USED FUEL DISPOSITION CAMPAIGN

Addition of Bromide to Radiolysis Model Formulation for Integration with the Mixed Potential Model

Fuel Cycle Research & Development

Prepared for U.S. Department of Energy Used Fuel Disposition Campaign

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July 15, 2016

PNNL-25539

M4FFT-16PN080302062

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EXECUTIVE SUMMARY

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This report fulfills the M4FT-16-PN080302062 to report on continuing the model integration of the PNNL Radiolysis Model and the ANL Mixed Potential Model for Argillite Disposal. In this work, we demonstrate and approximate the effects of bromide ions on hydrogen peroxide generation under conditions of low oxygen concentration and over pressure of hydrogen. As has been shown these are conditions for which hydrogen peroxide generation is strongly reduced. We find that this reduction is strongly canceled by the presence of even small concentrations of bromide. The full Radiolysis Models seems to be required to accurately predict the effect, but we offer an empirical conservative model for use in the ANL Mixed Potential Model applicable to the prediction of UO_2 degradation.

Details of the approach are intended to be sufficient for developing a module for calculating radiolytic generation of hydrogen peroxide with known concentration of H_2 , O_2 and Br^- . The Listings of the program and reactions considered in this report are given in Appendices.

ACKNOWLEDGMENTS

We thank Jim Jerden and Bill Ebert for helpful discussions on the operation of the ANL Mixed Potential Model and proposing the definition of a conditional *G*-value. We thank Carlos Jové-Colón, and David Sassani for support and helpful discussions on the effects of bromide and model interface alternatives.

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ACRONYMS

ANL	Argonne National Laboratory
DOE DOE-NE	U.S. Department of Energy U.S. Department of Energy Office of Nuclear Energy
MPM	Mixed Potential Model
ODE	ordinary differential equation
PNNL	Pacific Northwest National Laboratory
RM	Radiolysis Model
SNF	spent nuclear fuel
UFDC UNF	Used Fuel Disposition Campaign used nuclear fuel

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1. INTRODUCTION

The U.S. Department of Energy Office of Nuclear Energy (DOE-NE), Office of Fuel Cycle Technology has established the Used Fuel Disposition Campaign (UFDC) to conduct the research and development activities related to storage, transportation, and disposal of used nuclear fuel (UNF) and high-level radioactive waste. Within the UFDC, the components for a general system model of the degradation and subsequent transport of UNF is being developed to analyze the performance of disposal options [Sassani et al., 2012]. Two model components of the near-field part of the problem are the ANL Mixed Potential Model and the PNNL Radiolysis Model. This report is in response to the desire to integrate the two models as outlined in [Buck, E.C, J.L. Jerden, W.L. Ebert, R.S. Wittman, (2013) "Coupling the Mixed Potential and Radiolysis Models for Used Fuel Degradation," FCRD-UFD-2013-000290, M3FT-PN0806058]

Details of the approach are intended to be sufficient for developing a module for calculating radiolytic generation of hydrogen peroxide with known concentration of H_2 , O_2 and Br^- . The listings of the program and reactions considered in this report are given in the appendices.

2. RADIOLYSIS MODEL FOR USE IN USED FUEL OXIDATION

Previous work that reports the results of a radiolysis model sensitivity study [Wittman RS and EC Buck. 2012] showed that of the approximately 100 reactions [Pastina, B. and LaVerne, J. A., 2001] describing water radiolysis, only about 37 are required to accurately predict H_2O_2 to one part in 10⁵. The intended application of that radiolysis model (RM) was to calculate H_2O_2 production for an electrochemical based mixed potential model (MPM) [Jerden, J., Frey, K., Cruse, T., and Ebert, W., 2013] developed to calculate the oxidation/dissolution rate of used nuclear fuel [Shoesmith, D.W., Kolar, M., and King, F., 2003] under disposal conditions where O_2 is expected to be at low concentrations and H_2 is generated from oxidation of steel containers. As an initial approximation, that model (MPM) was developed under the assumption that H_2O_2 is generated at a rate determined only by its radiolytic *G*-value. Ideally, for a full RM-MPM integration, the MPM would use a reaction kinetics based model to predict H_2O_2 for various water chemistries. As a further step in that direction, this report updates the previously reported steady-state behavior of a full RM under conditions where small concentrations of bromide [Br⁻] are present.

2.1 Model Coupling Definition

The RM coupled kinetics/diffusion rate equations for H_2O_2 on discrete special zones (*n*) can be expressed in terms concentrations $[H_2O_2]_n$, fluxes J_n and dose rate \tilde{J} according to

$$\frac{d\left[\mathrm{H}_{2}\mathrm{O}_{2}\right]_{n}}{dt} + \frac{J_{n}^{(\mathrm{H}_{2}\mathrm{O}_{2})} - J_{n-1}^{(\mathrm{H}_{2}\mathrm{O}_{2})}}{x_{n} - x_{n-1}} = G_{\mathrm{H}_{2}\mathrm{O}_{2}}\dot{d}_{n} + (\text{reaction kinetics})_{n}$$
(1)

Assuming nonzero reaction kinetics and dose-rate only in the radiation zone (x_R) with diffusion out to the boundary (x_B) , the steady-state solution to Eq. (1) after inserting Fick's Law fluxes containing diffusion constant D and boundary concentration $[H_2O_2]_B$ can be written:

$$\frac{D_{\rm H_2O_2}}{x_R x_B} \left[{\rm H_2O_2} \right] = G_{\rm H_2O_2} \dot{d} + (\text{reaction kinetics}) + \frac{D_{\rm H_2O_2}}{x_R x_B} \left[{\rm H_2O_2} \right]_B \equiv G^C_{\rm H_2O_2} \dot{d}$$
(2)

Equation 2 serves as the working definition of "conditional" *G*-value [Buck, et al., (2013)] ($[H_2O_2]_B = 0$ is assumed). Here "conditional" refers to an effective H_2O_2 generation that is conditional on the local water chemistry. Additionally, because each time-step of the MPM the radiolysis model would have effectively reached steady-state, Eq. (2) is assumed to define the interface between the RM and MPM – i.e. the MPM evaluates a new conditional *G*-value for its H_2O_2 production calculation at each time-step.

The next section describes an analytical simplification of the full RM to approximate $[H_2O_2]$ and Eq. (2) for use in the MPM and how $[H_2O_2]$ is affected by the presence of bromide.

2.2 Model Inclusion of Bromide Reactions

This section reviews how a simple analytical function for a conditional H_2O_2 *G*-value compares with the full radiolysis model and shows the added effect of including [Br⁻] related reactions. The Table 2-1 reactions contain the H_2O_2 generating mechanism of the full RM predictions. Without Br⁻ and for low O₂ concentration, reaction 33 shows how the presence of H_2 converts the ·OH radical to the ·H radical to accelerate H_2O_2 destruction lowering its conditional *G*-value. At higher O₂ concentrations, O₂ effectively competes for ·H radicals to disable H_2O_2 destruction (reaction 27) (reaction numbers are those of the full RM and rate constants are from [Elliot, A.J.; McCracken, D.R. 1990] and [Kelm, M.; Bohnert, E. 2004]).

	Reaction	k_r
3	$H_2O_2 \rightarrow H^+ + \cdot HO_2^-$	1.1×10^{-1}
4	$H^+ + \cdot HO_2^- \rightarrow H_2O_2$	5.0×10^{10}
15	$\cdot HO_2 \rightarrow O_2^- + H^+$	1.3×10^{6}
16	$O_2^- + H^+ \rightarrow \cdot HO_2$	5.0×10^{10}
23	$e^- + H_2O_2 \rightarrow \cdot OH + OH^-$	1.1×10^{10}
26	$\cdot H + H_2O_2 \rightarrow \cdot OH + H_2O$	9.0×10^{7}
27	$\cdot H + O_2 \rightarrow \cdot HO_2$	2.1×10^{10}
33	$\cdot OH + H_2 \rightarrow \cdot H + H_2O$	4.3×10^{7}
34	$\cdot OH + H_2O_2 \rightarrow \cdot HO_2 + H_2O_2$	2.7×10^{7}
35	$\cdot HO_2 + O_2^- \rightarrow \cdot HO_2^- + O_2$	8.0×10^{7}
36	$H_2O_2 \rightarrow \cdot OH + \cdot OH$	2.5×10^{-7}
94	$Br^- + \cdot OH \rightarrow BrOH^-$	1.1×10^{10}
96	$Br^- + \cdot H \rightarrow BrH^-$	0.0×10^{6}
102	$\mathrm{Br}^- + \mathrm{H}_2\mathrm{O}_2 \rightarrow \mathrm{Br}^- + \mathrm{O}_2^- + 2\mathrm{HO}^+$	2.5×10^{9}
138	$BrOH^- \rightarrow Br^- + \cdot OH$	3.0×10^{7}
139	$BrOH^- \rightarrow \cdot Br + OH^-$	4.2×10^{6}

Table 2-1. Subset of reactions sufficient to represent the primary mechanisms for H_2O_2 generation in the full RM.^a

The net effect of this mechanism can be seen in Figure 2-1 where a reduction in H_2O_2 generation occurs for small O_2 and high H_2 concentration.

^a Reaction (96) was listed with zero reaction rate in Kelm and Bohnert, 2004.

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Figure 2-1. Comparison of Full RM and Empirical RM Steady-state conditional *G*-values at a dose rate of 160 rad/s.

The effect of even small concentrations of Br^- can be seen in Figure 2-2. Figure 2-2 shows a slice through Figure 2-1 where $[O_2]$ is fixed at 1 μ M. The effect of high H₂ concentrations to lower the H₂O₂ conditional *G*-value is nearly removed with the presence of Br^- .



Figure 2-2. Effect of $[Br^-]$ on the H₂O₂ conditional *G*-values in a ([H₂], [O₂]) region of suppressed H₂O₂ generation rate with Full RM.

It is interesting that even at a hydrogen pressure of 100 atm ([H₂] = 80000 μ M) only 100-400 μ M of Br⁻ can bring *G*^C from 0.1 to nearly 1.0 molecule/100-eV. The main reason for the effect is reaction 92 in Table 2-1 [Kelm, M.; Bohnert, E. 2004]. By competing for the ·OH radical, Br⁻ disables the mechanism for converting ·OH radicals to ·H radical, strongly lowering the rate of destruction of H₂O₂ destruction. It should be mentioned that this mechanism does not operate for the chloride ion because of the smaller rate constant for reaction 39 (see Appendix A).

Based on Table 2.1 an empirical model was previously developed with a minimal number of reactions for use in the MPM. A summary of that model can be described by four "simplified" rate equations that dominate when hydrogen concentration is large. In the radiation zone assuming diffusion only for H_2O_2 and O_2 , the four equations that incorporate reaction 92 are:

$$\tilde{D}_{\rm H_2O_2}[\rm H_2O_2] = \tilde{G}_{\rm H_2O_2} - k_{26}[\cdot\rm H][\rm H_2O_2] - k_{36}[\rm H_2O_2]$$
(3)

$$0 = \tilde{G}_{\cdot \mathbf{H}} - k_{27} [\cdot \mathbf{H}] [\mathbf{O}_2] - k_{23} [\cdot \mathbf{H}] [\mathbf{H}_2 \mathbf{O}] + k_{33} [\cdot \mathbf{O} \mathbf{H}] [\mathbf{H}_2]$$
(4)

$$0 = \tilde{G}_{.\rm OH} - k_{33} [\cdot \rm OH] [H_2] - k_{94} [\cdot \rm OH] [Br^-]$$
(5)

$$\tilde{D}_{0_2}[O_2] = -k_{27}[\cdot \mathbf{H}][O_2] + \tilde{D}_{0_2}[O_2]_B$$
(6)

where the bromide concentration is assumed to enter only through reaction 94 [Eq. (5)]. Additionally, if we assume the bromide concentration is the value in the radiation zone as with H_2 , the conditional G-value can be expressed as the solution to a quadratic equation

$$G_{\mathbf{n}_{2}\mathbf{O}_{2}}^{C} = \frac{-C_{1} + \left(C_{1}^{2} - 4C_{0}C_{2}\right)^{\frac{1}{2}}}{2C_{2}} \tag{7}$$

where the coefficients are given by:

$$C_0 = -k_{23}k_{27}[\mathrm{H}_2\mathrm{O}]\tilde{D}^2_{\mathrm{H}_2\mathrm{O}_2} \tag{8}$$

$$C_{1} = -\tilde{D}_{\text{H}_{2}\text{O}_{2}} \left[k_{26}k_{27}[\text{O}_{2}]_{B}\tilde{D}_{\text{O}_{2}} + k_{23}k_{26}[\text{H}_{2}\text{O}]\tilde{D}_{\text{O}_{2}} - 2k_{23}k_{27}[\text{H}_{2}\text{O}]\left(\tilde{D}_{\text{H}_{2}\text{O}_{2}} + k_{36}\right) \right] \\ + k_{26}k_{27}\tilde{D}_{\text{H}_{2}\text{O}_{2}} \left(\tilde{G}_{\cdot\text{H}} + \tilde{G}_{\cdot\text{OH}}F_{\text{B}c^{-}}\right)$$
(9)

$$C_{2} = \left[k_{26} k_{27} [O_{2}]_{B} \tilde{D}_{O_{2}} + k_{23} k_{26} [H_{2}O] \tilde{D}_{O_{2}} - k_{23} k_{27} [H_{2}O] \left(\tilde{D}_{H_{2}O_{2}} + k_{36} \right) \right] \left(\tilde{D}_{H_{2}O_{2}} + k_{36} \right) + k_{26} \left(k_{26} \tilde{D}_{O_{2}} - k_{27} \tilde{D}_{H_{2}O_{2}} - k_{27} k_{36} \right) \left(\tilde{G}_{\cdot H} + \tilde{G}_{\cdot OH} F_{Br^{-}} \right),$$
(10)

where

$$F_{\rm Br^-} = \frac{k_{33}[{\rm H}_2]}{k_{33}[{\rm H}_2] + k_{94}[{\rm Br}^-]}.$$
(11)

Diffusion constants were defined in earlier reports (see Buck et al., 2013). Unlike the pure water system, the presence of bromide introduces an additional dependence on hydrogen through Eq. (11). In this approximation, some of the effect of H_2 is handled empirically by making $G_{\cdot H}$ and $G_{\cdot OH}$ dependent on $[H_2]$ according to:

$$G_{\text{H}} = (0.10 \text{ molecules}/100 \text{-eV}) \left[1 - \exp\left(-\frac{[\text{H}_2]F_{\text{Br}^-}/0.1 \text{ atm}}{7.8 \times 10^{-4} M/\text{atm}}\right) \right]$$
(12)

$$G_{.\rm OH} = (0.35 \text{ molecules}/100 \text{-eV}) \left[1 - \exp\left(-\frac{[\text{H}_2]F_{\text{B}r^-}/0.3 \text{ atm}}{7.8 \times 10^{-4} M/\text{atm}}\right) \right]$$
(13)

Additionally, in this approximation k_{23} is reduced by a factor of 56, k_{94} is increased by a factor of 10 and x_B is adjusted between 0.4 and 0.5~cm to compare reasonably well with the full radiolysis model kinetics-diffusion result. Appendix B gives the FORTRAN listing for evaluating the empirical RM. Figure 2-3 shows the conditional *G*-value as a function of $[H_2]$ and $[O_2]_B$ for the full RM and for the one calculated from Eqs. (7-13).



Figure 2-3. Effect of bromide ($[Br^-] = 1 \mu M$ and $[Br^-] = 10 \mu M$) on Empirical RM Steady-state conditional *G*-values at a dose rate of 160 rad/s.

As in the case of Figure 2-1, a scaling behavior still occurs for Figure 2-3 where the shape of the concentration surface remains unchanged with the same scaling of dose rate, $[H_2]$, $[O_2]_B$ and now of $[Br^-]$. The empirical RM with bromide was seen to have less accuracy in comparison with the full RM, but because of the absence of the direct H_2O_2 destructive reaction 102, the prediction of G^C appears to be normally conservative for regions where a larger G^C is expected. While it appears that more reactions and further complexity is required for greater accuracy, the Empirical RM is seen to retain the general features of the Full RM (Figure 2-4) and has the advantage of being quickly evaluated.



Figure 2-4. Effect of $[Br^-]$ on the H₂O₂ conditional *G*-values in a ([H₂], [O₂]) region of suppressed H₂O₂ generation rate with Empirical RM (dashed) and Fill RM (solid).

2.3 Future Work

While a reasonable model for H_2O_2 generation with the presence of bromide can be constructed as in the pure water system, an accurate representation of the bromide effect on H_2O_2 seems to require the full radiolysis model. Future work will attempt to formulate a reduced model that more closely compares with the full model as well as incorporate carbonate chemistry. A future goal will be to represent a full RM with in the fuel degradation MPM, but as shown here, an empirical model is helpful for both simple calculation and for understanding the most relevant underlying mechanisms that are imbedded in the reactions.

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APPENDIX A: Reaction Listing for Full RM

Equilibrium constants: H2O $\langle -- \rangle$ H+ + OH- : RKeq(2) = $10^{(-13.999)}$ $H2O2 < --> H+ + HO2-: RKeq(3) = 10^{(-11.65)}$ OH $\langle -- \rangle$ H+ + O- : RKeq(4) = 10^(-11.9) HO2 <--> H+ + O2- : RKeq(5) = $10^{(-4.57)}$ $\langle -- \rangle$ H+ + E- : RKeq(6) = 10^(- 9.77) Η Rate constans (M⁻ⁿ/s) Reactions 1 H+ + OH- = H2O1.4d11 1.4dl rk(2) = rk(1)*RKeq(2) rk(3) = rk(4)*RKeq(3) 2 H2O = H+ + OH-3 H2O2 = H+ + HO2-4 H+ + HO2- = H2O2 5.0d10 H2O2 + OH- = HO2- + H2O 5 1.3d10 6 HO2- + H2O = H2O2 + OH- rk(6) = rk(5) * RKeq(2) / RKeq(3)E- + H2O = H + OH-7 1.9d1 8 2.2d7 9 E - + H + = H10 2.3d10 11 12 13 OH = O- + H+rk(13) = rk(14) * RKeq(4)14 O- + H+ = OH1.0d11 HO2 = 02 + H + rk(15) = rk(16) * RKeq(5) O2 - t u + - uO2 5.0d115 O2 - + H + = HO216 5.0d10 HO2 + OH- = O2- + H2O 17 5.0d10 02 - + H20 = H02 + OH - rk(18) = rk(17) * RKeq(2) / RKeq(5)18 E- + H2O2 = OH + OH-19 1.1d10 E- + O2- + H2O = HO2- + OH-2.0 1.3d10 E - + HO2 = HO2 -21 2.0d10 22 E - + 02 = 02 -1.9d10 23 H + H2O = H2 + OH1.1d1 H + H = H22.4 7.8d9 25 H + OH = H2O7.0d9 26 H + H2O2 = OH + H2O9.0d7 H + O2 = HO2 27 2.1d10 2.8 H + HO2 = H2O21.8d10 29 H + O2- = HO2-1.8d10 OH + OH = H2O2 30 3.6d9 31 OH + HO2 = H2O + O26.0d9 OH + O2 - = OH - + O232 8.2d9 OH + H2 = H + H2O33 4.3d7 OH + H2O2 = HO2 + H2O2.7d7 34 35 HO2 + O2 - = HO2 - + O28.0d7 36 H2O2 = OH + OH2.25d-7 37 OH + HO2 - = HO2 + OH -7.5D9 HO2 + HO2 = H2O2 + O238 7.0d5 OH + Cl- = ClOH-39 4.300D+09 40 OH + HClO = ClO + H2O9.000D+09 6.300D+09 41 OH + ClO2- = ClO2 + H2O - H+ E- + Cl = Cl- + H2O42 1.000D+10 E- + Cl2- = Cl- + Cl- + H2O43 1.000D+10 44 E- + ClOH- = Cl- + OH- + H2O1.000D+10 45 E- + HClO = ClOH-5.300D+10 E- + C12 = C12-46 1.000D+10 47 E- + C13- = C12- + C1-1.000D+10 48 E- + ClO2- = ClO + OH- - H+4.500D+10 E- + ClO3- = ClO2 + OH- - H+ 49 0.000D+00 50 H + Cl = Cl - + H +1.000D+10

51	H + C12 - = C1 - + C1 - + H +	8.000D+09
52	H + ClOH - = Cl - + H2O	1.000D+10
53	H + C12 = C12 - + H +	7.000D+09
54	H + HClO = ClOH - + H +	1.000D+10
55	H + Cl3- = Cl2- + Cl- + H+	1.000D+10
56	HO2 + C12 - = C1 - + HC1 + O2	4.000D+09
57	HCl = Cl - + H +	5.000D+05
58	HO2 + C12 = C12 - + H + + O2	1.000D+09
59	HO2 + C13 - = C12 - + HC1 + O2	1.000D+09
60	02 - + 012 - = 01 - + 01 - + 02	1,200D+10
61	02 + 012 = 01 + 01 + 02	7 500D+06
62	$H_{202}^{-2} + C_{122}^{-2} - H_{C1}^{-1} + H_{C1}^{-1} + O_{22}^{-2}$	1 4000+05
63	$H_{202} + C_{12} = H_{02} + C_{12} + H_{14}$	1 9000+02
64	$H_{202} + H_{12} - H_{02} + H_{12} + H_{12}$	1.300D+02
64 CE	$H_2O_2 + H_CO_2 - H_CO_2 + H_2O_2 + O_2$	1.700D+05
65	OH - + CI2 CIOH - + CI - OH - + CI2 - OH - + CI2 CIOH - + - CI2 CIOH - + - CI2 CIOH - + - CI2 CIOH - + CI2 CIUA CIA	1.300D+00
66	OH- + CI2 = HCIO + CI-	1.000D+10
67	H+ + ClOH- = Cl + H2O	2.100D+10
68	H20 + C1202 = HC10 + C102 - + H +	2.000D+02
69	H20 + C1202 = 02 + HC10 + HC1	0.000D+00
70	H2O + Cl2O = HClO + HClO	1.000D+02
71	H2O + C12O4 = C1O2 - + C1O3 - + H + + H +	1.000D+02
72	H2O + C12O4 = HC1O + HC1 + O4	1.000D+02
73	O4 = O2 + O2	1.000D+05
74	Cl- + Cl = Cl2-	2.100D+10
75	Cl- + ClOH- = Cl2- + OH-	9.000D+04
76	Cl - + HClO = Cl2 + OH -	6.000D-02
77	C1- + C12 = C13-	1.000D+04
78	Cl - + H + = HCl (assuming pKa = -3.9)	6.295D+01
79	ClOH- = OH + Cl-	6.100D+09
80	C12 - = C1 + C1 - C1	1.100D+05
81	C12 - + C12 - = C13 - + C1 -	7 0000+09
82	C12 + C12 + C1-	5 000D+04
83	$C_{10} + C_{10} = C_{1202}$	1 500D+04
0.0	C102 + C102 = C1202	1.0000+02
04	C102 + C102 - C1204	1.00000+02
00	C1202 + C102 C103 - + C120	1.000D+02
00	E = + CIOS = - CIR = -	1.0000+03
87	CIR + OH = OH- + CIO3-	1.000D+10
88	CIR - + 0 - = 0H - + CI03 H +	1.200D+09
89	HC10 + HC10 = C1 - + C102 - + H + H + H +	6.000D-09
90	C102 - + HC10 = C1 - + C103 - + H +	9.000D-07
91	HClO + HClO = O2 + HCl + HCl	3.000D-10
92	HC104 = H+ + C104- (a guess)	1.000D+10
93	H+ + ClO4- = HClO4 (assuming pKa = -7)	1.000D+03
94	Br- + OH = BrOH-	1.100D+10
95	Br - + Br = Br2 -	1.000D+10
96	Br - + H = HBr -	0.000D+06
97	Br- + O- = Br + OH H+	2.200D+08
98	Br + BrO - = Br - + BrO	4.100D+09
99	Br = BrOH - + H + - H2O	1.400D+00
100	Br + HO2 = H + Br - + O2	1.600D+08
101	Br + OH- = BrOH-	1.300D+10
102	Br + H2O2 = Br - + O2 - + H + + H +	2.500D+09
103	$Br^2 - = Br + Br -$	1,900D+04
104	$Br^{2} + Br^{2} = Br^{2} + Br^{3}$	3 4000+09
105	$Br^{2} + Br^{2} = Br^{2} + Br^{2} + Br^{2}$	8 0000+07
106	$Br^2 + Br^2 = Br^2 + Br^2 + Br^2$	6 2000+07
107	$Br_{2} + ClO_{2} - Br_{2} + ClO_{2} + Br_{2}$	2 0000+07
100	D_{2} + D_{2} + D_{2} + D_{2} + D_{2} + D_{2}	2.000D+07
100	$DIZ = T \Pi = \Pi T T BI = T BI =$	1.400D+10
T0A	$Br_2 - + HO_2 = H_1 + Br_2 + Br_3 + O_2$	1.000D+08
110	Br2 + 02 = Br + Br + 02	1.700D+08
111	Br2- + E- = Br- + Br-	1.100D+10
112	Br2- + H2O2 = Br- + Br- + HO2 + H+	1.900D+06
113	BrO- + OH = BrO + OH-	4.200D+09
114	BrO- + O- = BrO + OH H+	3.500D+09

115	BrO- + E- = Br- + O-	1.500D+10
116	BrO2- + OH = BrO2 + OH-	2.300D+09
117	BrO2- + BrO = BrO- + BrO2	4.000D+08
118	BrO2- + O- = BrO2 + OH H+	1.600D+09
119	BrO2- + E- = BrO + H2O - H+ - H+	1.100D+10
120	BrO3- + OH = BrO3 + OH-	0.000D+06
121	BrO3- + H = BrO2 + OH-	2.000D+07
122	BrO3- + O- = BrO3 + OH H+	0.000D+06
123	BrO3- + E- = BrO2 + OH- + OH H2O	3.400D+09
124	Br2 + H = Br2 - + H +	1.000D+10
125	Br2 + HO2 = H+ + O2 + Br2 -	1.300D+08
126	Br2 + O2- = O2 + Br2-	5.000D+09
127	Br2 + Br- = Br3-	9.600D+08
128	Br2 + E - = Br2 -	5.300D+10
129	HOBr + OH = BrO + H2O	2.000D+09
130	HOBr + O2 - = O2 + Br + OH -	3.500D+09
131	BrO2 + OH = BrO3 - + H +	2.000D+09
132	BrO2 + BrO2 = BrO3 - + BrO2 - + H + + H + - H2O	4.000D+07
133	Br02 + C102 - = Br02 - + C102	3.600D+07
134	Br3- + H = H+ + Br2- + Br-	1.200D+10
135	Br3- + 02- = 02 + Br2- + Br-	1.500D+09
136	Br3- = Br2 + Br-	5.500D+07
137	Br3- + E- = Br2- + Br-	2.700D+10
138	BrOH- = Br- + OH	3.000D+07
139	BrOH- = Br + OH-	4.200D+06
140	BrOH- + H+ = Br + H2O	1.300D+10
141	BrOH- + Br- = Br2- + OH-	1.900D+08
142	BrO + BrO = BrO - + BrO2 - + H + + H + - H2O	2.800D+09
143	BrO + BrO2 - = BrO - + BrO2	4.000D+08
144	HOBr = H+ + BrO-	1.580D+01
145	BrO- + H+ = HOBr	1.000D+10
146	Br - + Cl2 - = BrCl - + Cl -	4.00D+09
14/	BrCI - + CI - = CI2 - + Br -	1.10D+02
148	Brcl = cl + Br	8.50D+07
149	Br + CI - = BrCI -	1.00D+10
150	BrCI - + Br - = BrZ - + CI -	8.00D+09
152	BIZ + CI = BICI + BI =	4.30D+08
152	$BI^{-} + CI2 = BICI2^{-}$ $Brcl2 = Cl2 + Br =$	0.00D+03
154	BrCl2 = BrCl + Cl =	9.00D+05
155	BrCl + Cl = BrCl2	1.00D+06
156	$\frac{\text{Brcl}^2}{\text{Brcl}^2} + \frac{\text{Brc}}{\text{Brc}} = \frac{\text{Brc}^2}{\text{Brc}^2} + \frac{\text{Cl}}{\text{Cl}}$	3 000+08
157	BrCl = HOBr + H+ + Cl H2O	3.00D+06
158	HOBr + Cl = BrCl + H2O - H+	2 30D+10
159	BrCl = HCl0 + H+ + Br H20	1 150-03
160	HC10 + Br = BrC1 + H20 - H+	1 32D+06
161	$Br - + HOBr = Br^2 + H^2O - H^+$	3 000+09
162	$Br^{2} = Br^{-} + HOBr + H^{+} - H^{2}O$	2.000+00
163	Br - + HBrO2 = HOBr + HOBr - H+	3.00D+06
164	HOBr + HOBr = Br - + HBrO2 + H+	2.00D-05
165	Br- + BrO3- = HOBr + BrO2 H+	2.500D-7
166	HOBr + HBrO2 = Br - + BrO3 - + H + + H +	3.20D+00
167	HBrO2 + HBrO2 = HOBr + BrO3 - + H+	3.00D+03
168	HOBr + BrO3- = HBrO2 + HBrO2 - H+	1.00D-08
169	HBrO2 + BrO3- = BrO2 + BrO2 + H2O - H+	4.20D+01
170	Br02 + Br02 = HBr02 + Br03- + H+ - H20	4.20D+07
171	HBrO2 = BrO2 - + H +	5.00D+05
172	BrO2 - + H + = HBrO2	1.35D+09
173	BrCl- + BrCl- = BrCl + Br- + Cl-	1.20D+09
174	Br2 + Cl- = Br2Cl-	1.00D+07
175	Br2Cl- = Br2 + Cl-	7.69D+06
176	BrCl + Br- = Br2Cl-	1.00D+07
177	Br2Cl- = BrCl + Br-	5.56D+02

APPENDIX B: FORTRAN Listing for Empirical RM

```
Emp-RM.f
       implicit real*8 (a-h,o-z)
       ddot = 160.d0 ! rad/s
      Brext = 1.d-6
       do i=0,200
      do j=0,200
      O2ext = dfloat(i)/2.d7 + 1.d-11
G2 = Gcond(det) 22
                                                   ! mole/L
                                                  ! mole/L
       G2 = Gcond(ddot,O2ext,H2ext,Brext)
       write(*,*) H2ext,O2ext,G2
       enddo
       write(*,"(1x)")
       enddo
       STOP
       end
       FUNCTION Gcond(ddot,O2ext,H2ext,Brext)
       implicit real*8 (a-h,o-z)
                                  ! L/mole-s
      rk27 = 2.1d10
      rk23 = 1.1d1/56.d0 ! L/mole-s divided by 56
       rk26 = 9.0d7 ! L/mole-s
             = 0.0d0
= 4.3d7
      rk36
                                  ! L/mole-s
      rk33
      rk94
             = 1.1d10 * 10.
      BrFact = rk33*H2ext/(rk33*H2ext + rk94*Brext)
       if(Brext.eq.0.) BrFact = 1.d0

      GH
      = 0.100d0*(1.d0-dexp(-(H2ext*BrFact/7.8d-4)/.1d0))
      ! molecules/eV

      GOH
      = 0.350d0*(1.d0-dexp(-(H2ext*BrFact/7.8d-4)/.3d0))
      ! molecules/eV

      CH2O = 1.d3/18.d0 ! mole/L
DO2 = 2.500d-05 ! cm^2/s
       DH2O2 = 1.900d-05
                                 ! cm^2/s
       dx = 3.5d-3
                                 ! cm
             = 0.475 d0/dx
       dN
       GOH = GOH * BrFact
          02 = 02ext + 2.d-6*Brext/(Brext+0.5d-6)
          H2 = H2ext
          H2O = CH2O
          \begin{array}{rcl} dk27 & = & rk27 \\ dk23 & = & rk23 \end{array}
          dk26 = rk26
          dk36 = rk36
      dkO2 = DO2/(dN*dx**2) ! 1/s
dkH2O2 = DH2O2/(dN*dx**2) ! 1/s
```

dot= ddot*(1.d0/(1.602d-19*1.d4*6.022d23))

```
A0 =
         -dk23*dk27*H20*dkH202**2
A1 = -dkH202*(dk26*dk27*dk02*02+dk23*dk26*dk02*H20)
1 - 2.d0*(dk23*dk27*H2O)*(dkH2O2+dk36))
2 + dot*(gH+gOH)*dk26*dk27*dkH2O2
A2 = (dkH202+dk36)*(dk26*dk27*dk02*02+dk23*dk26*dk02*H20)
1 - (dk23*dk27*H2O)*(dkH2O2+dk36) )
2 + dot*(gH+gOH)*dk26*(dk26*dkO2-dk27*dkH2O2-dk27*dk36)
Gcond = (-A1 + dsqrt(A1**2 - 4.d0*A2*A0))/(2.d0*A2)
 Gcond = dkH2O2/(dkH2O2+dk36+dk26*dot*(qOH+gH)/
1
      (dk23*H2O+dk27*O2))
 RETURN
 end
 SUBROUTINE NLconc(C1p,C1m,C0,dlam0,A,dN,dk)
 implicit real*8 (a-h,o-z)
 B = -(1.d0 - 1.d0/(A*C0) - dN*dlam0/(dk*A*C0))
 C = -1.d0/(A*C0)
 C1p = (-B + dsqrt(B**2 - 4.d0*C))/2.d0
 Clm = (-B - dsqrt(B**2 - 4.d0*C))/2.d0
 RETURN
 end
```

С

С