organic acids, alcohols, and polymers from fermentation broth and gaseous streams.

Based on the portfolio of work to date and feedback from industry and BETO-internal stakeholders, the Consortium expects to undertake a new slate of projects for FYs 2020–2022, as outlined in Table 9. This portfolio balances interactions with other BETO projects and consortia, the development of new separations technologies, and analysis and computation. Furthermore, TEA and LCA will be conducted consistently and comprehensively for each Consortium project in this three-year period.

Table 9 Consortium project slate: FYs 2020–2022.

Project	Streams	Technologies	Products
Lignin separations	APL, Reductive Catalytic Fractionation (RCF), Catalytic Oxidation RCF COO, RCF	Membrane-less EDI, membranes	Monomeric acids, high-molecular weight lignin species, NaOH
Redox-based electrochemical separations (RECS)	Fermentation broth	Pseudo-capacitive deionization	Short-chain volatile fatty acids
2,3-butanediol separations	Fermentation broth	Membranes and sorbents	2,3-butanediol
Counter-current chromatography (CCC)	HTL oils, APL, RCF, pyrolysis oil	CCC	Cresols, phenols, carboxylic acids, metal impurities, from lignin-rich streams: trimers, dimers, monomers
Volatile product recovery	Vapor phase from fermentation	Nanostructured adsorbents	3-methyl anisole, isoprene, terpenes, C <sub>5</sub> alcohols
Computation	Fermentation broth and vapor phase	Density functional theories and classical molecular dynamics methods	3-methyl anisole, isoprene, terpenes, C <sub>5</sub> alcohols, 2,3-butanediol

# 7 References

---

Agile BioFoundry, 2020, *Agile BioFoundry*. Available at: <https://agilebiofoundry.org/>

Arnell, A., J. Olsson, and O. Wallberg, 2014, "Process performance in lignin separation from softwood black liquor by membrane filtration," *Chemical Engineering Research and Design*. 92(9): 1792–1800.

Beckham, G.T., "Lignin-First Biorefinery Development" Presented at the 2019 Bioenergy Technologies Office Peer Review. Denver, Colorado. March 4–8. Available at: [https://www.energy.gov/sites/prod/files/2019/04/f61/Lignin%20First%20Biorefinery%20Development\\_NL0033400\\_1.pdf](https://www.energy.gov/sites/prod/files/2019/04/f61/Lignin%20First%20Biorefinery%20Development_NL0033400_1.pdf)

Bioprocessing Separations Consortium, 2017, *Summary of Bioprocessing Separations Consortium Industrial Listening Day May 2017*, June 30. Available at [http://www.bioesep.org/wp-content/uploads/sites/72/2017/08/20170731\\_Listening-Day-Report.pdf](http://www.bioesep.org/wp-content/uploads/sites/72/2017/08/20170731_Listening-Day-Report.pdf)

CCPC, 2020, *Consortium for Computational Physics and Chemistry*. Available at: <https://www.cpcbmass.org/>

ChemCatBio, 2020, *Chemical Catalysis for Bioenergy*. Available at: <https://www.chemcatbio.org/>

Coons, J., Gasway, C., Yap, B., Bischoff, B., Sweeney, N., Dong, T., Pienkos, P., Dale, T., Sanders, C. 2019, "The Energy Costs of Dewatering Feedstock microalgae Species Using Standard Implementations of Ultrasonic and Membrane Filtration Technologies," in preparation.

Coons, J.E., D.M. Kalb, T. Dale, and B.L. Marrone, 2014, "Getting to low-cost algae biofuels: A monograph on conventional and cutting-edge harvesting and extraction technologies," *Algal Research* 6: 250–270.

Davis, R., N. Grundl, L. Tao, M.J. Bidy, E.C.D. Tan, G.T. Beckham, D. Humbird, D.N. Thompson, and M.S. Roni, 2018, *Process Design and Economics for the Conversion of Lignocellulosic Biomass to Hydrocarbon Fuels and Coproducts: 2018 Biochemical Design Case Update*, NREL/TP-5100-71949.

Dunn, J., T. Pray, T. Dale, 2019, "Bioprocessing Separations Consortium." Presented at the 2019 Bioenergy Technologies Office Peer Review. Denver, Colorado. March 4–8.

Dutta, A., K. Iisa, C. Mukarakate, M. Griffin, E.C.D. Tan, J. Schaidle, D. Humbird, H. Wang, D. Hartley, D. Thompson, and H. Cai, 2018, *Ex Situ Catalytic Fast Pyrolysis of Lignocellulosic Biomass to Hydrocarbon Fuels: 2018 State of Technology and Future Research*, NREL/TP-5100-71954, National Renewable Energy Laboratory. Golden, Colorado. Available at: <https://www.nrel.gov/docs/fy19osti/71954.pdf>.

EERE (Energy Efficiency and Renewable Energy), 2015, *Bioproducts to Enable Biofuels Workshop Summary Report*. Available at: [https://www.energy.gov/sites/prod/files/2015/12/f27/bioproducts\\_to\\_enable\\_biofuels\\_workshop\\_report.pdf](https://www.energy.gov/sites/prod/files/2015/12/f27/bioproducts_to_enable_biofuels_workshop_report.pdf),

EERE, 2014, *Process Integration and Carbon Efficiency Workshop Summary Report*. Available at: [https://www.energy.gov/sites/prod/files/2014/12/f19/process\\_integration\\_workshop\\_report\\_dec\\_2014.pdf](https://www.energy.gov/sites/prod/files/2014/12/f19/process_integration_workshop_report_dec_2014.pdf)

EERE, 2020, *Co-Optimization of Fuels & Engines*. Available at: <https://www.energy.gov/eere/bioenergy/co-optimization-fuels-engines>



Elander, R.T., D. Vardon, D.K. Johnson, Z. Li, A.D. Sutton, V. Dagle, K.K. Ramasamy, "Catalytic Upgrading of Biochemically Derived Intermediates (CUBI)." Presented at the 2019 Bioenergy Technologies Office Peer Review. Denver, Colorado. March 4–8. Available at: [https://www.energy.gov/sites/prod/files/2019/03/f61/Catalytic%20Upgrading%20of%20Biochemically%20Derived%20Intermediates%20%28CUBI%29\\_NL0026681.pdf](https://www.energy.gov/sites/prod/files/2019/03/f61/Catalytic%20Upgrading%20of%20Biochemically%20Derived%20Intermediates%20%28CUBI%29_NL0026681.pdf)

Fitzgerald, N. and A. Bailey, 2018, *Moving Beyond Drop-In Replacements: Performance-Advantaged Biobased Chemicals Workshop Summary Report*. Available at: <https://www.energy.gov/sites/prod/files/2018/06/f53/Performance-Advantaged%20Biobased%20Chemicals%20Workshop%20Report.pdf>

Hu, M., C. Engtrakul, B.L. Bischoff, M. Lu, and M. Alemseghed, 2018, "Surface-Engineered Inorganic Nanoporous Membranes for Vapor and Pervaporative Separations of Water–Ethanol Mixtures," *Membranes* 8(4):95.

Humpert, D., M. Ebrahimi, and P. Czermak, 2016, "Membrane Technology for the Recovery of Lignin: A Review," *Membranes* 6(3):42.

Lu, M., and M. Hu, 2020, "[Novel Porous Ceramic Tube-Supported Polymer Layer Membranes for Acetic Acid/Water Separation by Pervaporation Dewatering.](https://doi.org/10.1016/j.seppur.2019.116312)" *Separation and Purification Technology* 236: 116312. Available at: <https://doi.org/10.1016/j.seppur.2019.116312>.

Lu, M., M. Hu, S. Lee, H. Wang, and J. Liu, 2019, "Selective adsorption removal of carbonyl molecular foulants from real fast pyrolysis bio-oils," *Biomass & Bioenergy*, submitted.

Lu, M., A.W. Lepore, J.S. Choi, Z. Li, Z. Wu, F. Polo-Garzon, and M.Z. Hu, 2019, "Acetic Acid/Propionic Acid Conversion on Metal Doped Molybdenum Carbide Catalyst Beads for Catalytic Hot Gas Filtration," *Catalysts* 8(12):643.

Peterson, B., C. Engtrakul, A.N. Wilson, S. Dell'Orco, K.A. Orton, S. Deutch, M.M. Yung, A.K. Starace, Y. Parent, D. Chiamonti, and K.A. Magrini, 2019, "Catalytic Hot-Gas Filtration with a Supported Heteropolyacid Catalyst for Preconditioning Biomass Pyrolysis Vapors," *ACS Sustainable Chemistry & Engineering* 7(17): 14941–14952. Available at <http://dx.doi.org/10.1021/acssuschemeng.9b03188>.

Saboe, P., L. Manker, W. Michener, D. Peterson, D. Bradner, S. Deutch, M. Kumar, R. Cywar, G. Beckham, and E. Karp, 2018, "*In situ* recovery of bio-based carboxylic acids," *Green Chemistry* 20:1791–1804.

Saboe, P., H. Monroe, W. Michener, L. Manker, S. Haugen, G. Beckham, and E. Karp, 2019, "*In situ* product recovery of bio-based ethyl esters *via* hybrid extraction-distillation," *Green Chemistry* 21:5306–5315. Available at: <https://doi.org/10.1039/C9GC01844A>.

Shao, P., and A. Kumar, 2009, "Recovery of 2, 3-butanediol from water by a solvent extraction and pervaporation separation scheme," *Journal of Membrane Science* 329(1-2):160–168.

Sholl, D.S., and R.P. Lively, 2016, "Seven chemical separations to change the world,". *Nature*. 532, 435.

Xu, S., H. Zhang, F. Yu, X. Zhao, and Y. Wang, 2018, "Enhanced ethanol recovery of PDMS mixed matrix membranes with hydrophobically modified ZIF-90," *Separation and Purification Technology* 206:80–89.